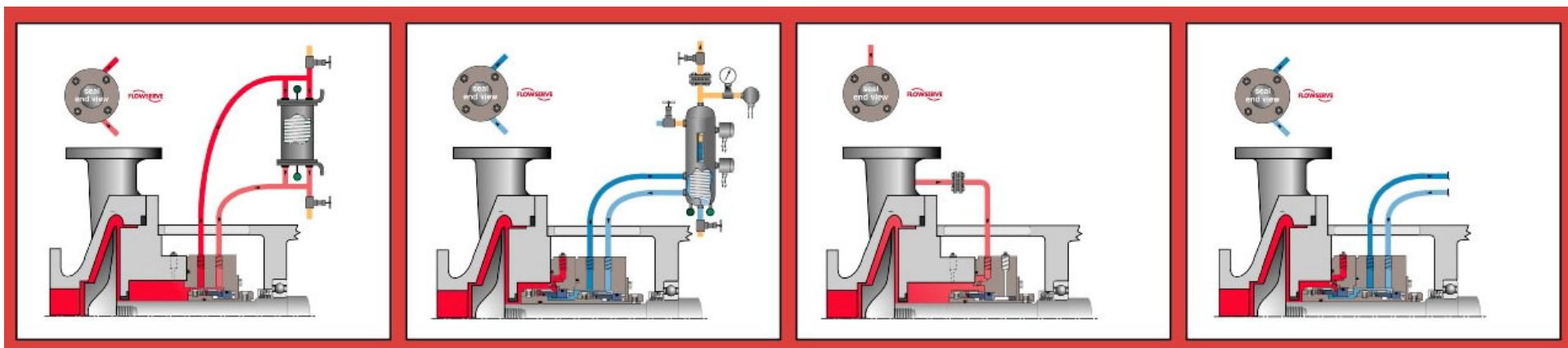


Piping Plans for Dual Mechanical Seals



Purpose of Piping Plans

➤ Create a more favorable environment for the mechanical seal

- Flushing to remove heat
- Lowering fluid temperature
- Altering the seal chamber pressure
- Cleaning the process fluids
- Control atmospheric side of seal



Purpose of Piping Plans

- Provide a means of detecting and controlling seal leakage
 - Capture and/or prevent leakage
 - Detect leakage
 - Route leakage to appropriate collection or disposal system
 - Provide fluid other than process fluid for the seal environment



Requirements of Mechanical Seals

➤ Liquid seals

- Stable fluids
- Good lubricating properties
- Fluids do not flash or vaporize in seal chamber
- Free from contamination and solids
- Moderate viscosities



Requirements of Mechanical Seals

➤ Gas seals

- Gas or vapor suitable for sealing
- Constant supply of external buffer/barrier gas
- Process fluids free from contamination from both liquids and solids
- Process fluids which are not adversely affected by gas leakage



Methods of Achieving Goals

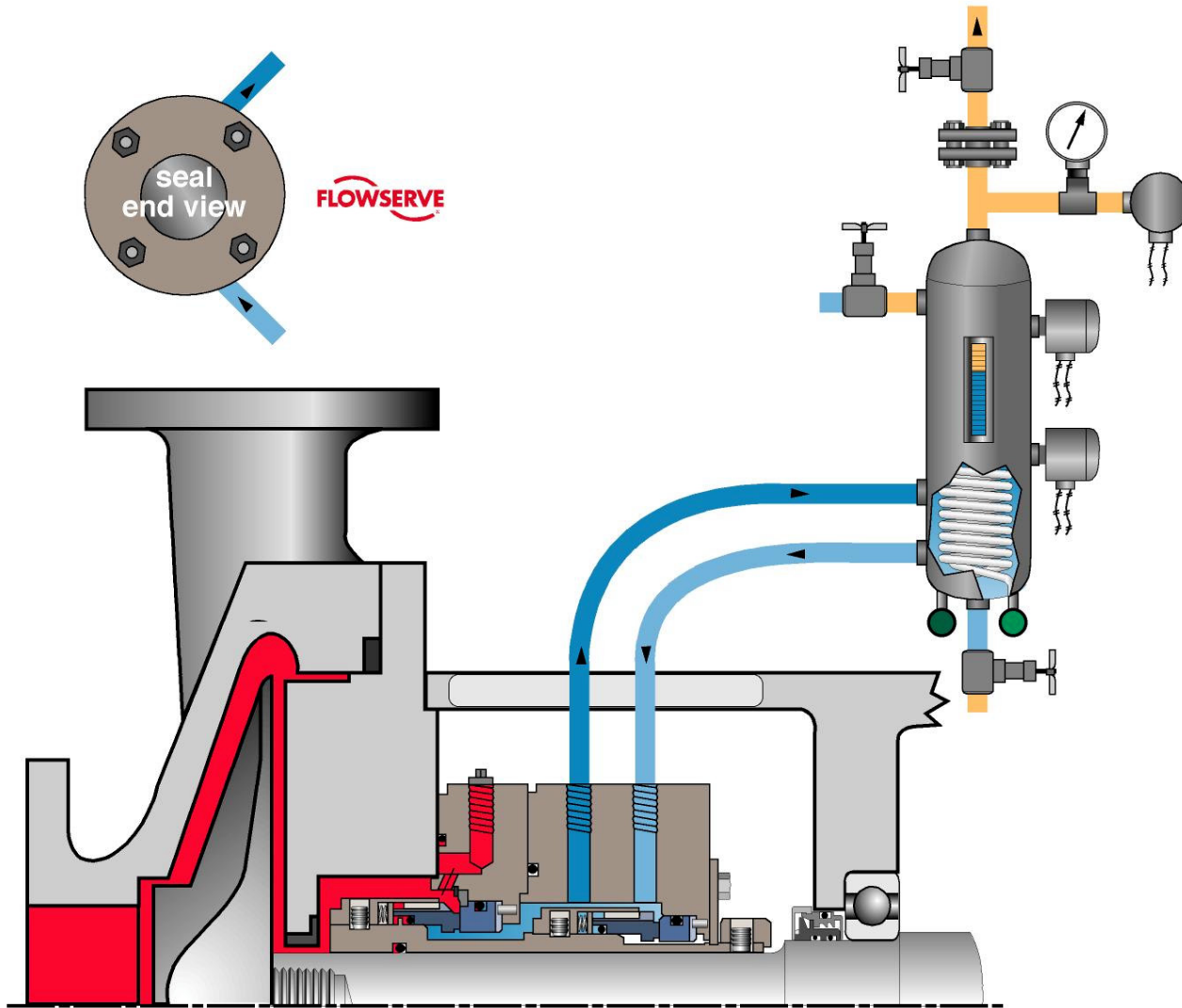
- Piping or routing of process fluids
- Introduction of external fluids
- Auxiliary equipment
 - Seal coolers
 - Cyclone separators
 - Reservoirs
- Instrumentation



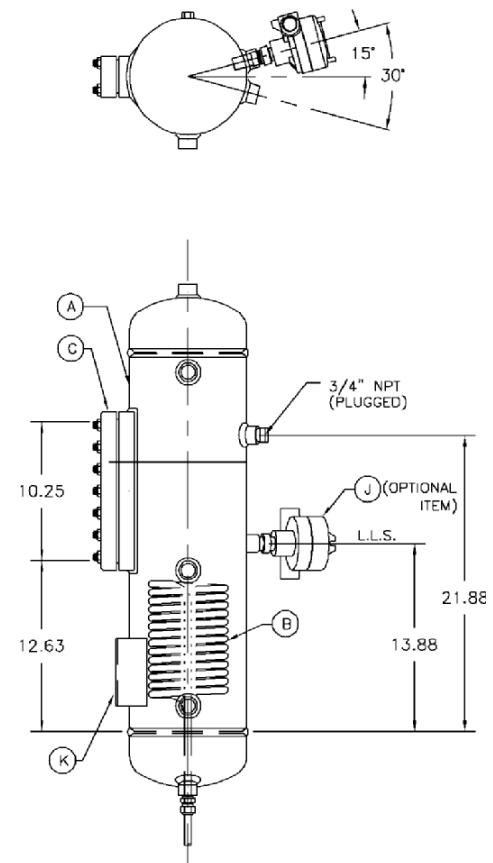
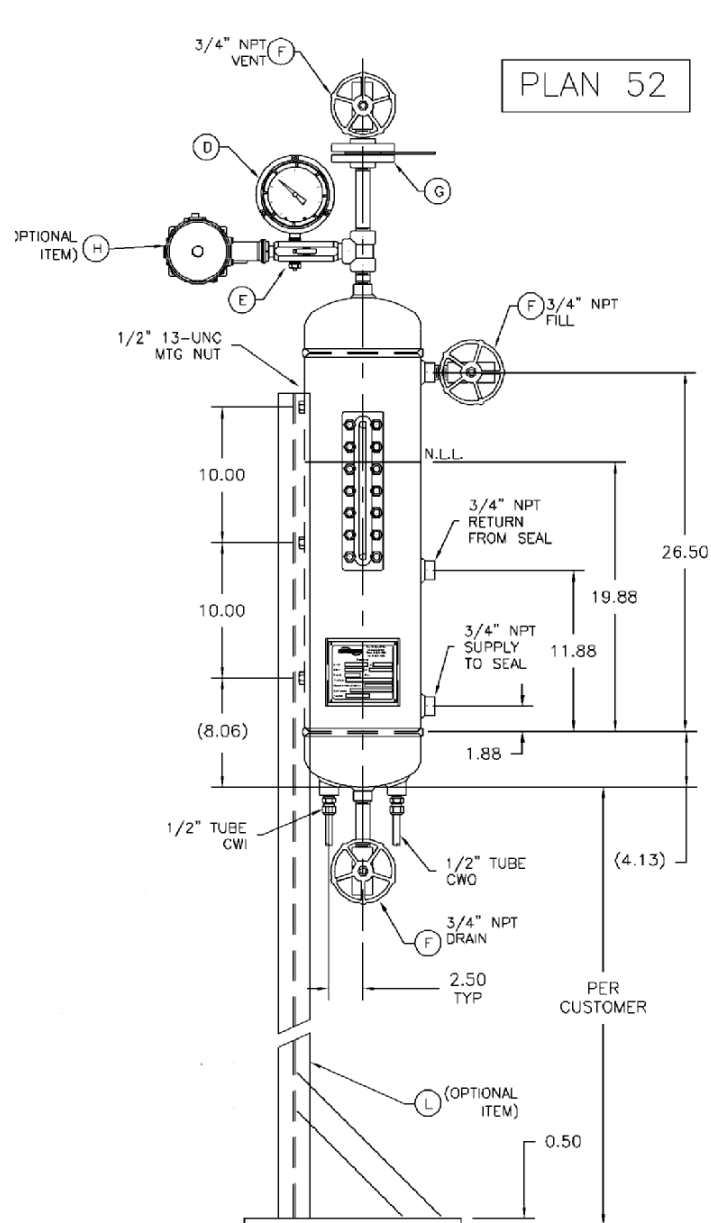
Plan 52

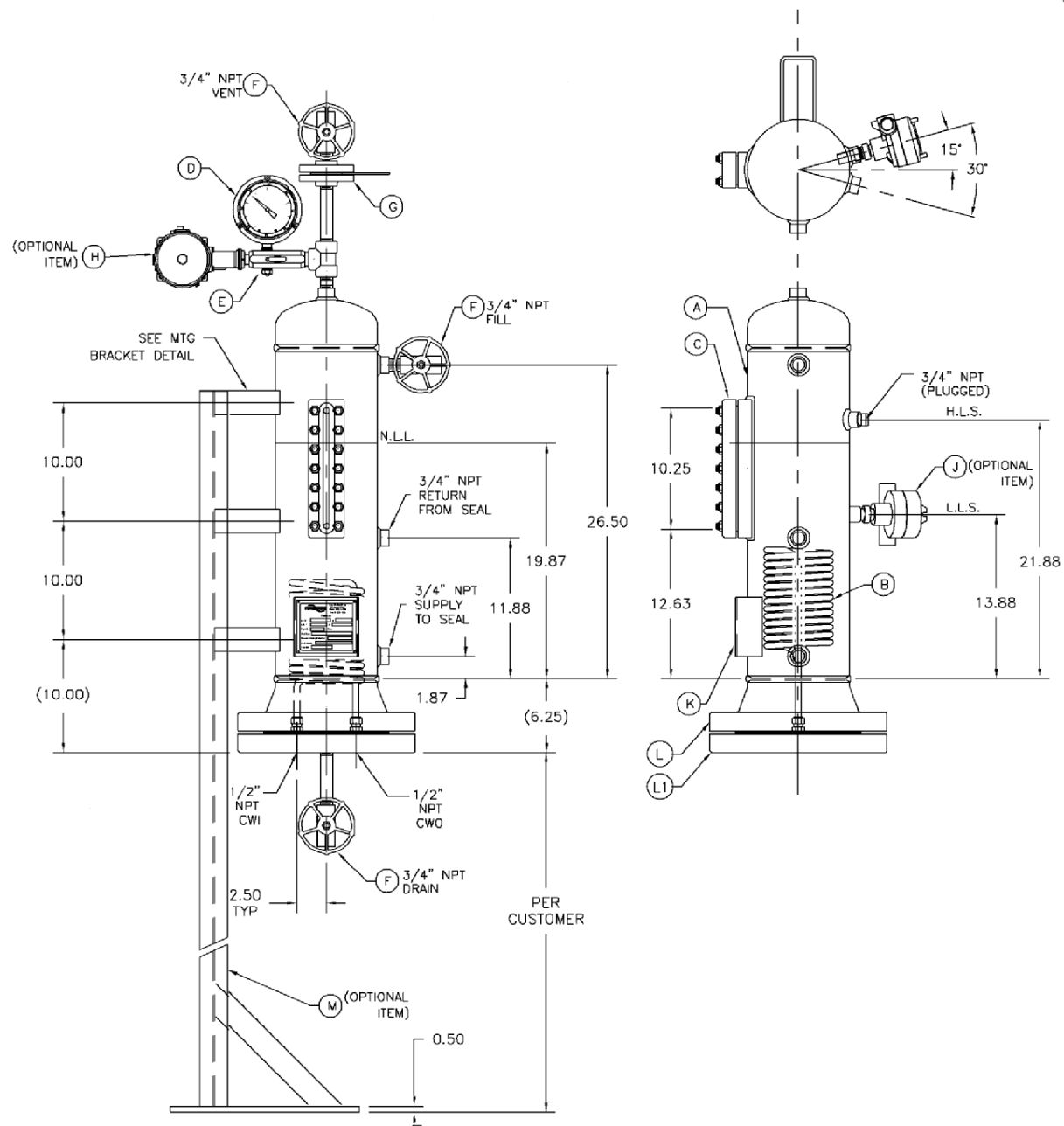
What

- Unpressurized buffer fluid circulation through reservoir.
- Fluid is circulated by a pumping ring in the dual seal assembly.



PLAN 52

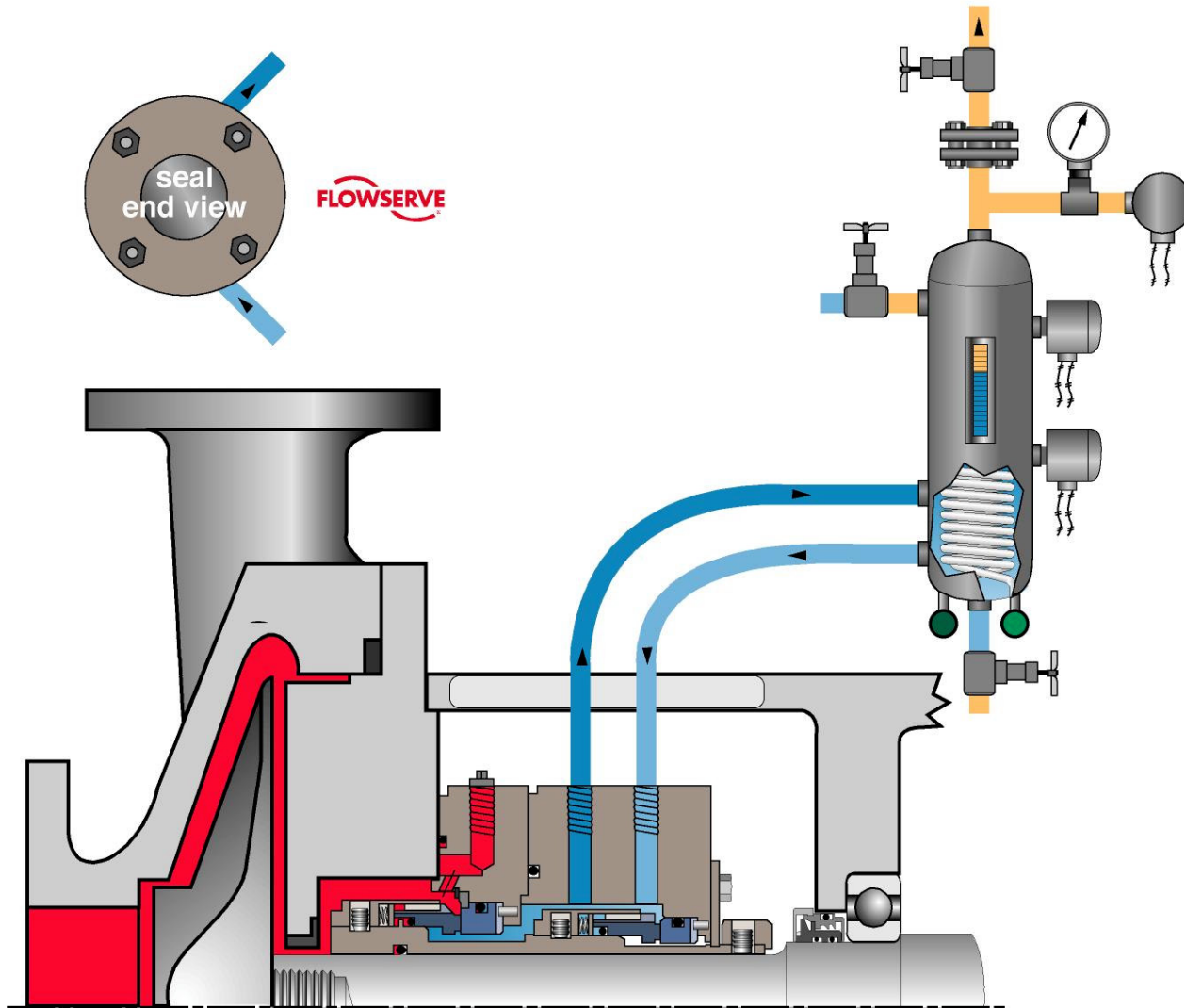




Plan 52

Why

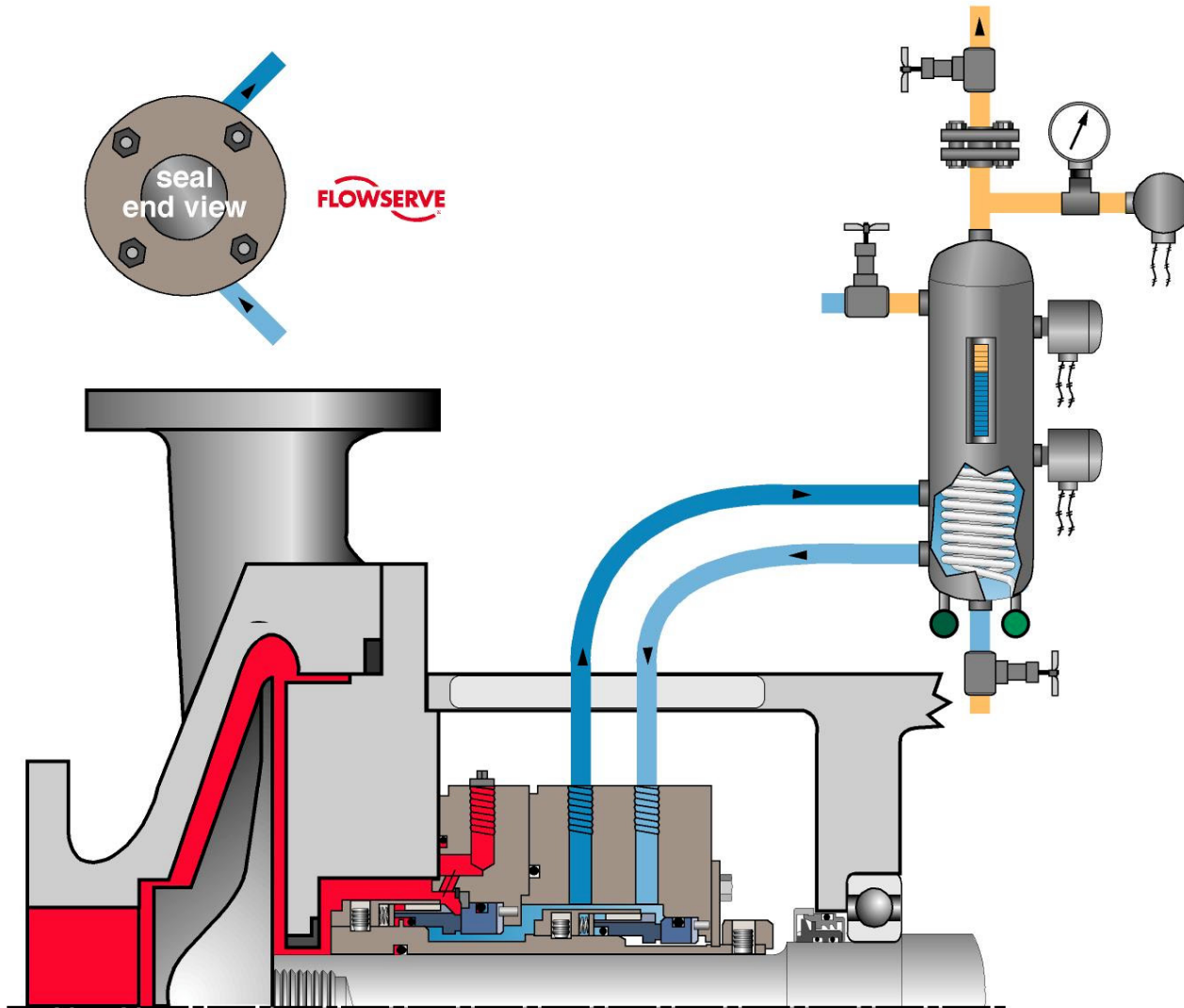
- Outboard seal acts as a safety backup to the primary seal.
- Zero to very low process emissions.
- No process contamination is allowed.



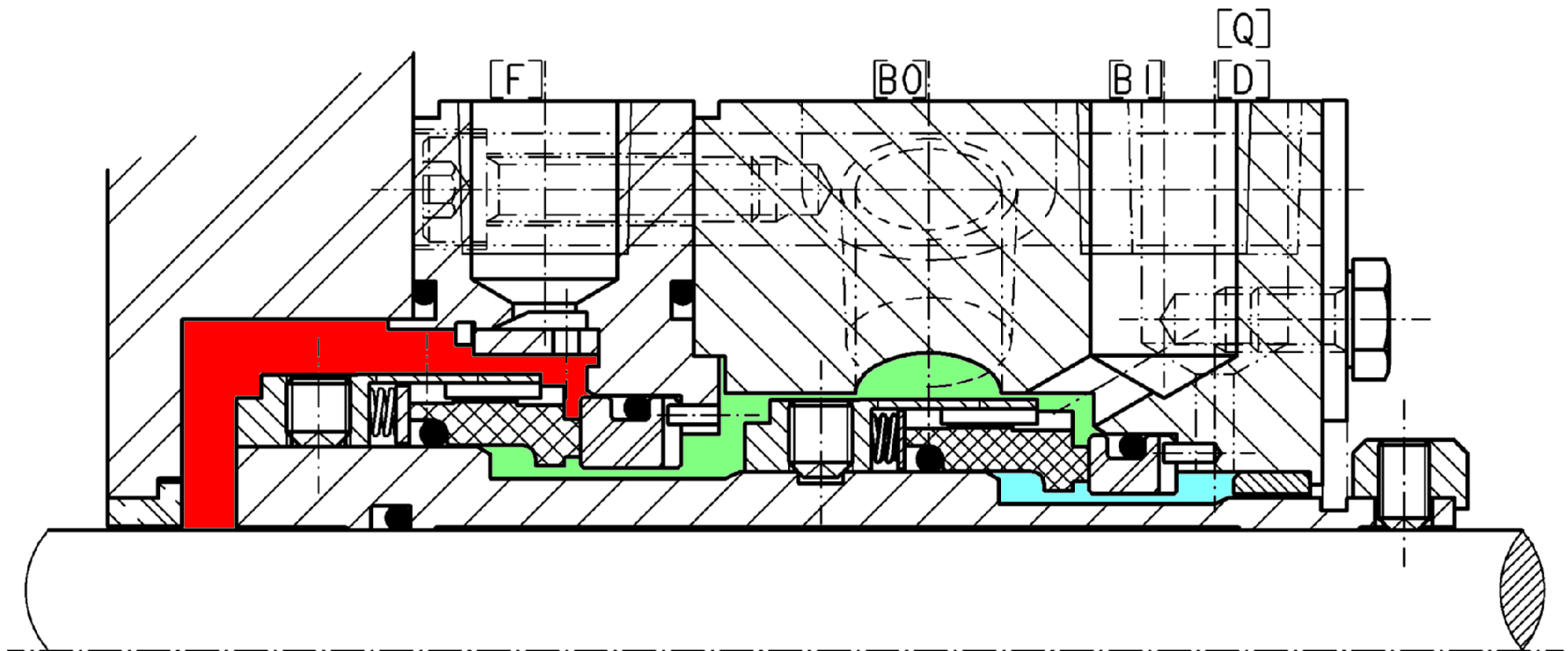
Plan 52

Where

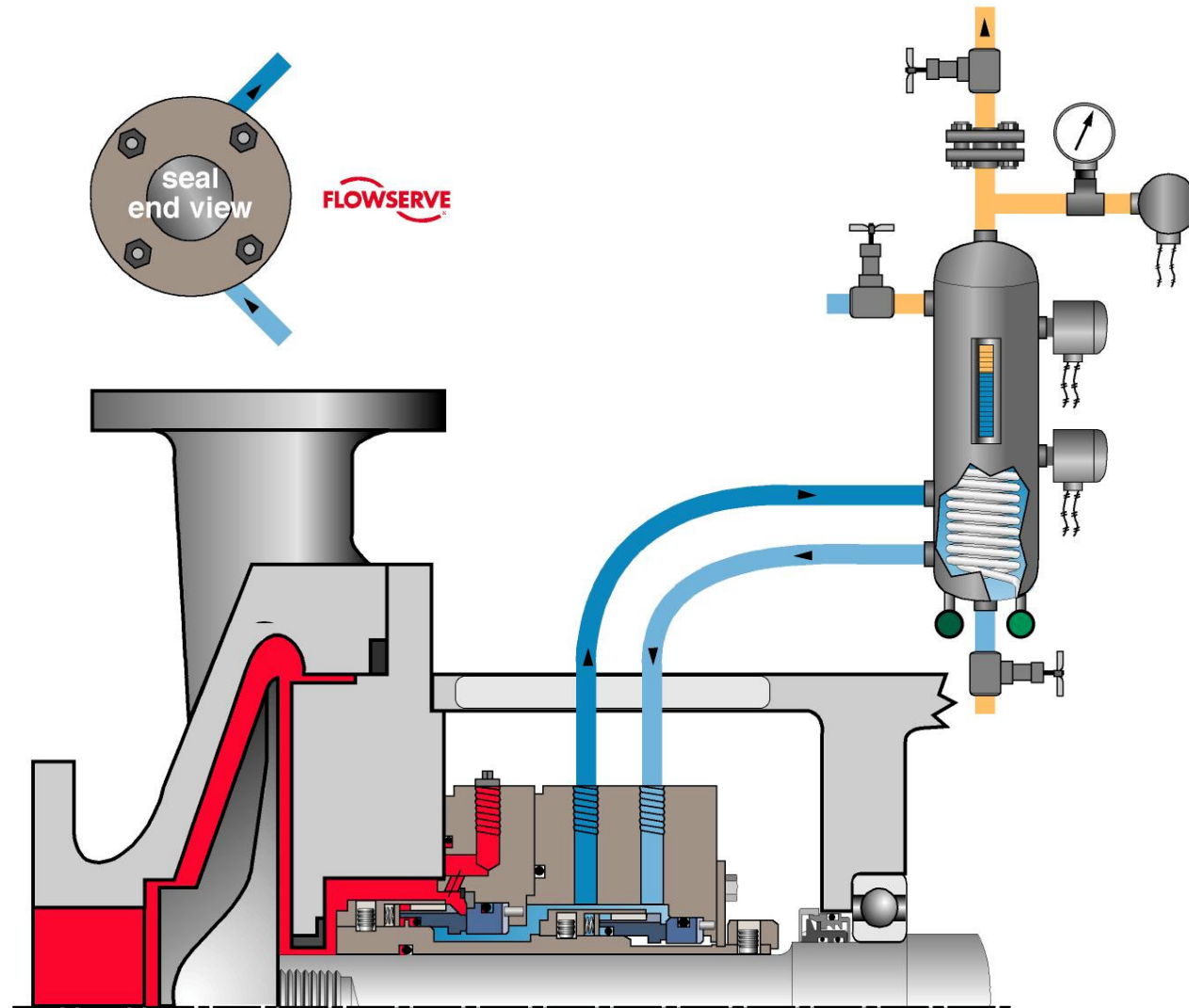
- Used with dual unpressurized seals (“tandem”).
- High vapor pressure fluids, light hydrocarbons.
- Hazardous or toxic fluids.
- Heat transfer fluids.



API 682 Type A Arrangement 2 2CW-CW



Plan 52



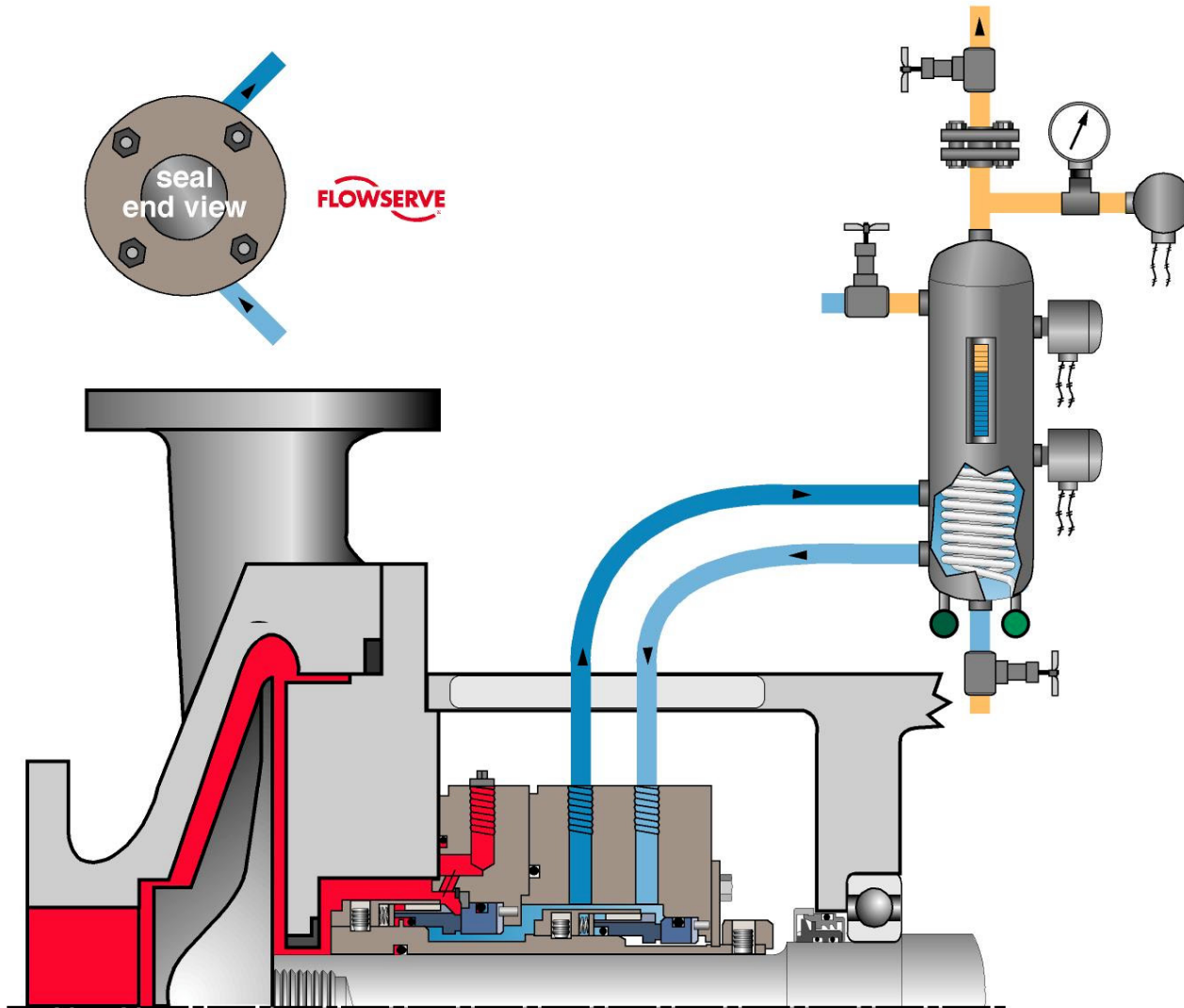
Preventative Maintenance

- Piping loop must self-vent to vapor recovery/flare system near atmospheric pressure.
- Process vapor pressure is generally greater than reservoir pressure.
- Buffer fluid must be compatible with process leakage.

Plan 52

Preventative Maintenance (continued)

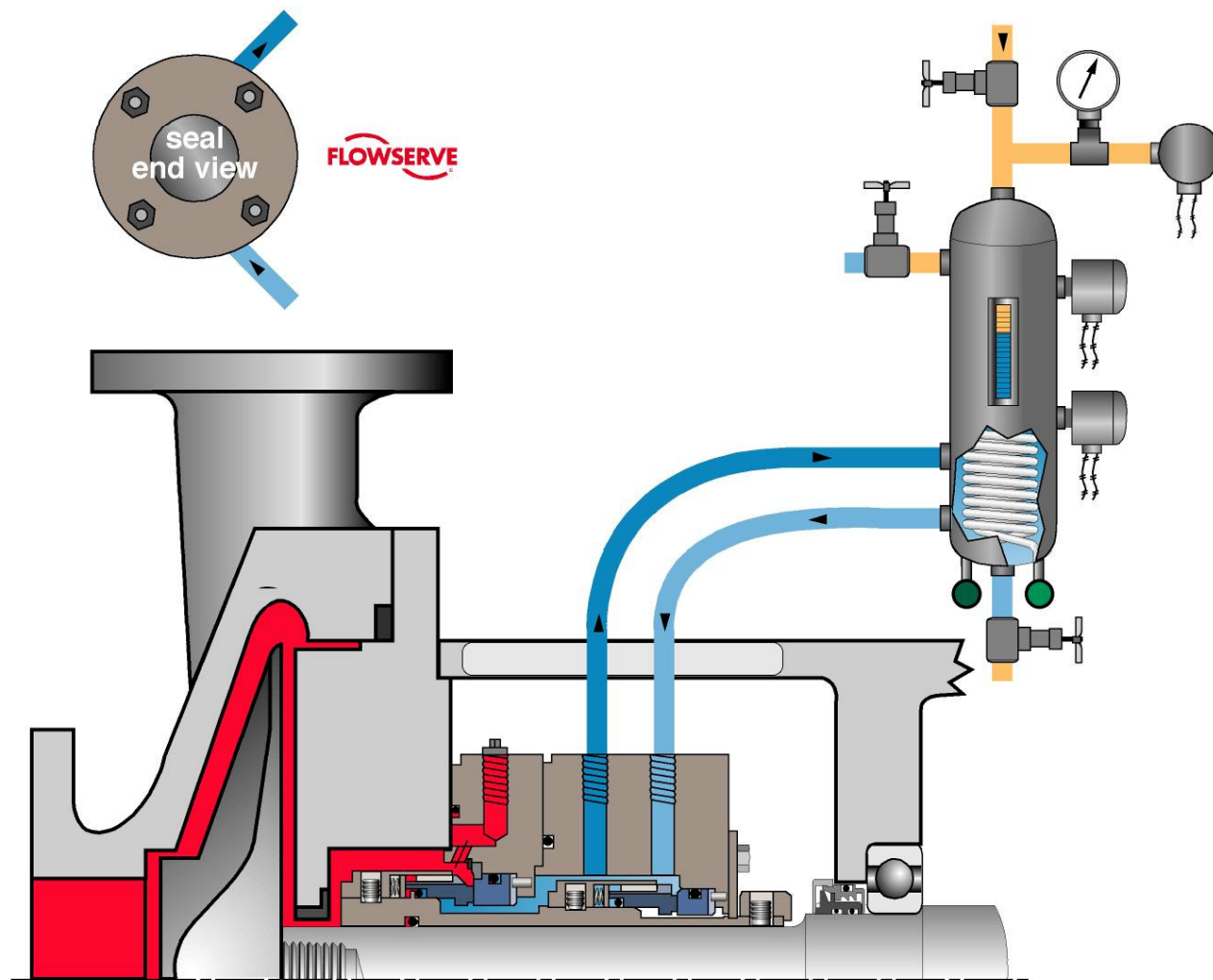
- Primary seal leakage is indicated by increased vent pressure.
- Reservoir level gage indicates outboard seal leakage.

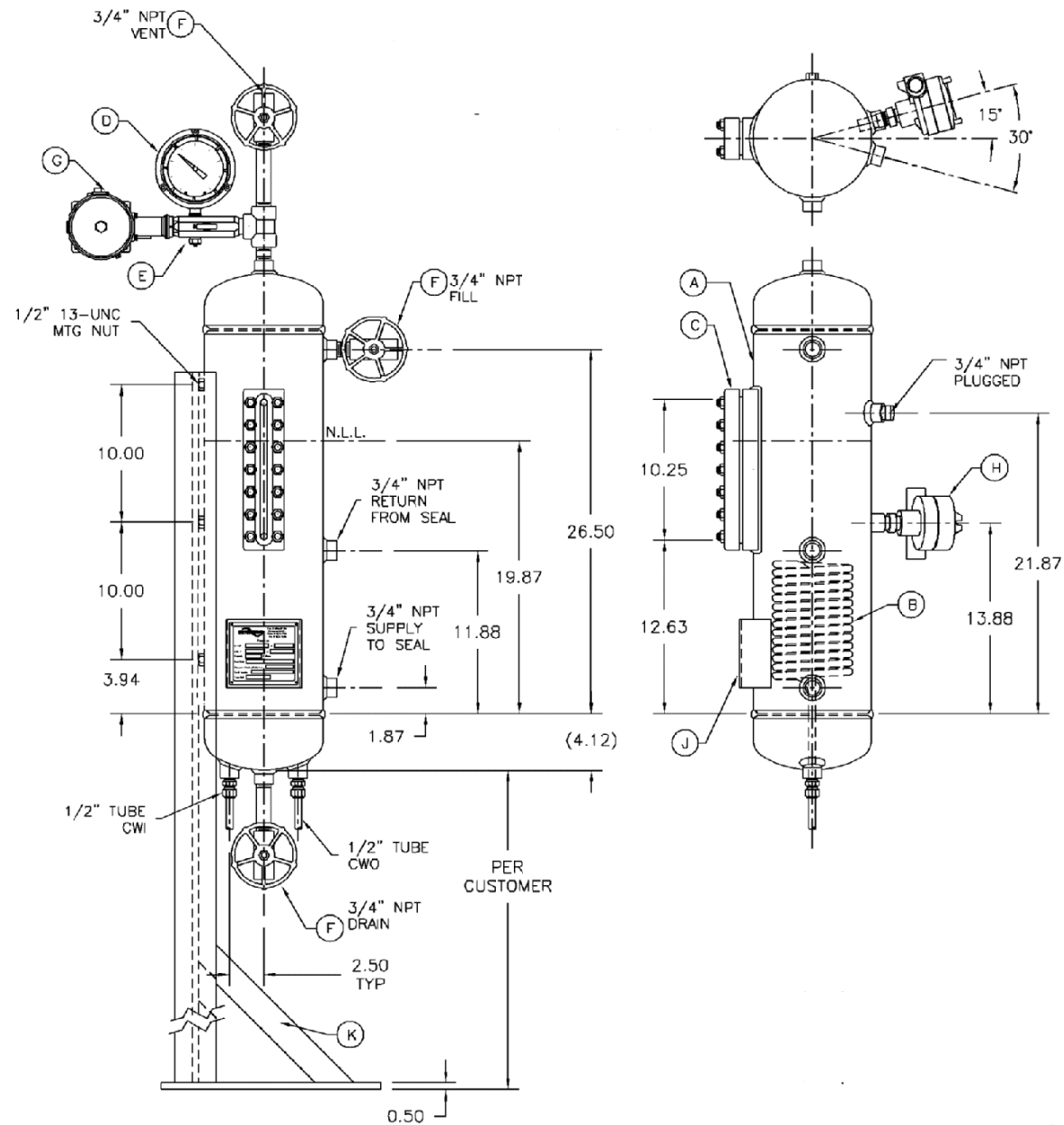


Plan 53A

What

- Pressurized barrier fluid circulation through reservoir.
- Fluid is circulated by a pumping ring in the dual seal assembly.

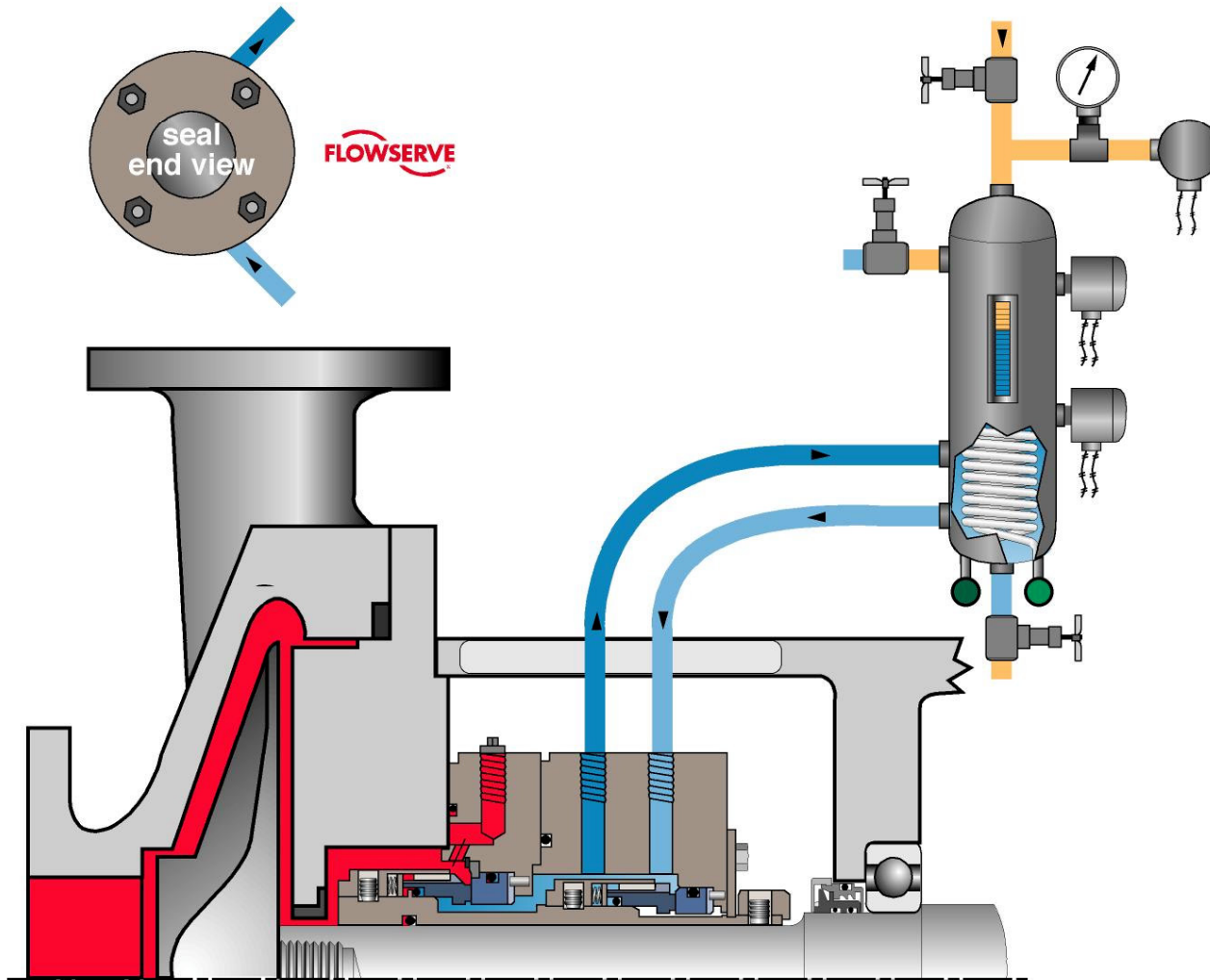




Plan 53A

Why

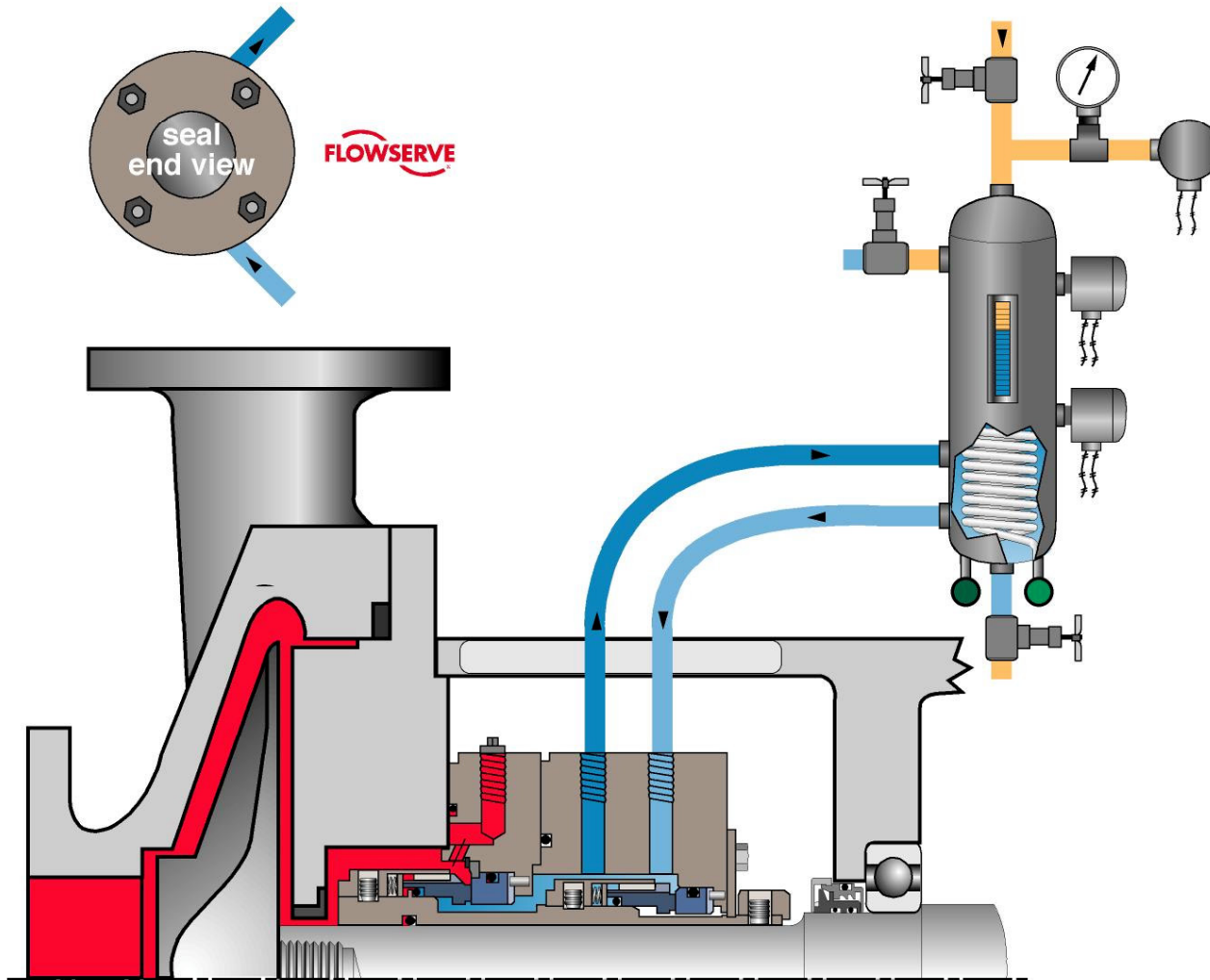
- Isolate process fluids.
- Zero process emissions.



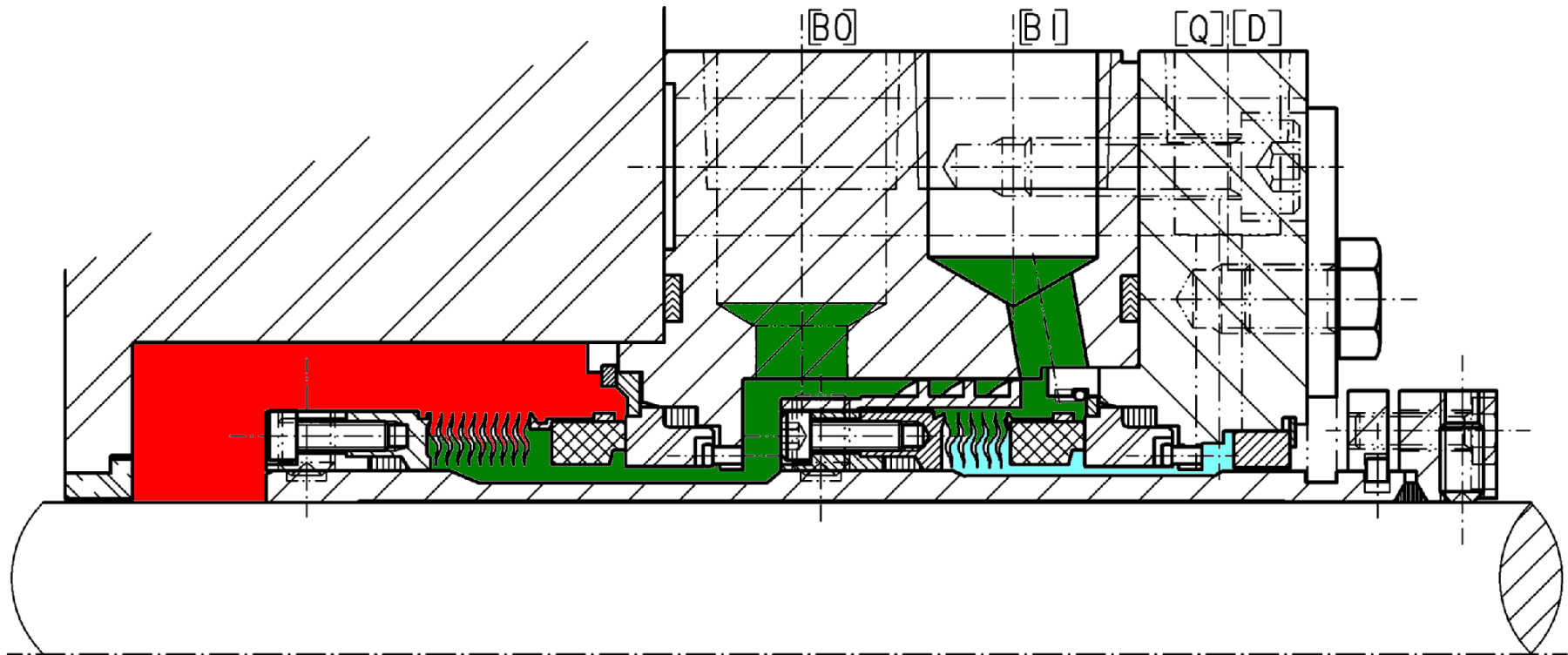
Plan 53A

Where

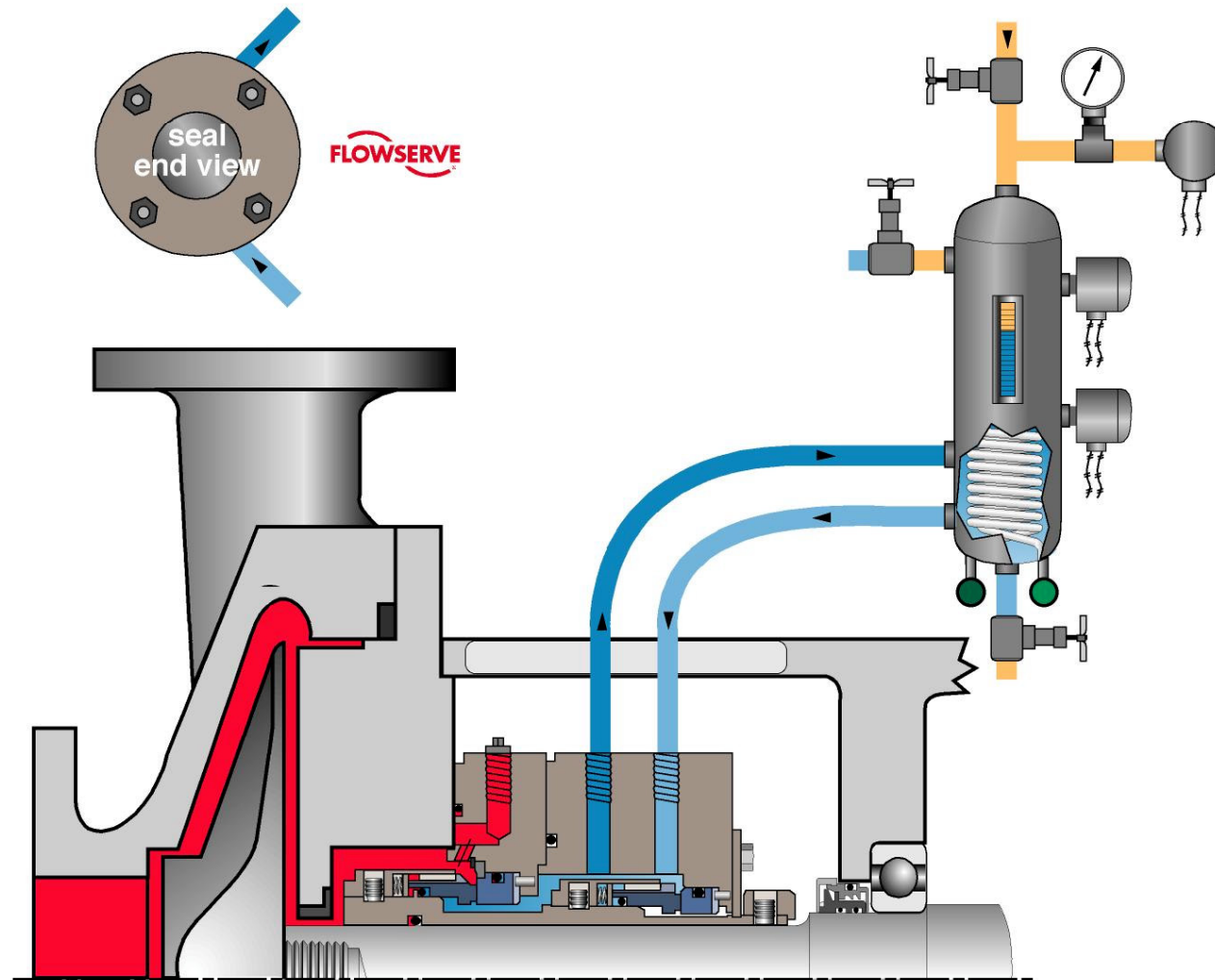
- Used with dual pressurized seals (“double”).
- High vapor pressure fluids, light hydrocarbons.
- Hazardous or toxic fluids.
- Heat transfer fluids.
- Dirty, abrasive or polymerizing fluids.
- Mixers or agitators.
- Vacuum service.



API 682 Type C Arrangement 3 3CW-FB



Plan 53A



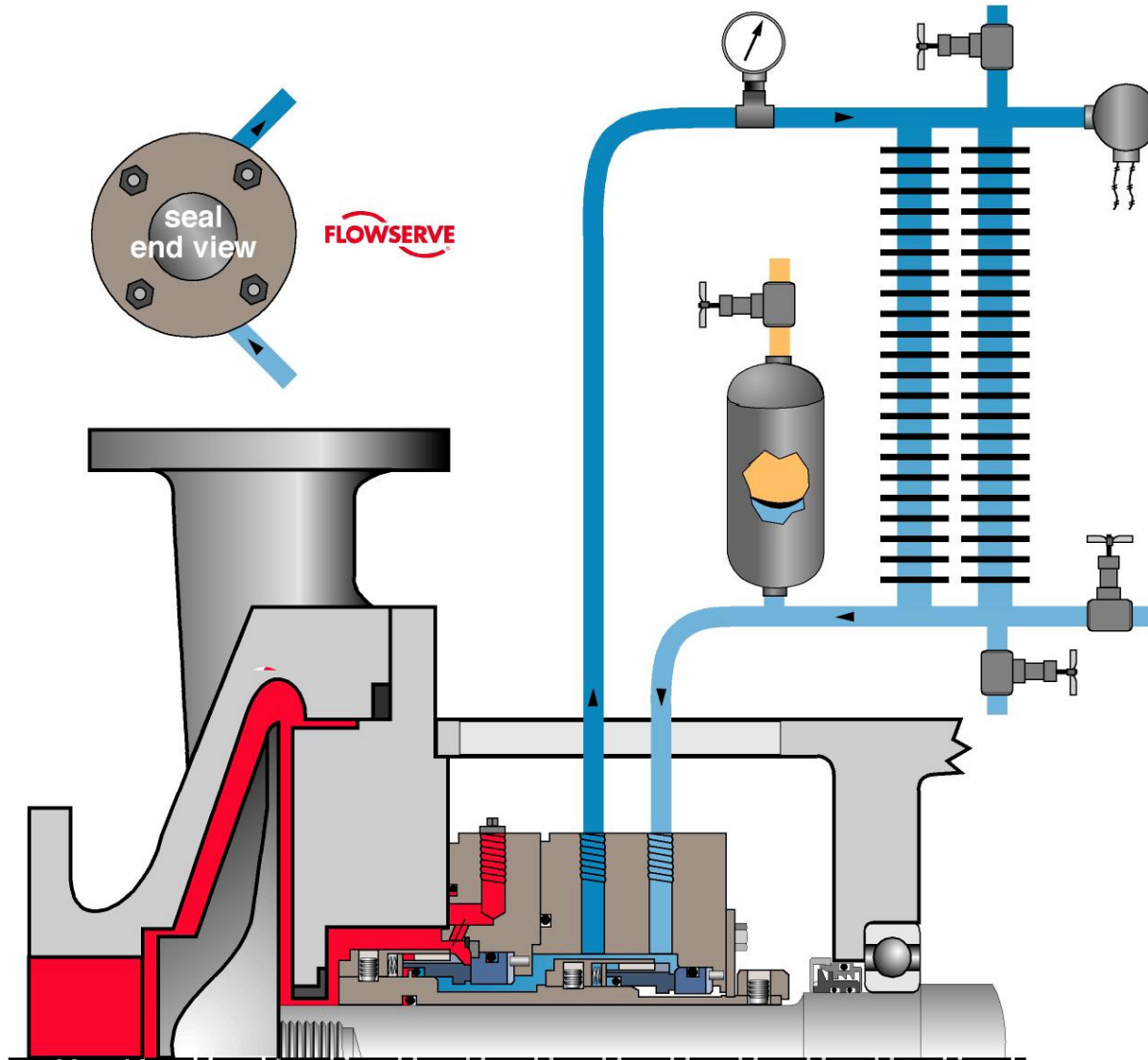
Preventative Maintenance

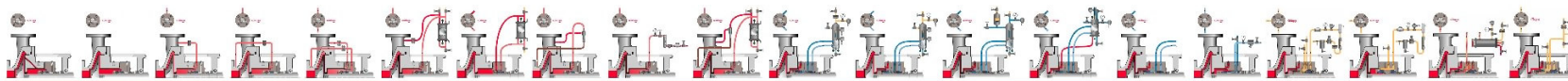
- Piping loop must self-vent to reservoir located at highest elevation.
- Pressurize reservoir at all times, maximum gas charge 150 - 200 psi (10 - 14 bar)
- Barrier fluid must be compatible with process.
- Reservoir level gage indicates both IB and OB seal leakage.

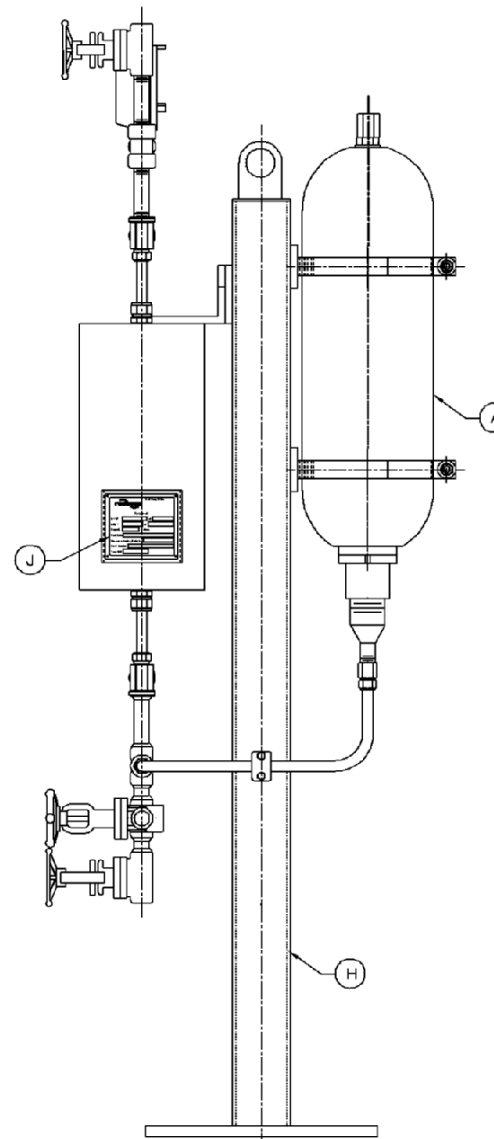
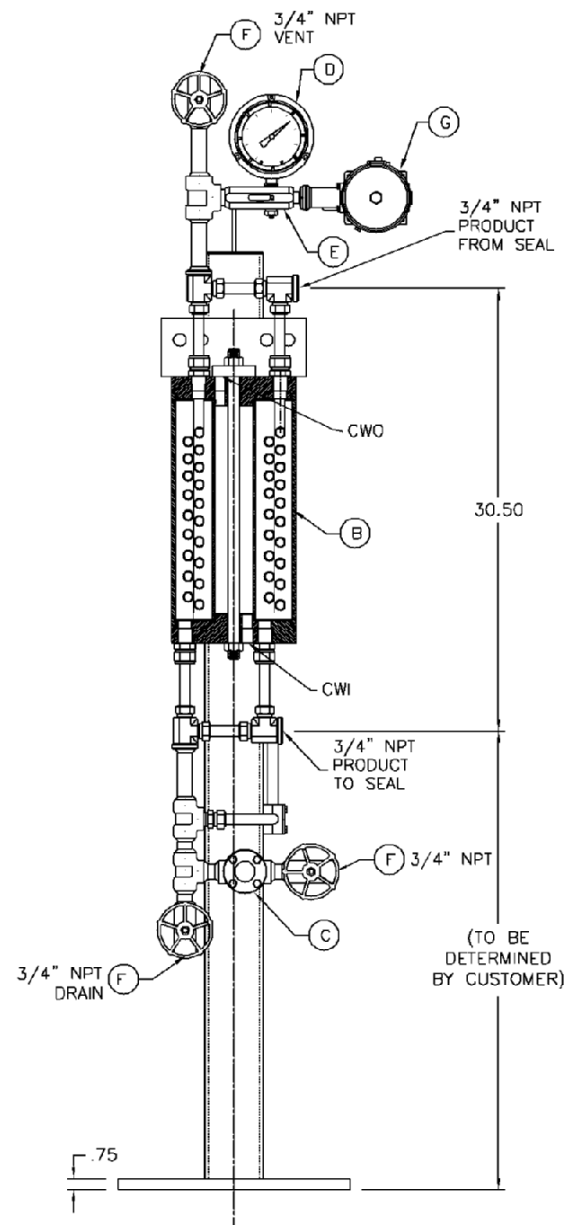
Plan 53B

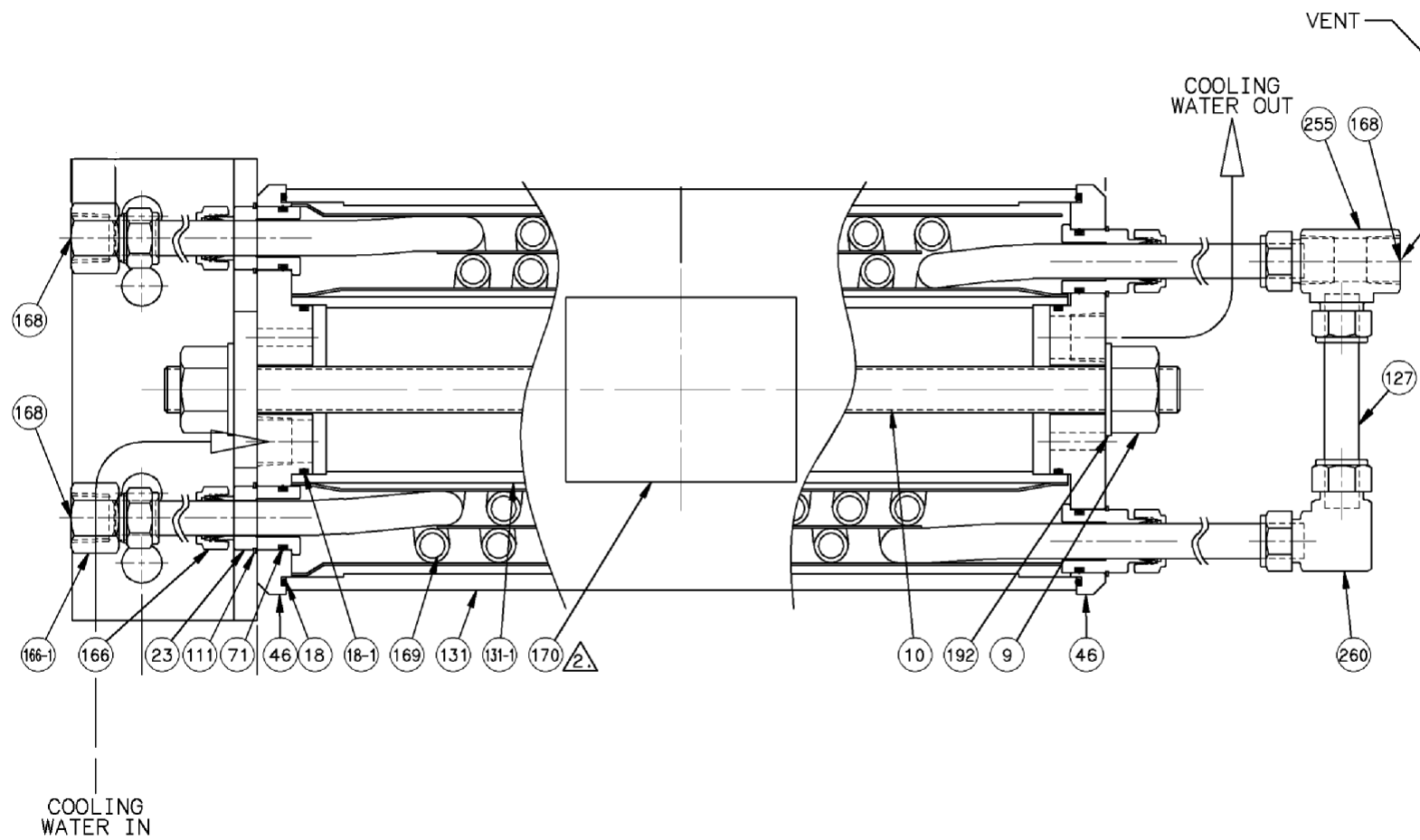
What

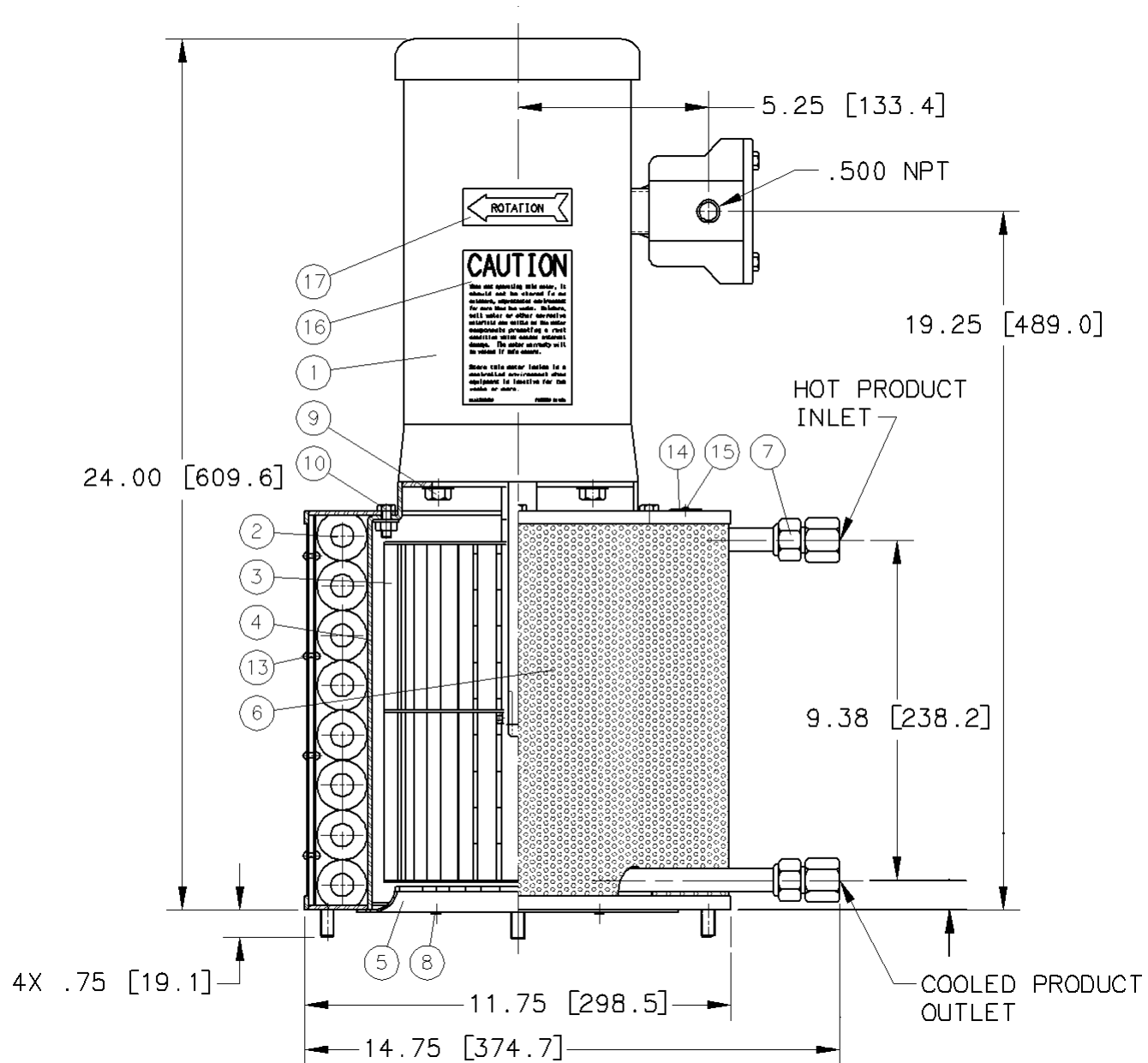
- Pressurized barrier fluid circulation with a bladder accumulator.
- Fluid is circulated by a pumping ring in the dual seal assembly.







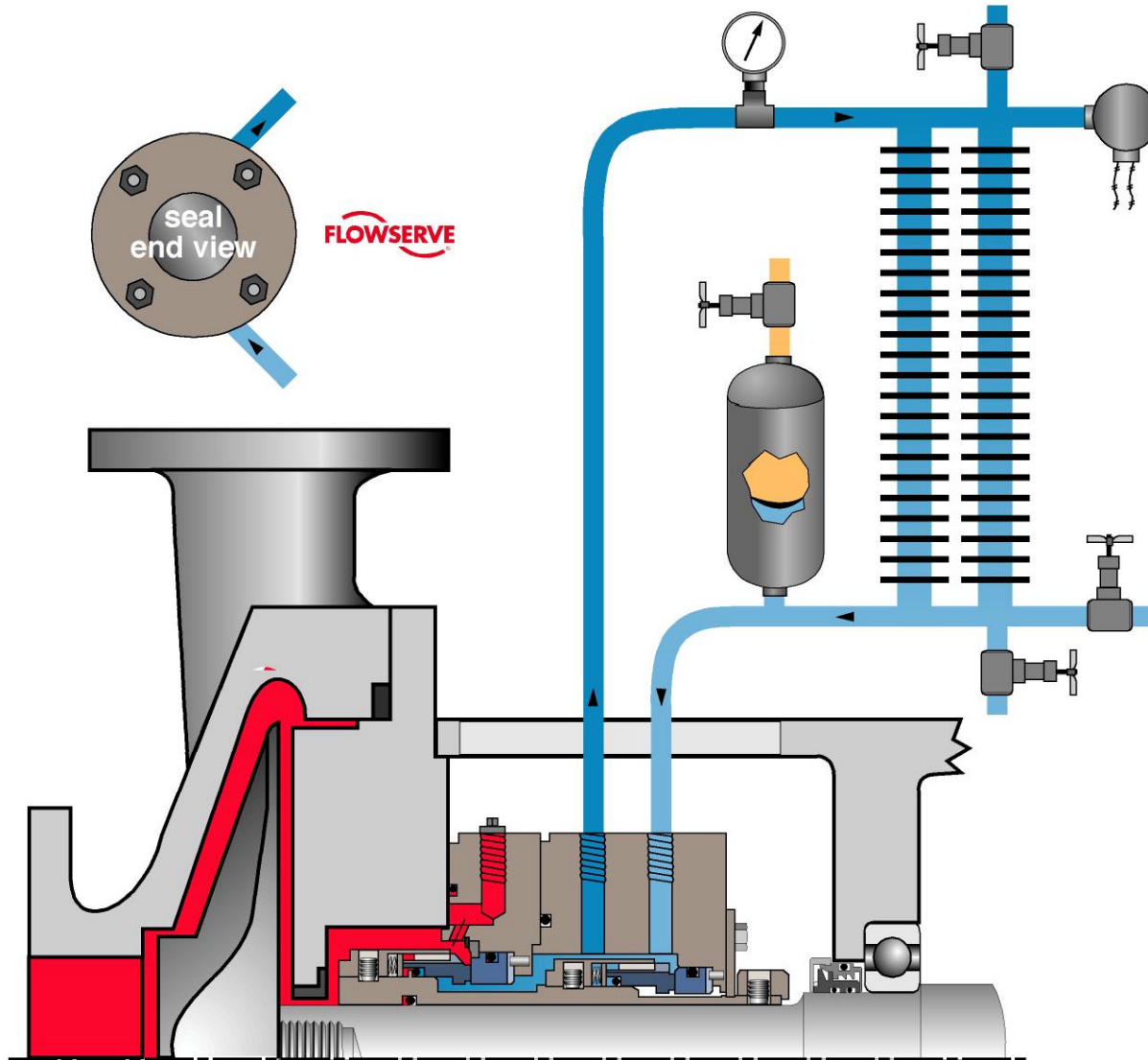




Plan 53B

Why

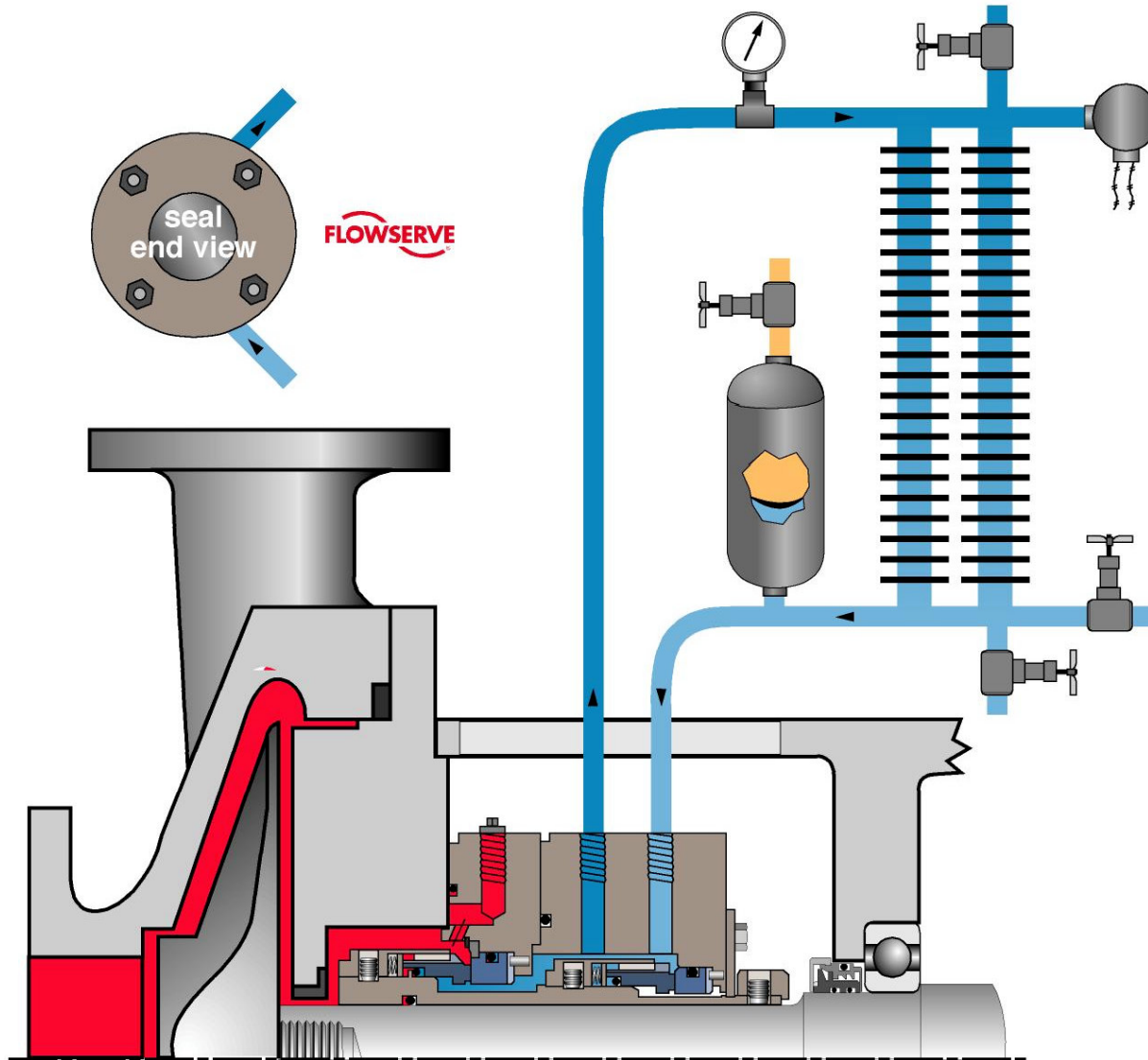
- Isolate process fluid.
- Zero process emissions.
- Higher pressure than Plan 53A.



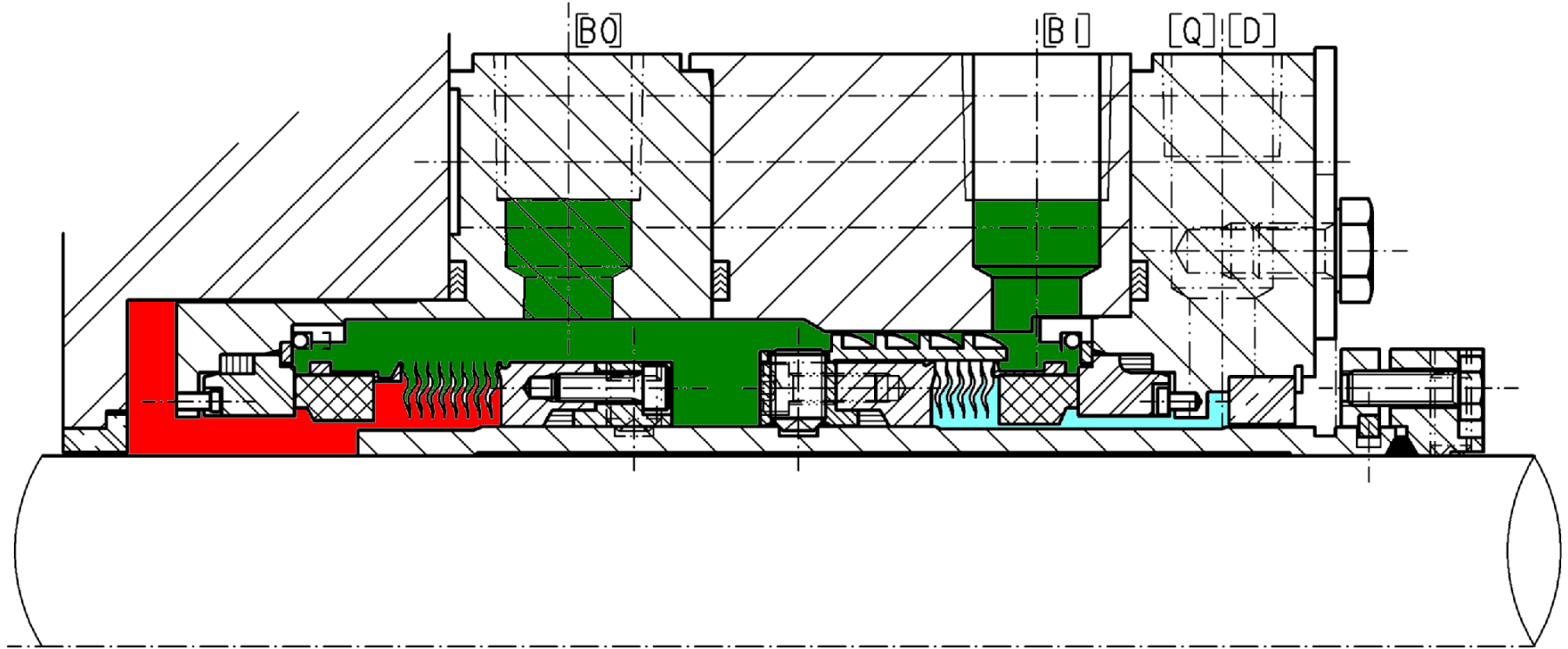
Plan 53B

Where

- Used with dual pressurized seals (“double”).
- High vapor pressure fluids, light hydrocarbons.
- Hazardous or toxic fluids.
- Heat transfer fluids.
- Dirty, abrasive or polymerizing fluids.



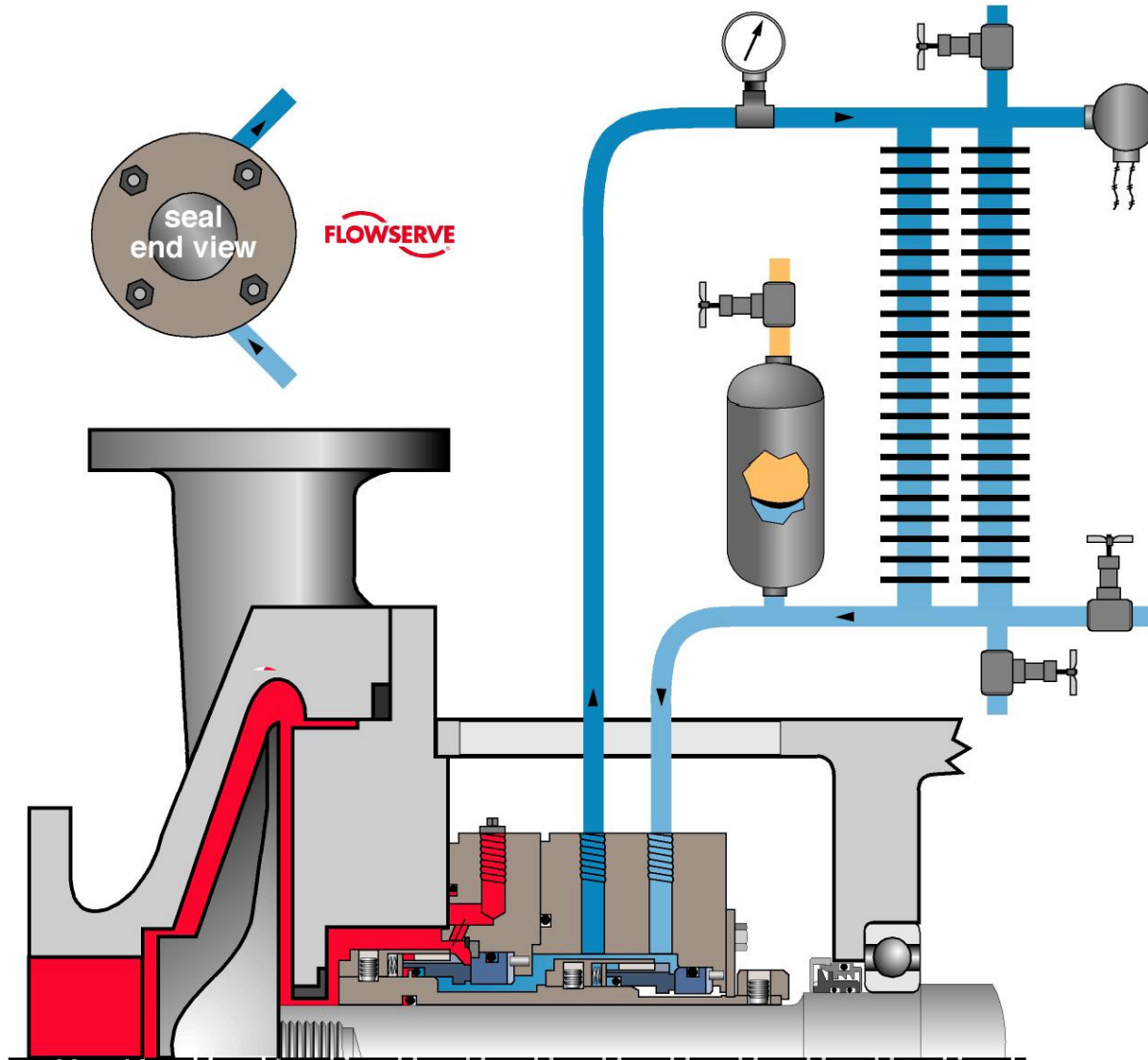
API 682 Type C Arrangement 3 3CW - BB



Plan 53B

Preventative Maintenance

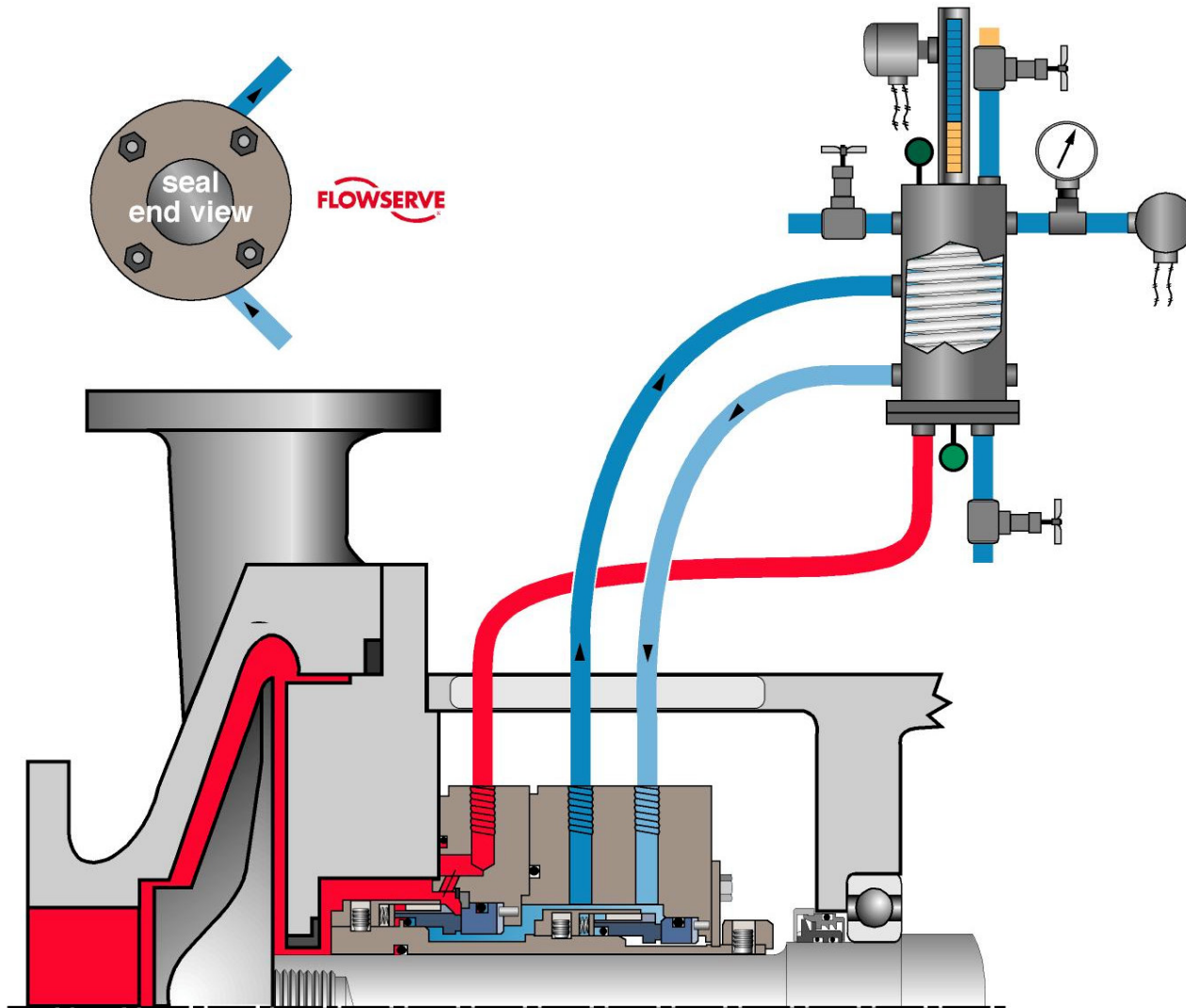
- Piping loop must be fully vented before starting.
- Accumulator must be pressurized at all times, usually by gas charge.
- Barrier fluid must be compatible with process.
- Regularly monitor barrier pressure – manually add barrier fluid when pressure decays.

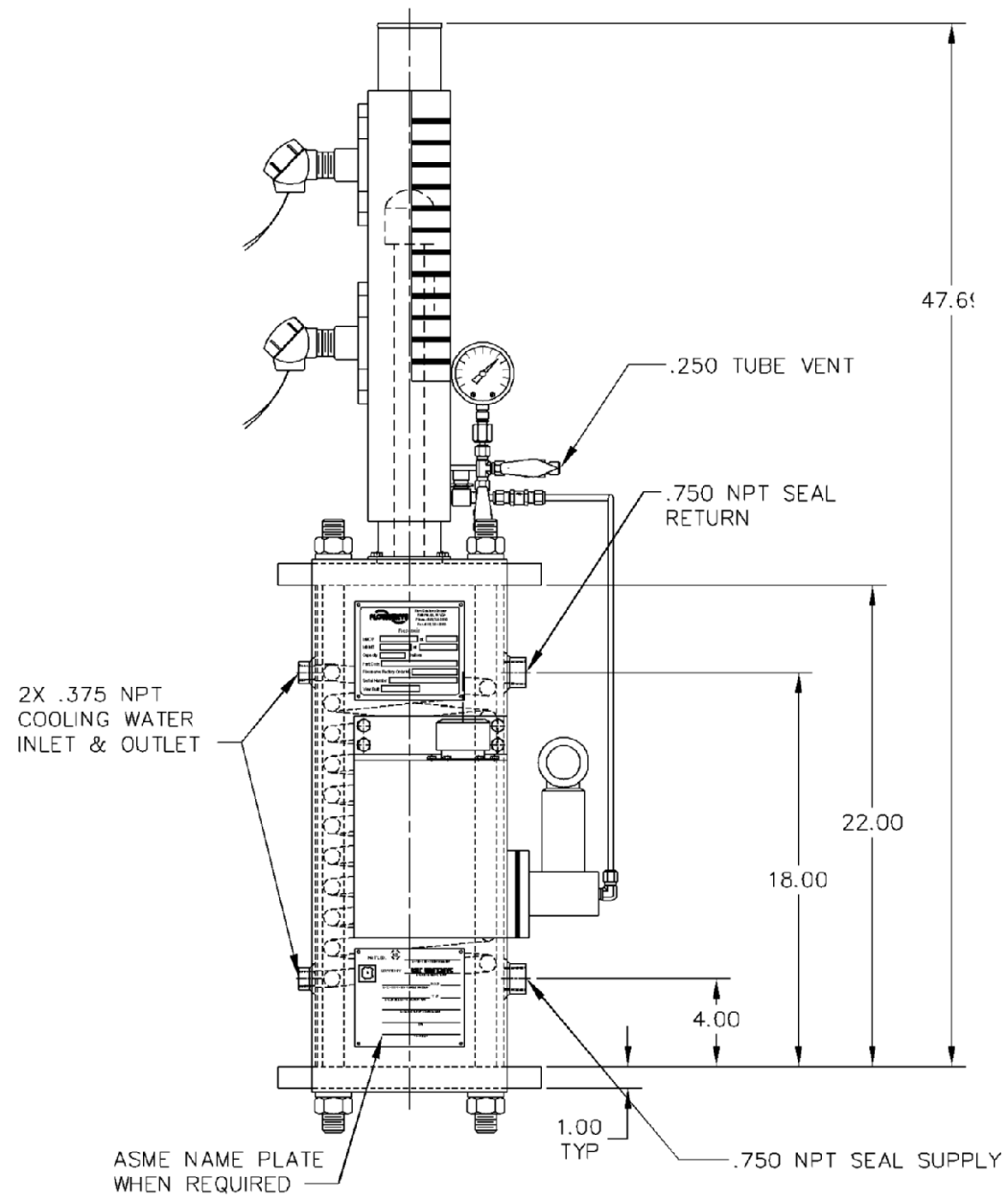


Plan 53C

What

- Pressurized barrier fluid circulation with a piston accumulator.
- Fluid is circulated by a pumping ring in the dual seal assembly.

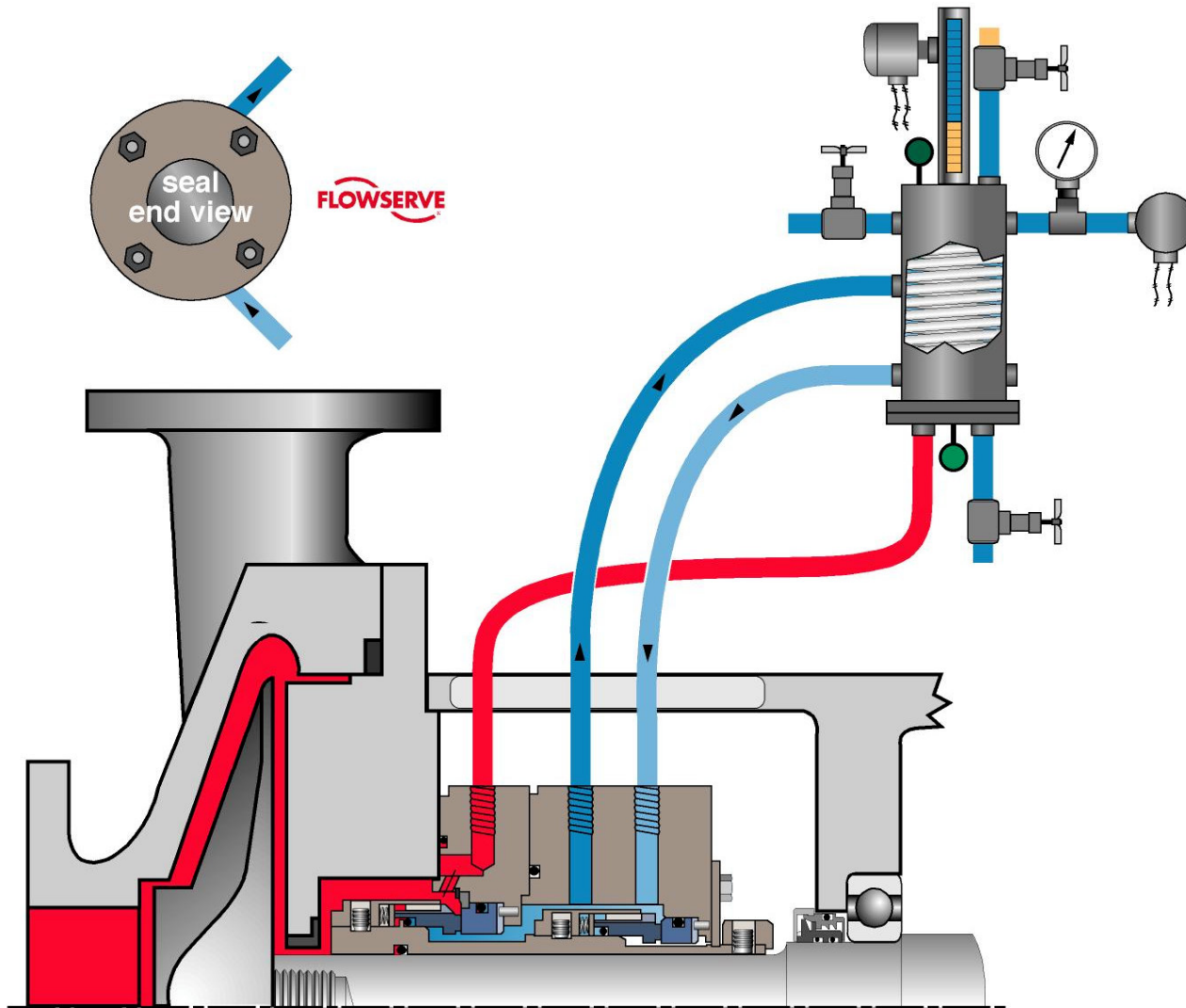




Plan 53C

Why

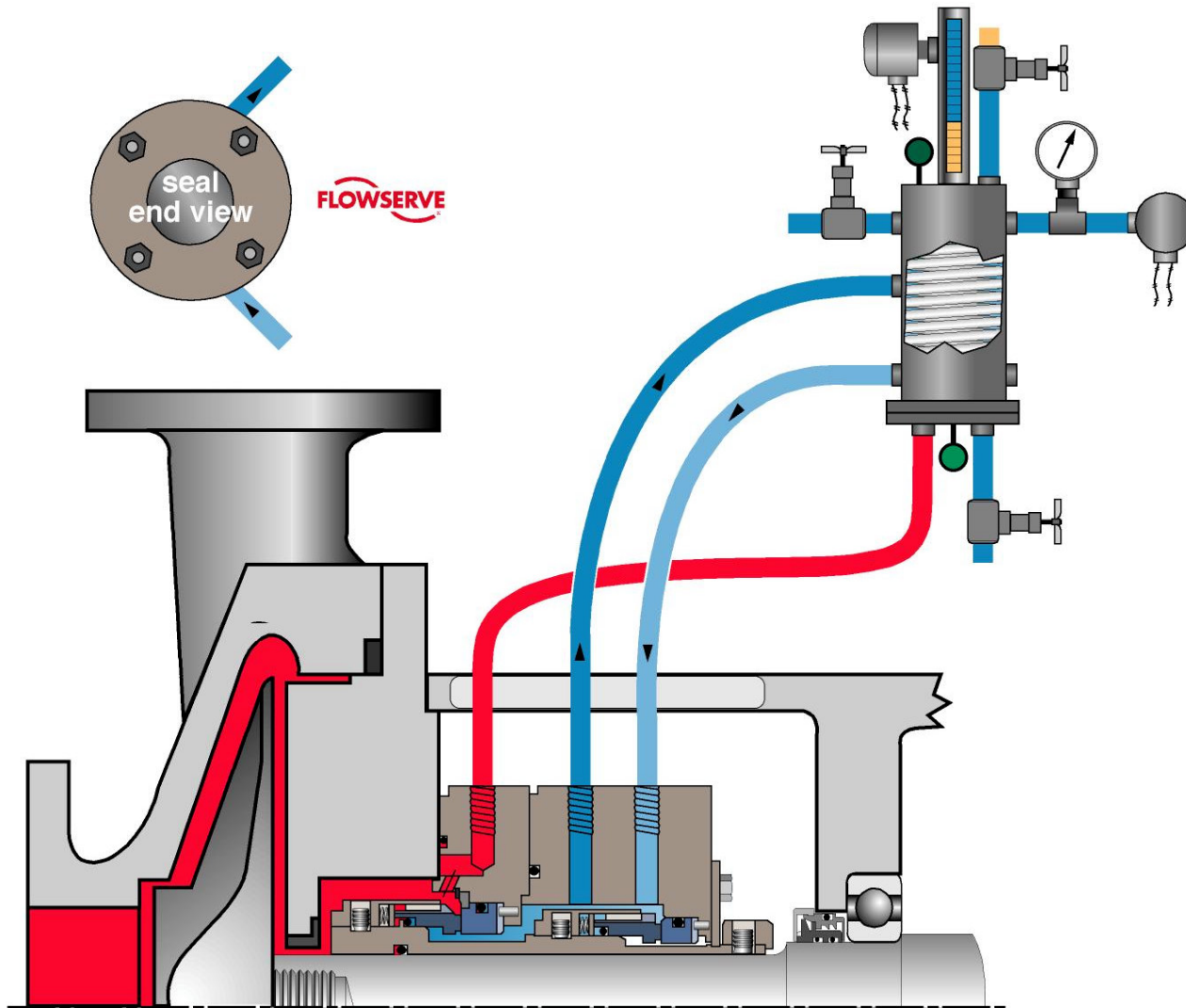
- Isolate process fluid.
- Zero process emissions.
- Higher pressure than Plan 53A.
- Dynamic tracking of system pressure.



Plan 53C

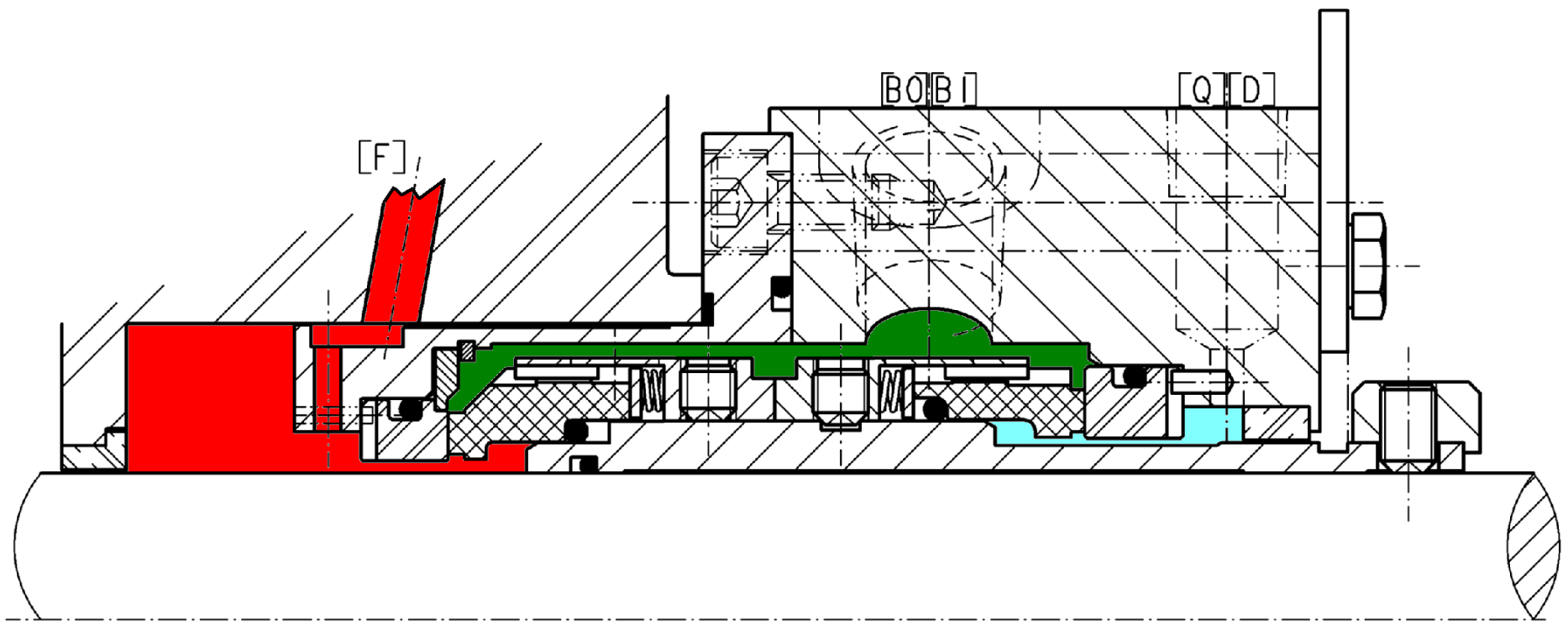
Where

- Used with dual pressurized seals (“double”).
- High vapor pressure fluids, light hydrocarbons.
- Hazardous or toxic fluids.
- Heat transfer fluids.



API 682 Type A Arrangement 3

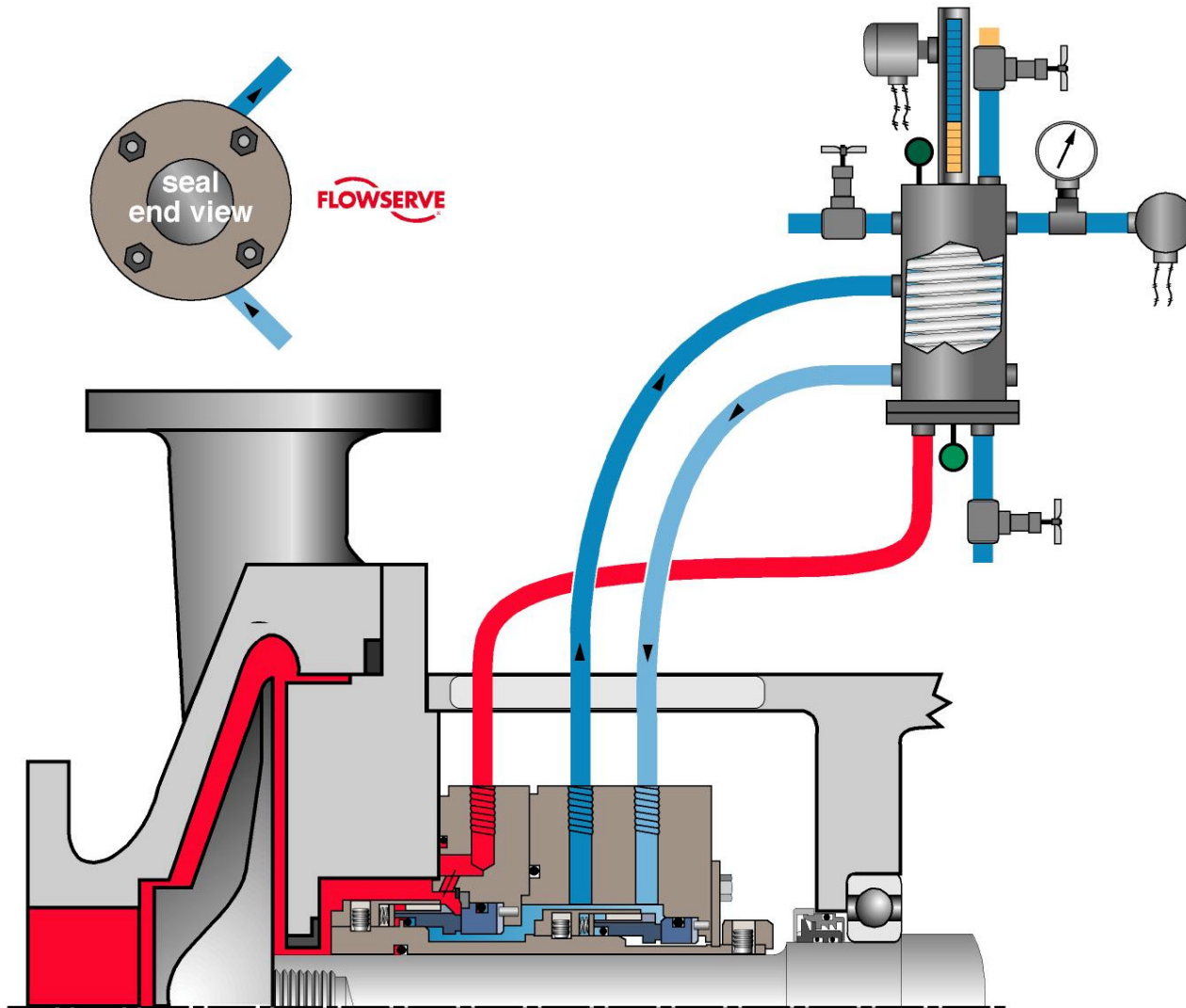
3CW - BB



Plan 53C

Preventative Maintenance

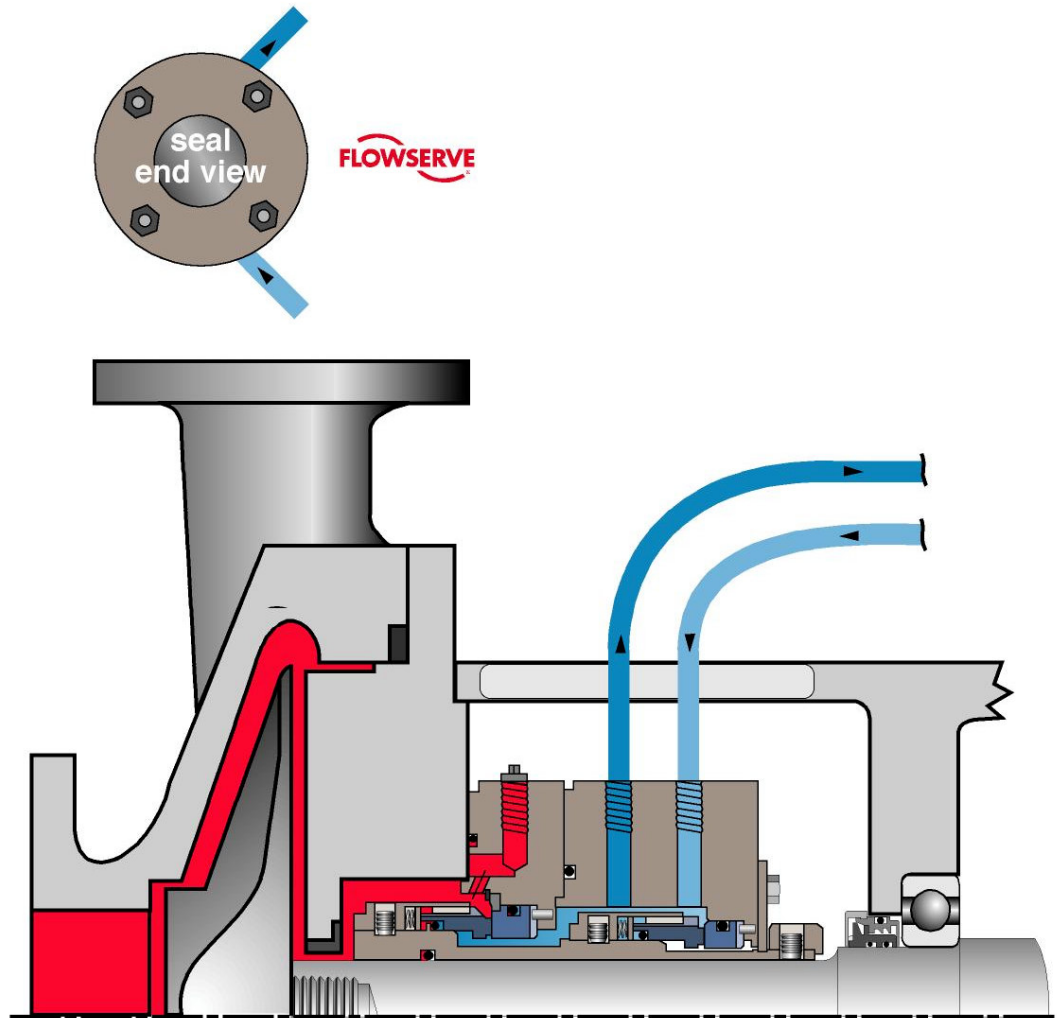
- Piping loop must be fully vented before starting.
- Reference line must tolerate process contamination without plugging.
- Barrier fluid must be compatible with process.
- Reservoir level gage indicates both inboard and outboard seal leakage.

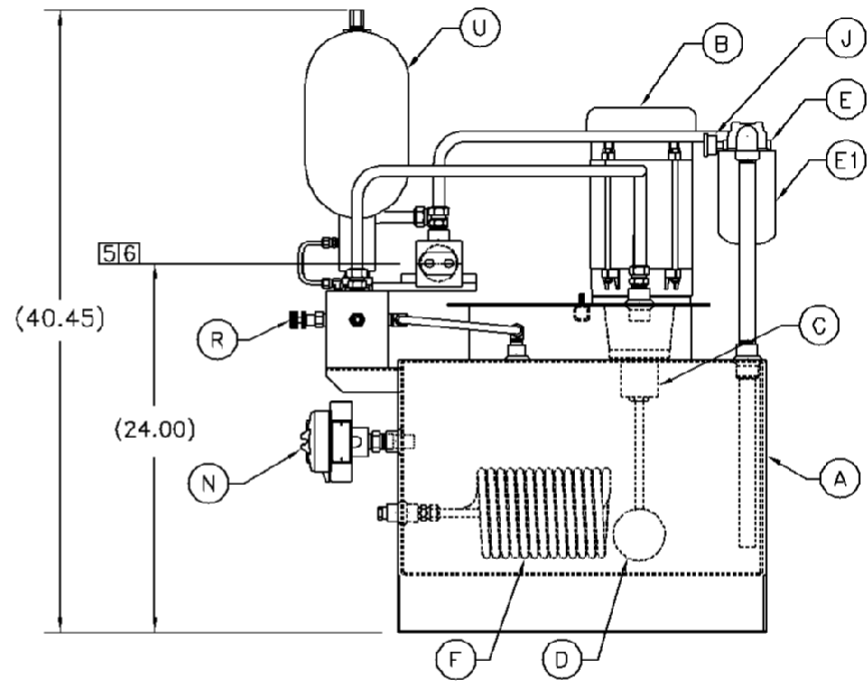
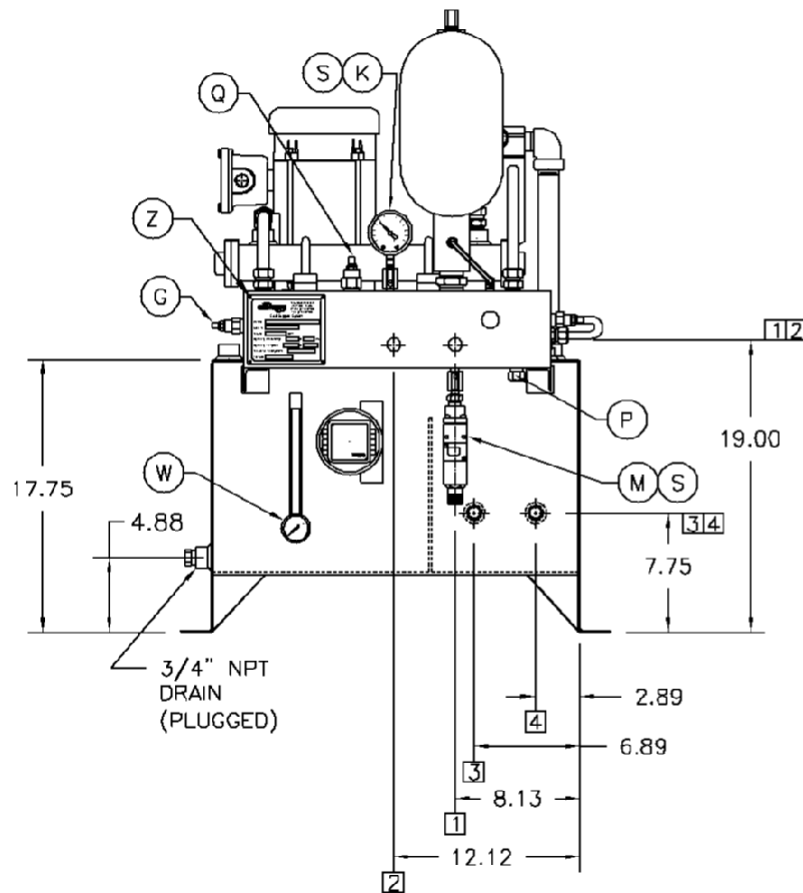


Plan 54

What

- Pressurized barrier fluid circulation by an external system.

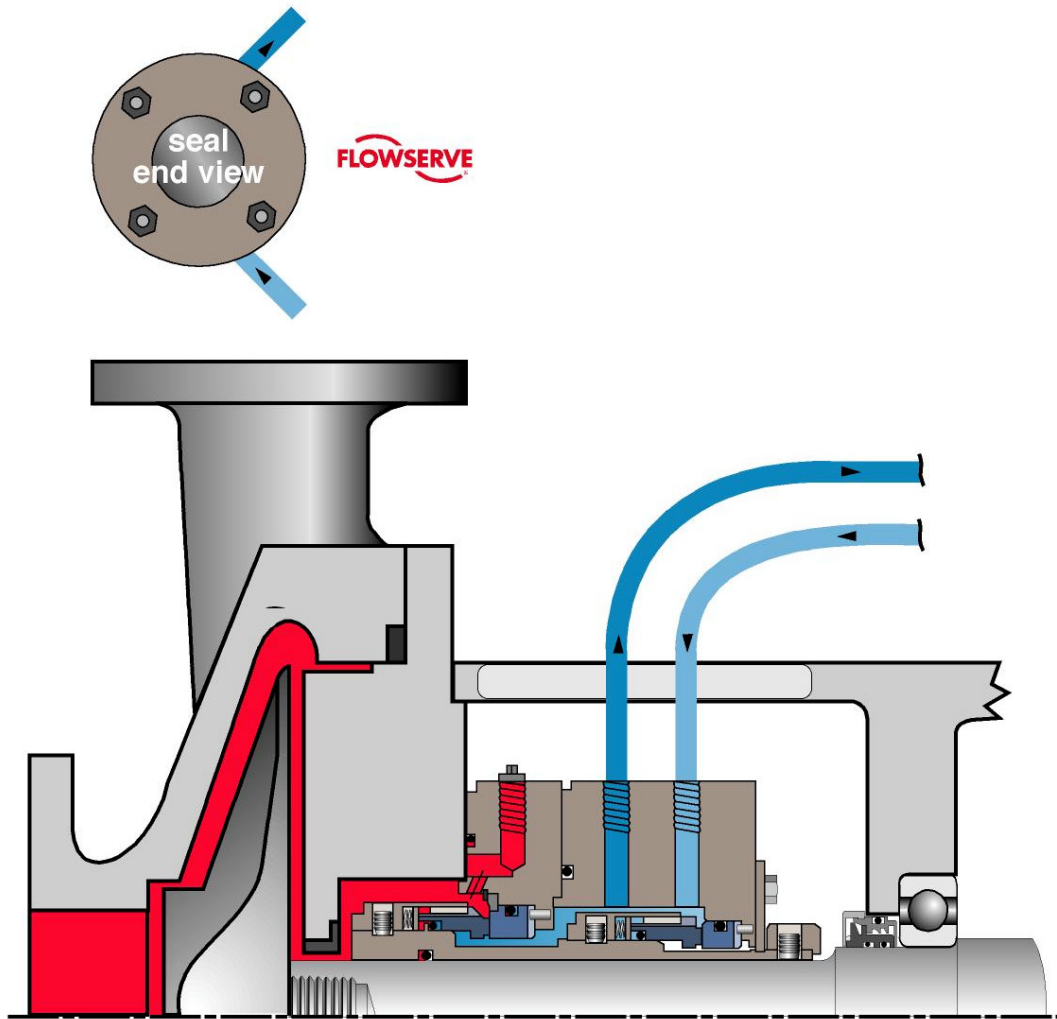




Plan 54

Why

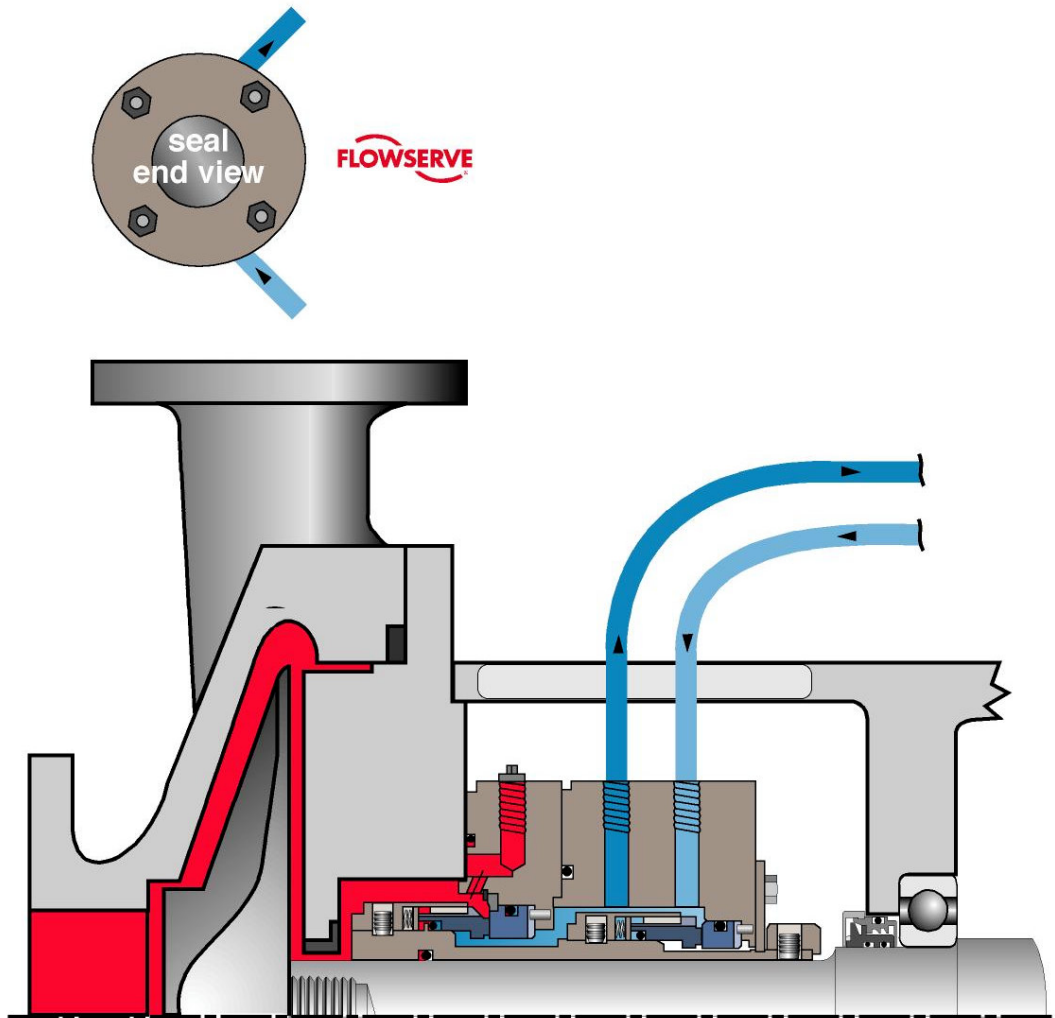
- Isolate process fluid.
- Zero process emissions.
- Seal cannot induce circulation.



Plan 54

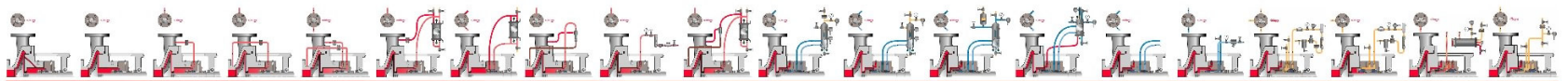
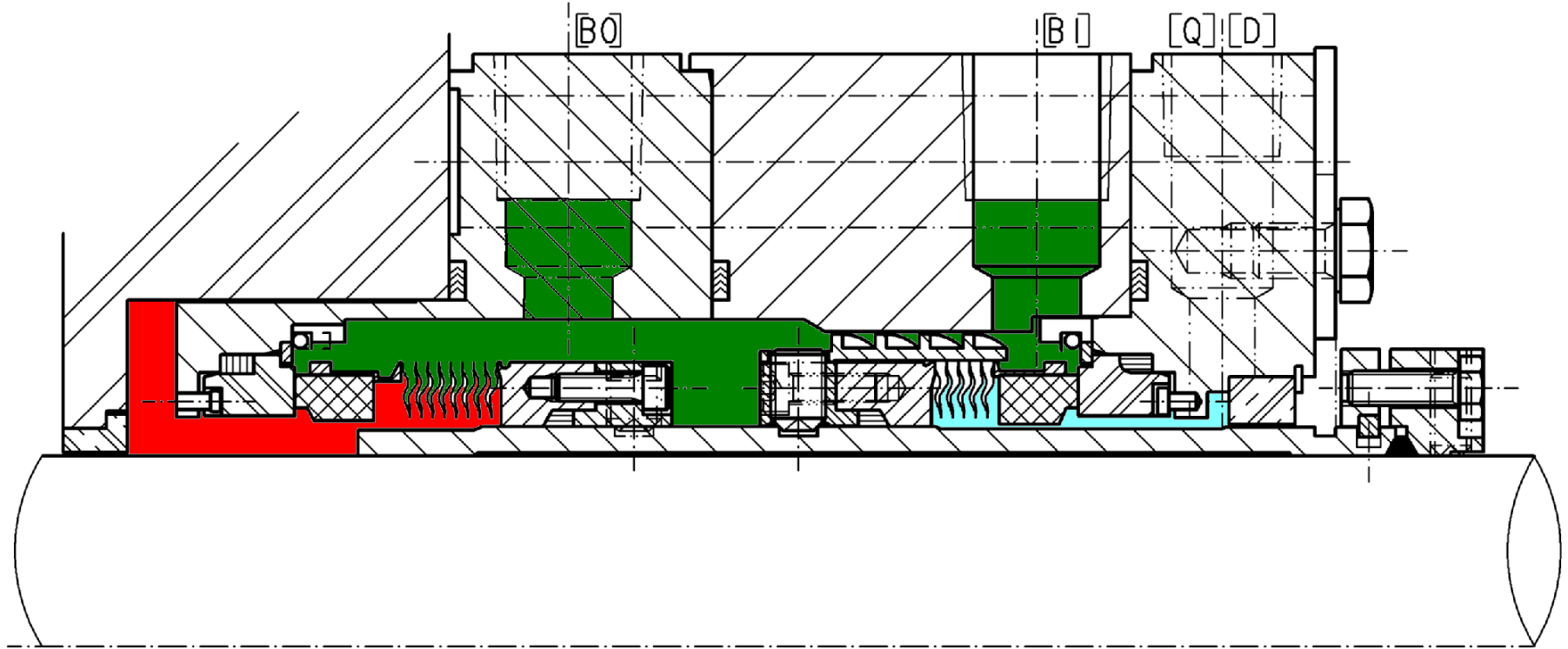
Where

- Used with dual pressurized seals (“double”).
- High vapor pressure fluids, light hydrocarbons.
- Hazardous or toxic fluids.
- Heat transfer fluids.
- Dirty, abrasive, or polymerizing fluids.
- Mixers or agitators.



API 682 Type C Arrangement 3

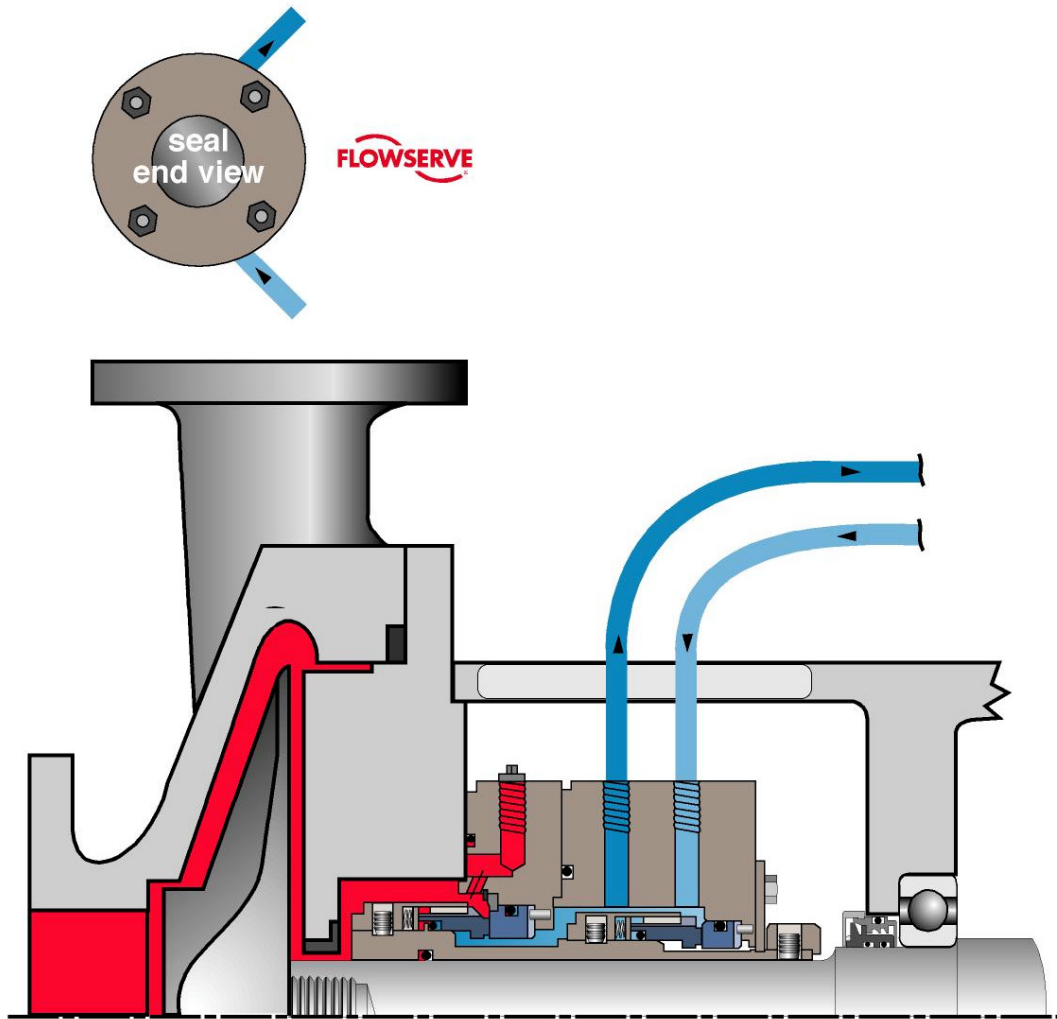
3CW - BB



Plan 54

Preventative Maintenance

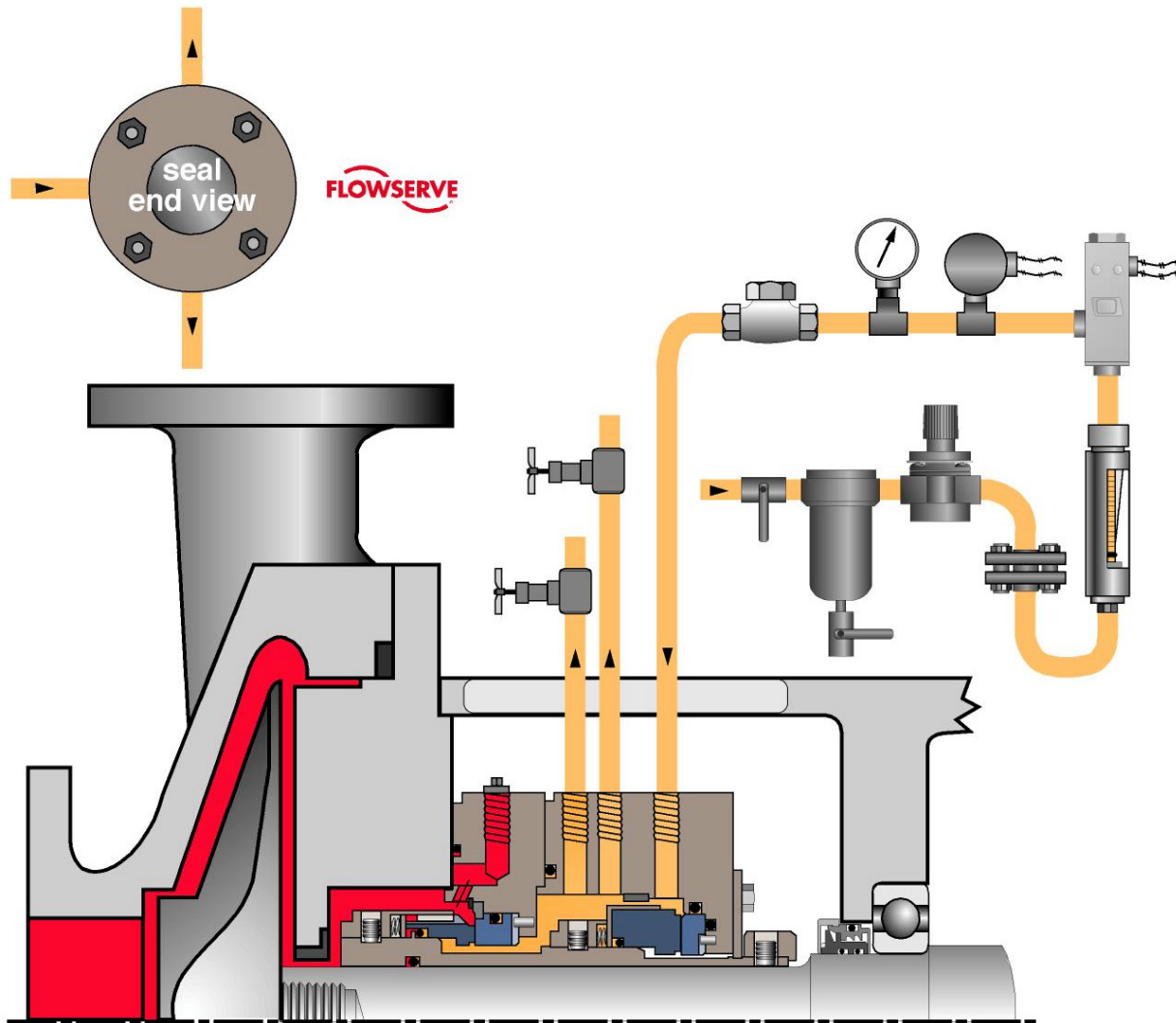
- Piping loop must be fully vented before starting.
- Circulating system must be pressurized and energized at all times.
- Barrier fluid must be compatible with process.
- Circulation system level gage indicates both inboard and outboard seal leakage.

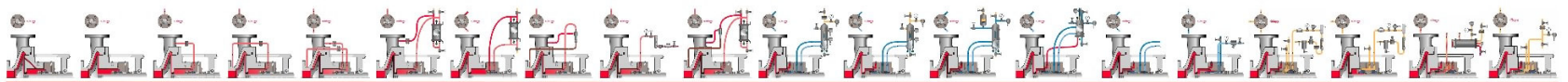


Plan 72

What

- Unpressurized buffer gas control system.
- Containment seal support typically with nitrogen buffer gas.

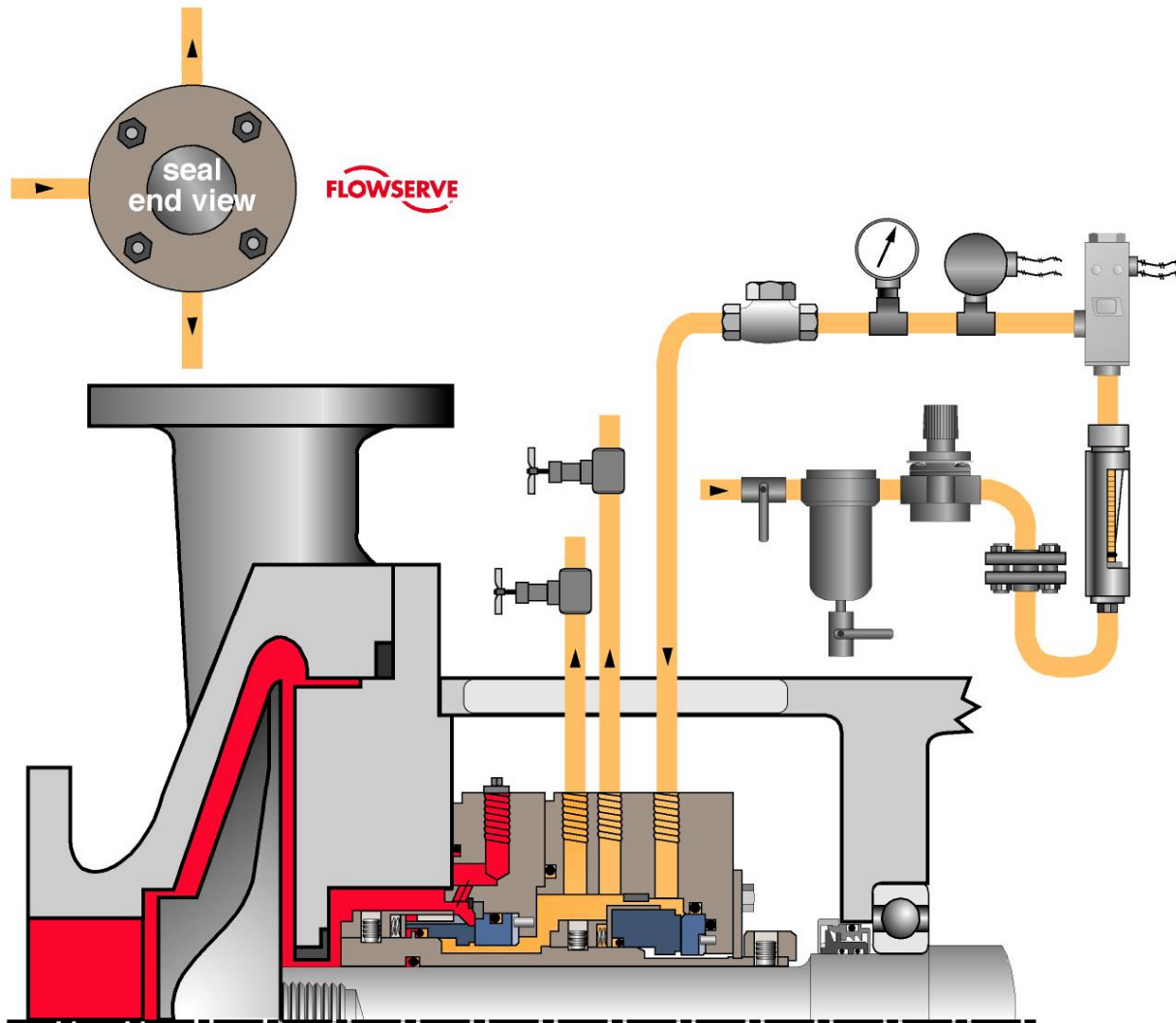




Plan 72

Why

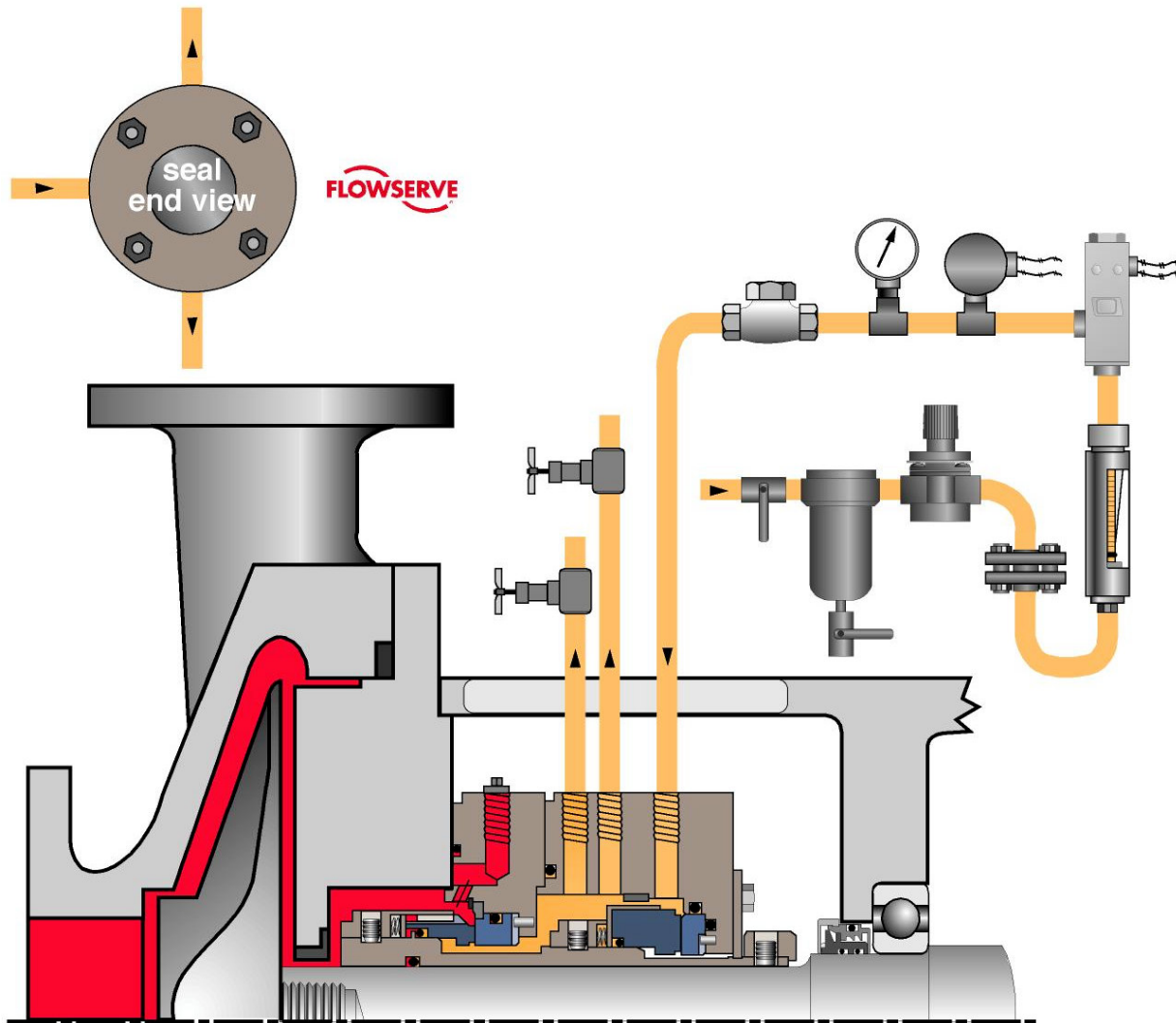
- Zero to very low process emissions.
- Safety backup to primary seal.



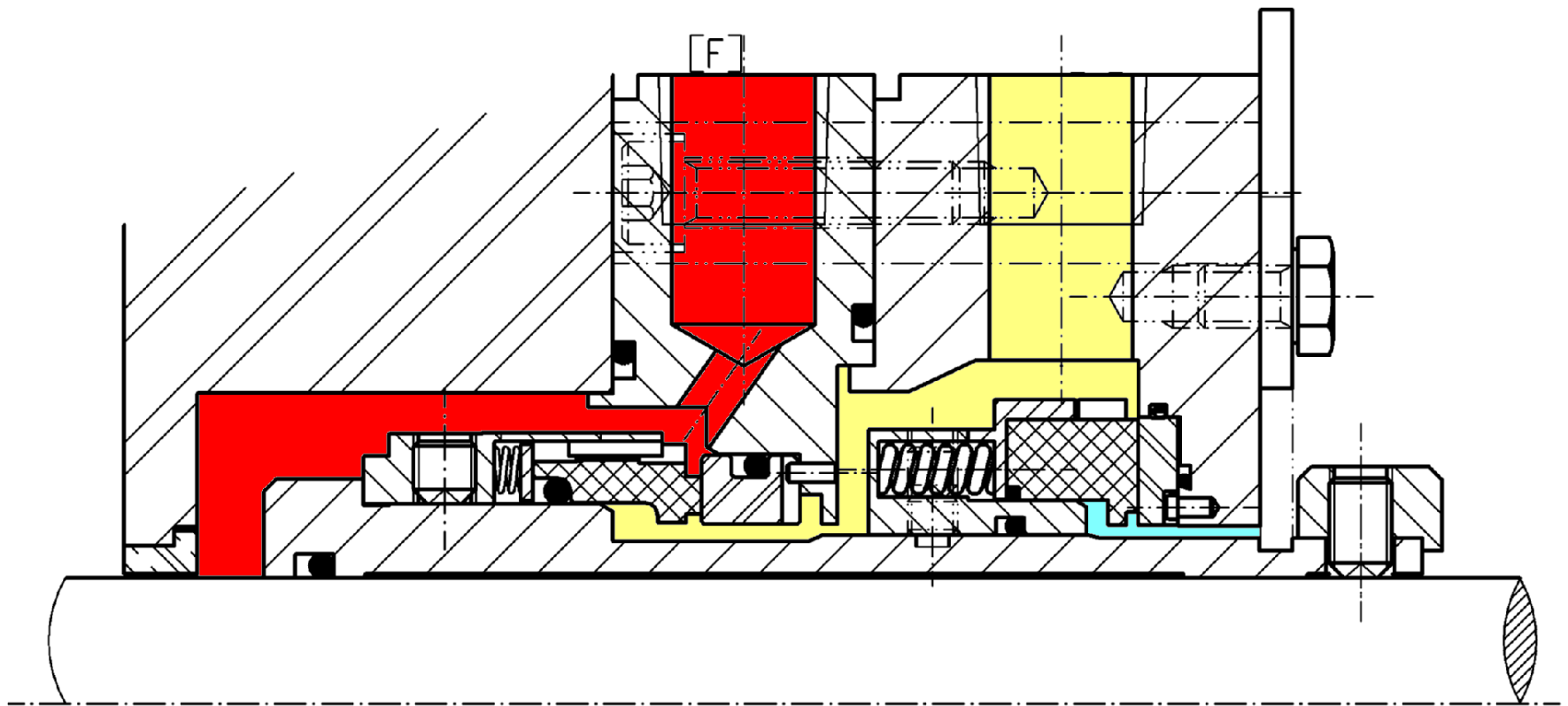
Plan 72

Where

- Used with dual unpressurized containment seals (“tandem”).
- High vapor pressure fluids, light hydrocarbons.
- Hazardous or toxic fluids.
- Clean, non-polymerizing, non-oxidizing fluids.
- Used in combination with Plan 75 and/or Plan 76.



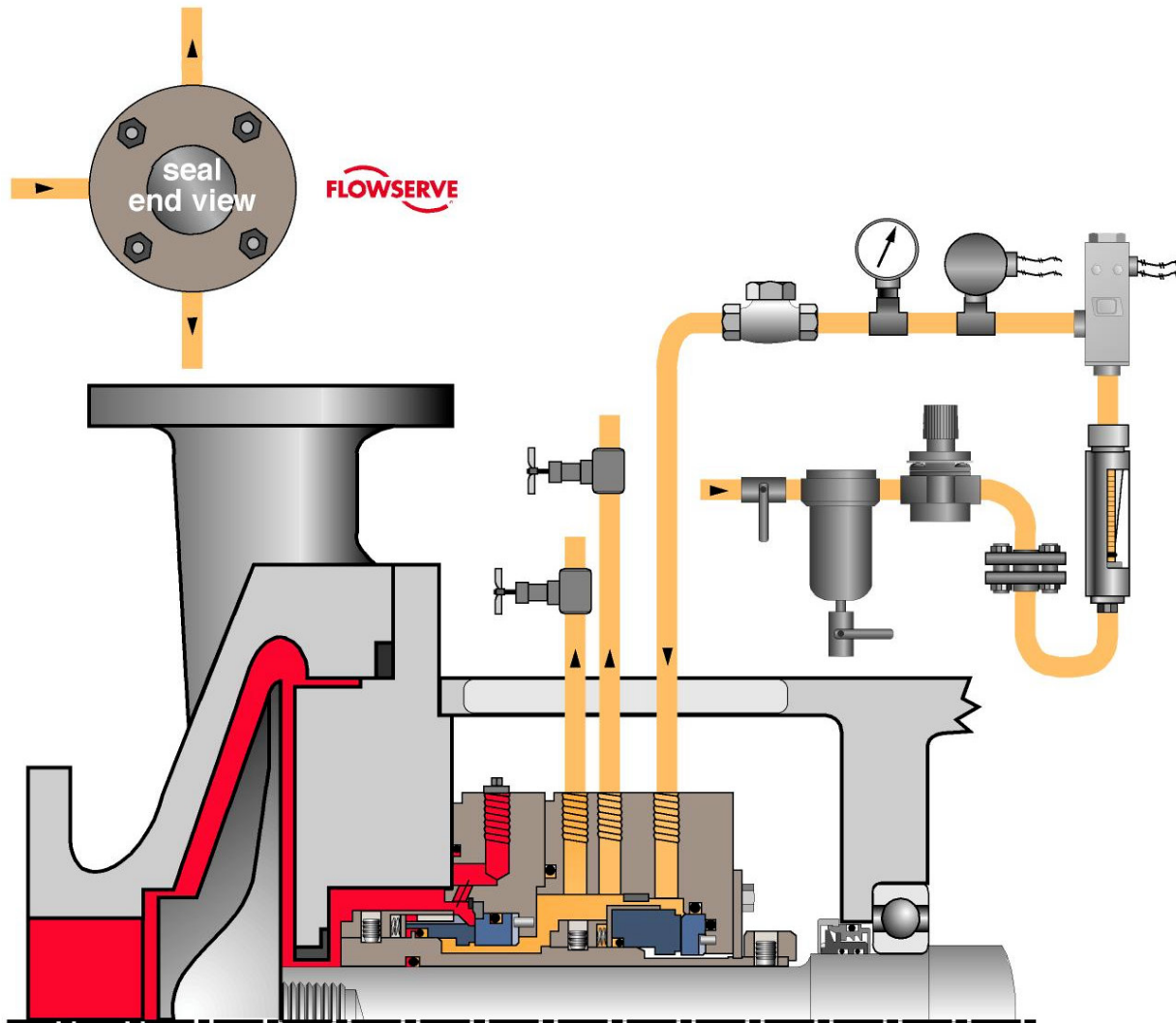
API 682 Type A with Containment 2CW - CS



Plan 72

Preventative Maintenance

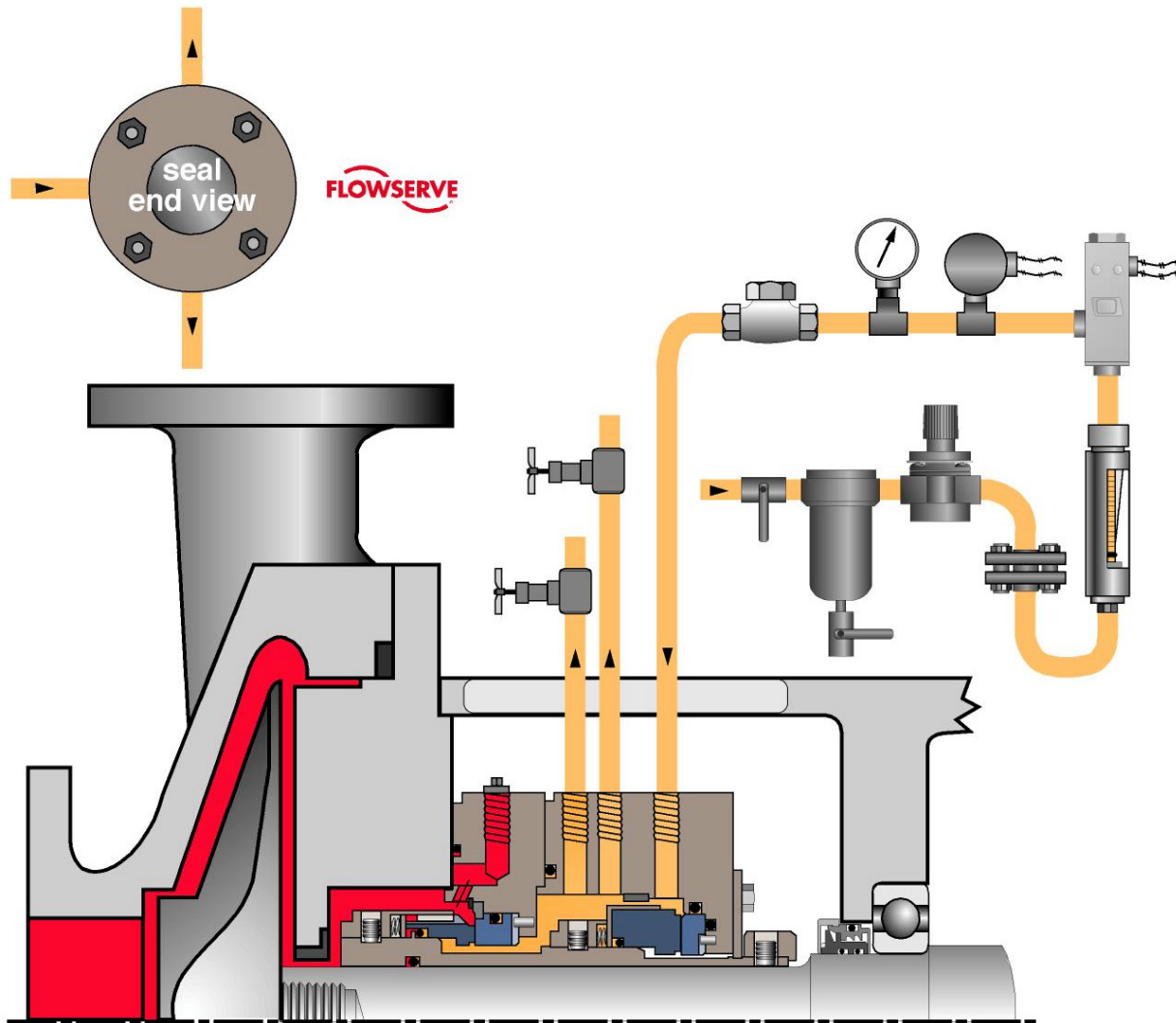
- Clean, reliable, low pressure gas must be supplied to seal at all times.
- Bottled gas supply is not recommended except as part of an emergency backup system.
- Primary seal leakage is indicated by pressure in the vent line.



Plan 72

Preventative Maintenance (continued)

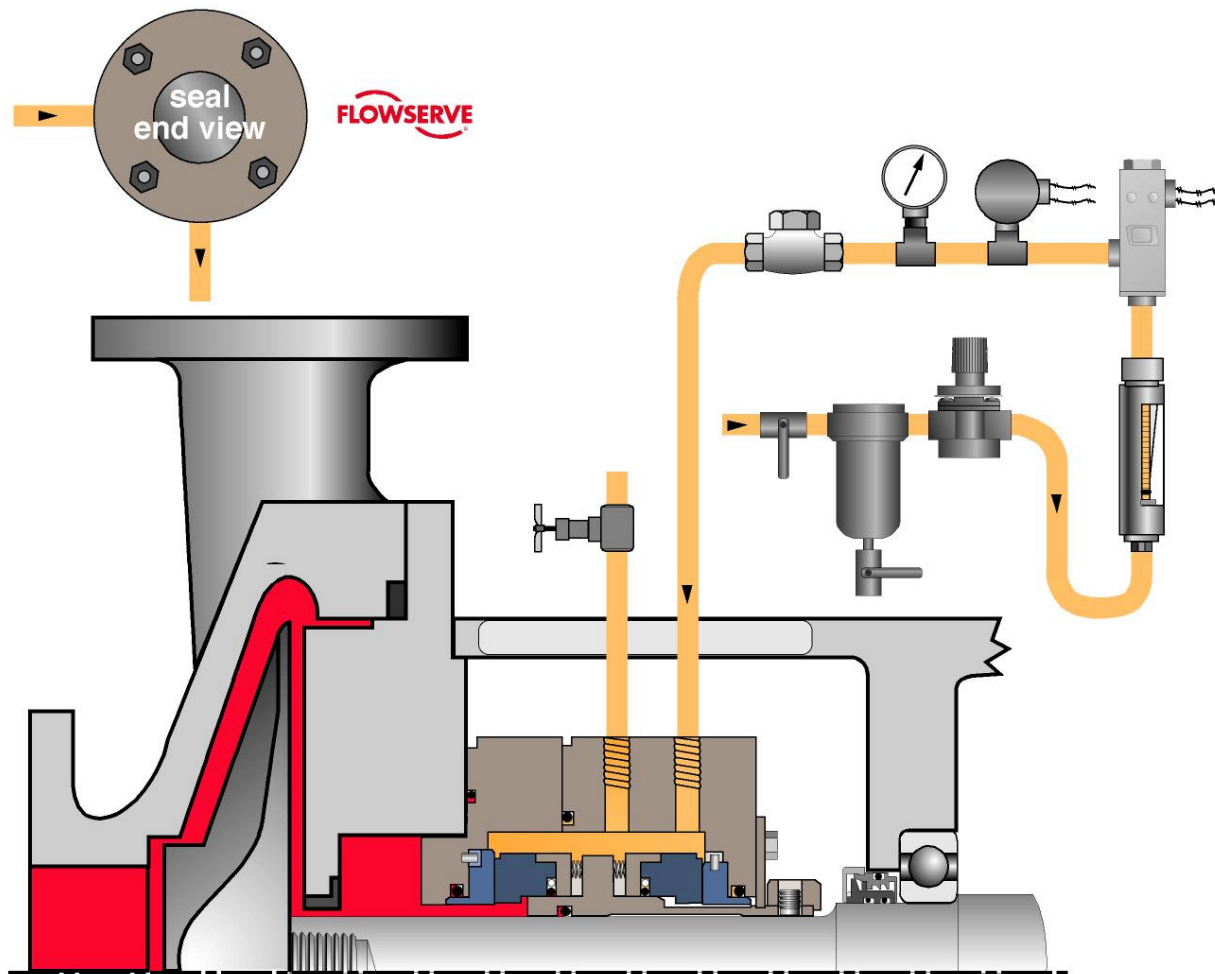
- Vent or drain are usually connected to low pressure vapor recovery/flare system.

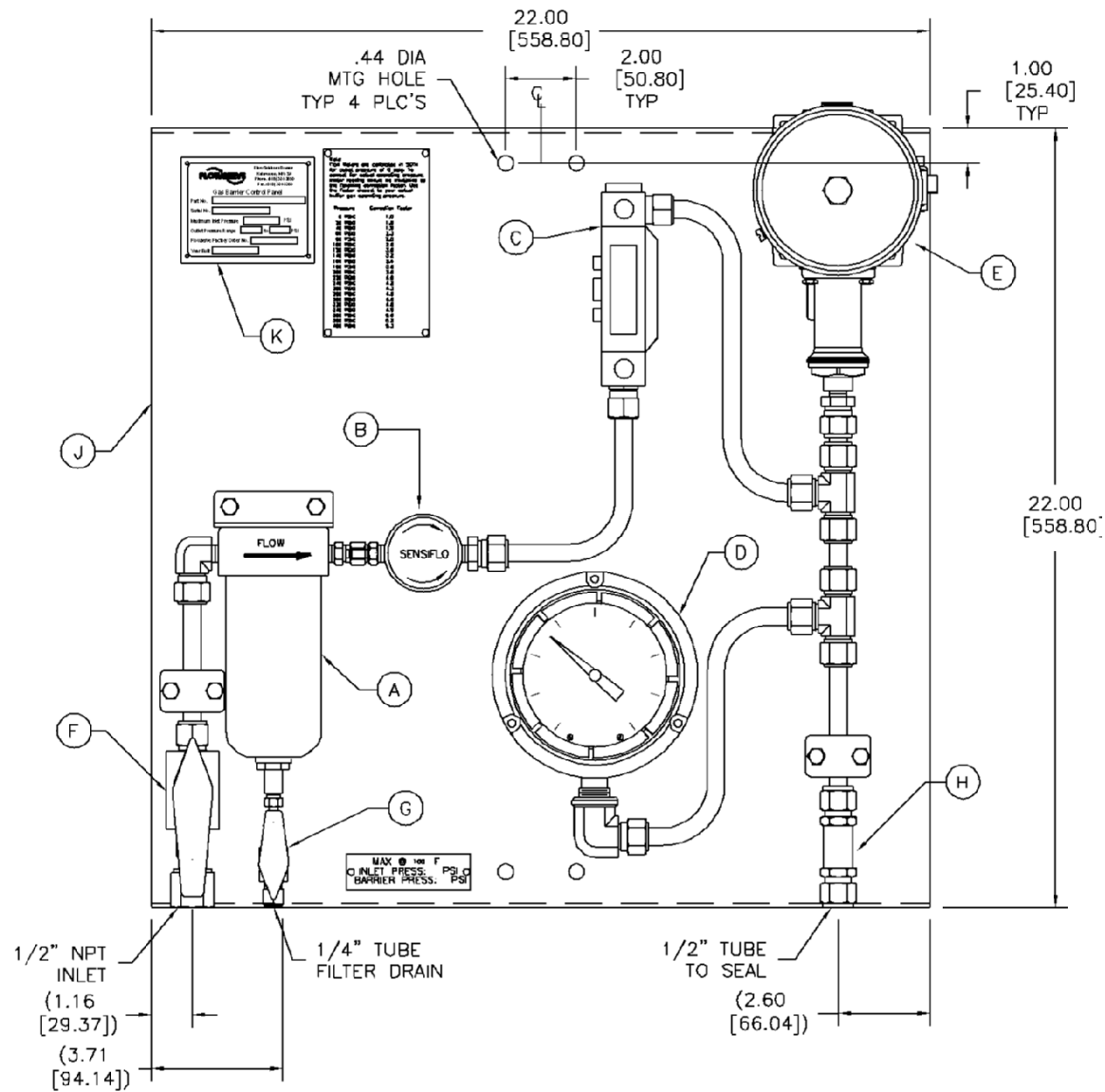


Plan 74

What

- Pressurized barrier gas control system.
- Gas seal support typically with nitrogen barrier gas.

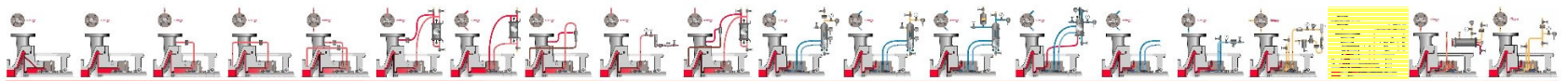
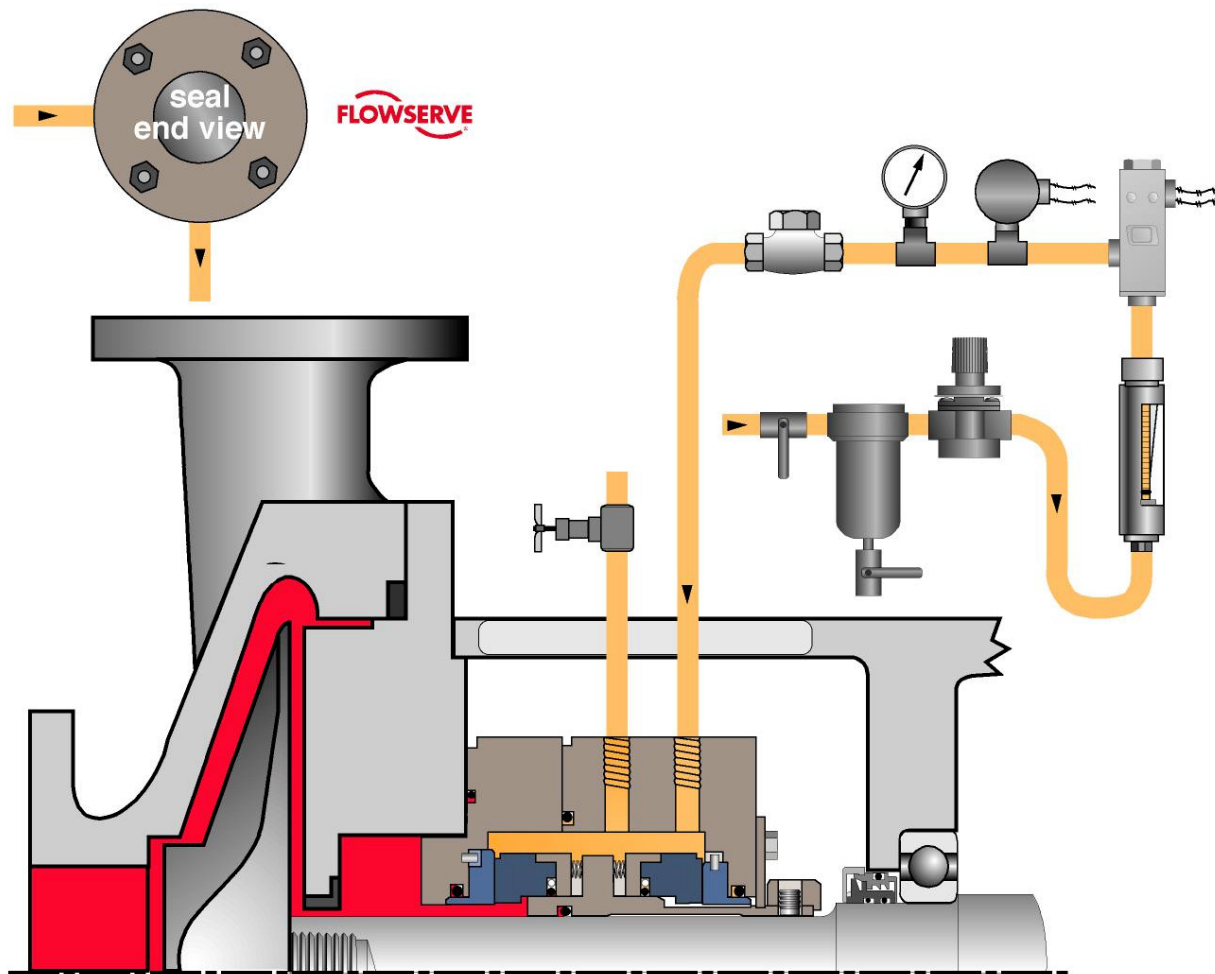




Plan 74

Why

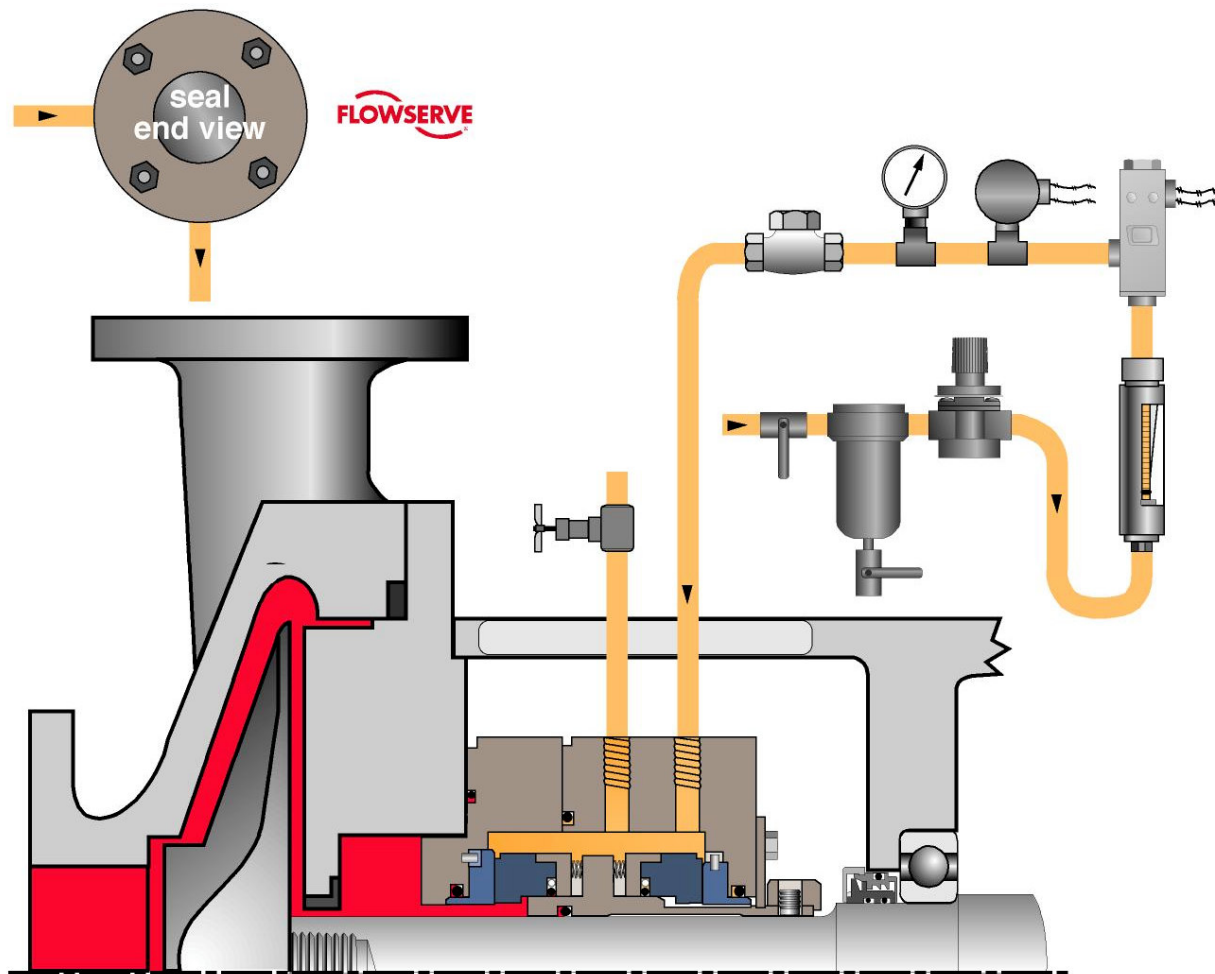
- Isolate process fluid.
- Zero process emissions.



Plan 74

Where

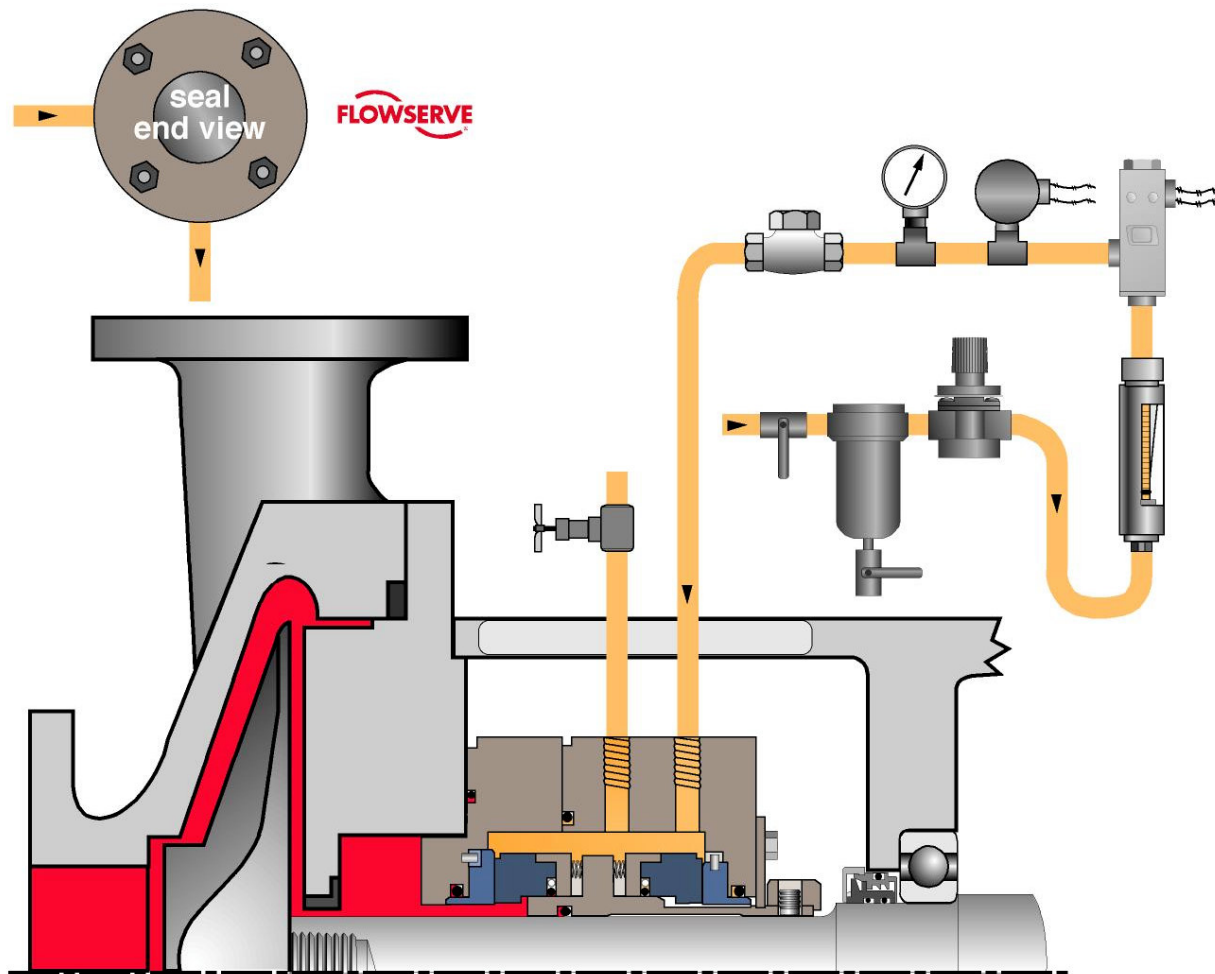
- Used with dual pressurized gas seals (“double”).
- High vapor pressure fluids, light hydrocarbons.
- Hazardous or toxic fluids.
- Services that do not tolerate barrier fluids.
- Clean, non-polymerizing fluids.
- Moderate temperature fluids.



Plan 74

Preventative Maintenance

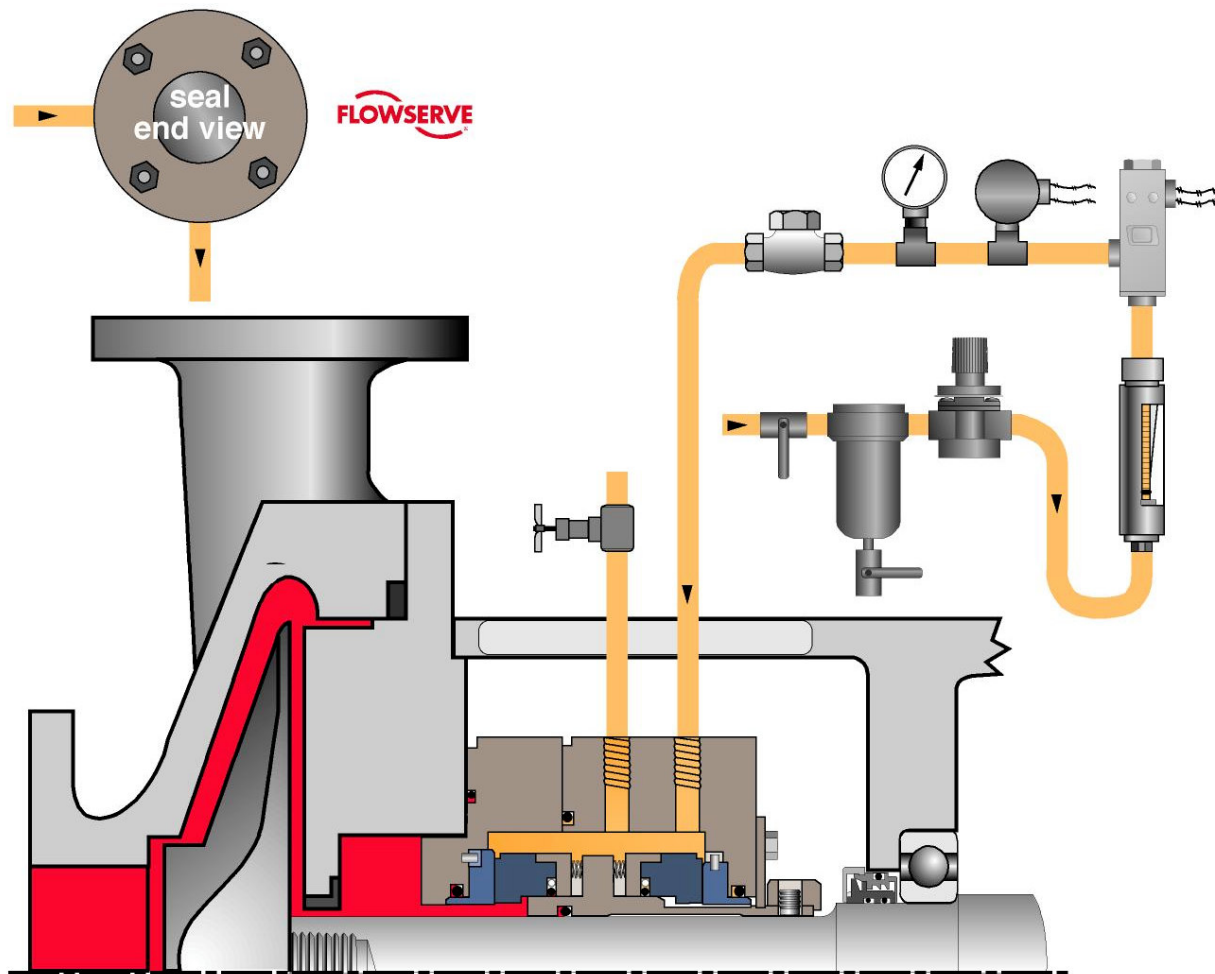
- Clean, reliable, pressurized gas must be supplied to seal at all times.
- Barrier pressure is typically at least 25 psi (1.75 bar) above seal chamber pressure.
- Flow meter indicates both inboard and outboard seal leakage.



Plan 74

Preventative Maintenance (continued)

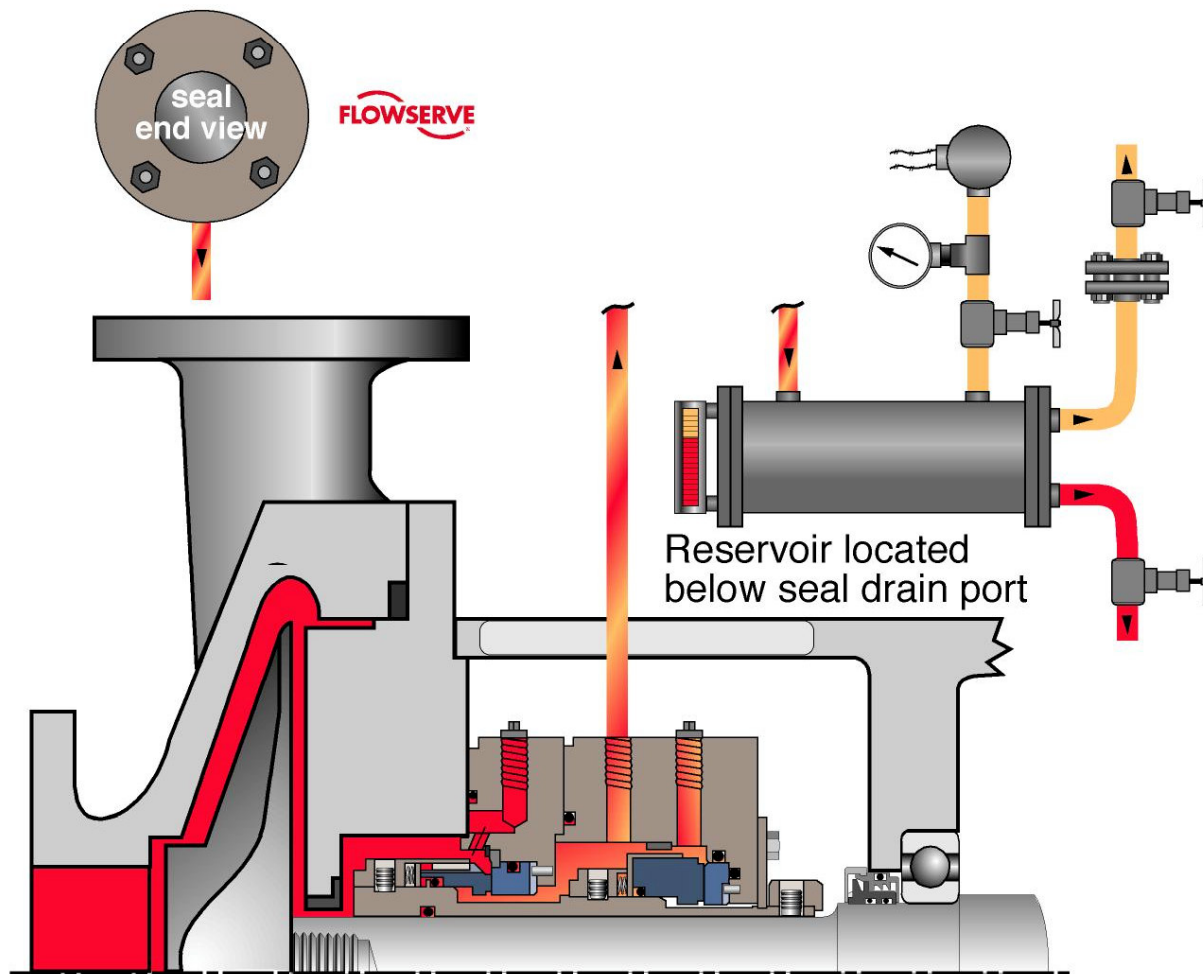
- Bottled gas supply is not recommended except as part of an emergency backup system.

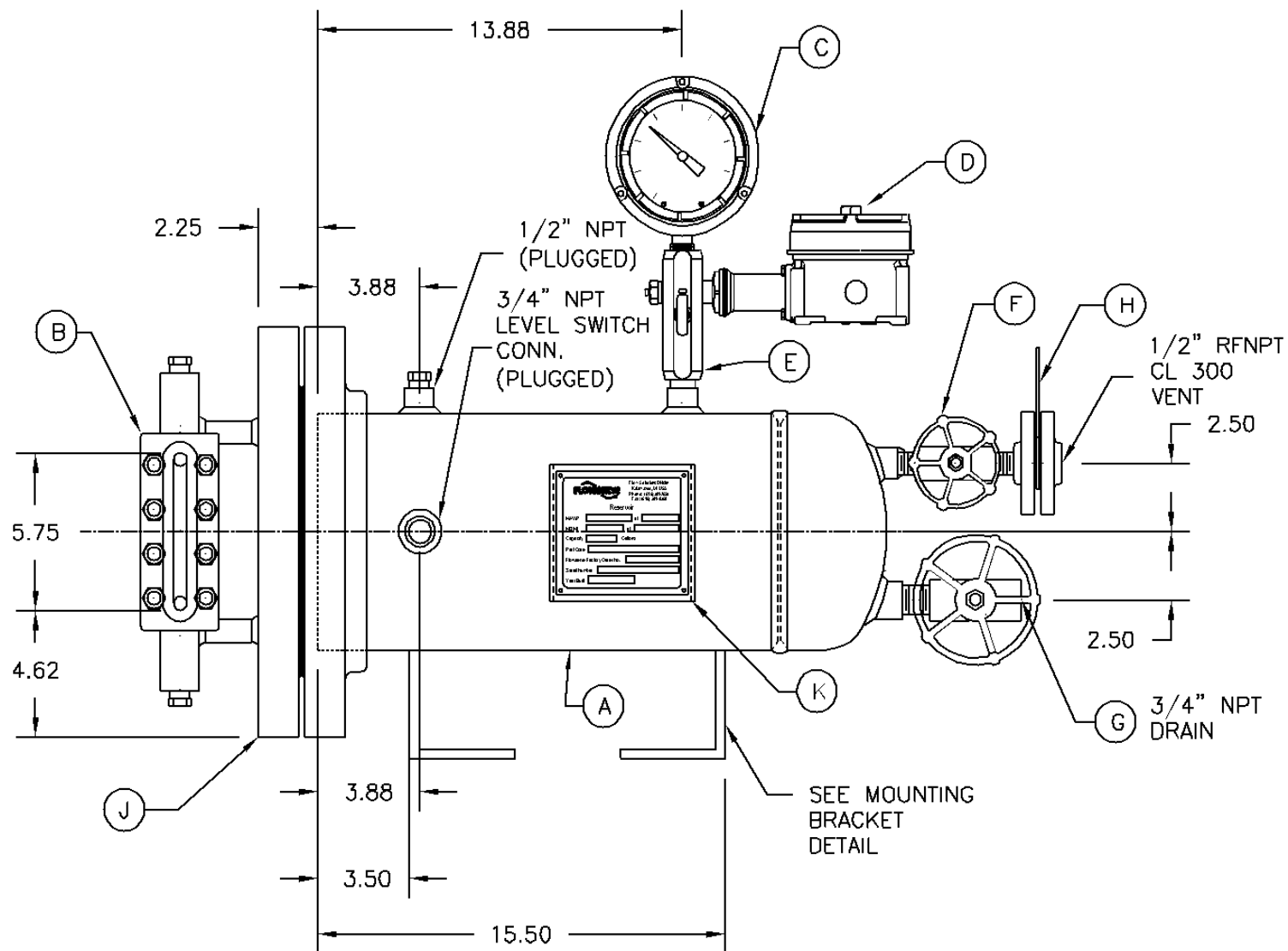


Plan 75

What

- Drain from containment seal cavity to liquid collector and vapor recovery.

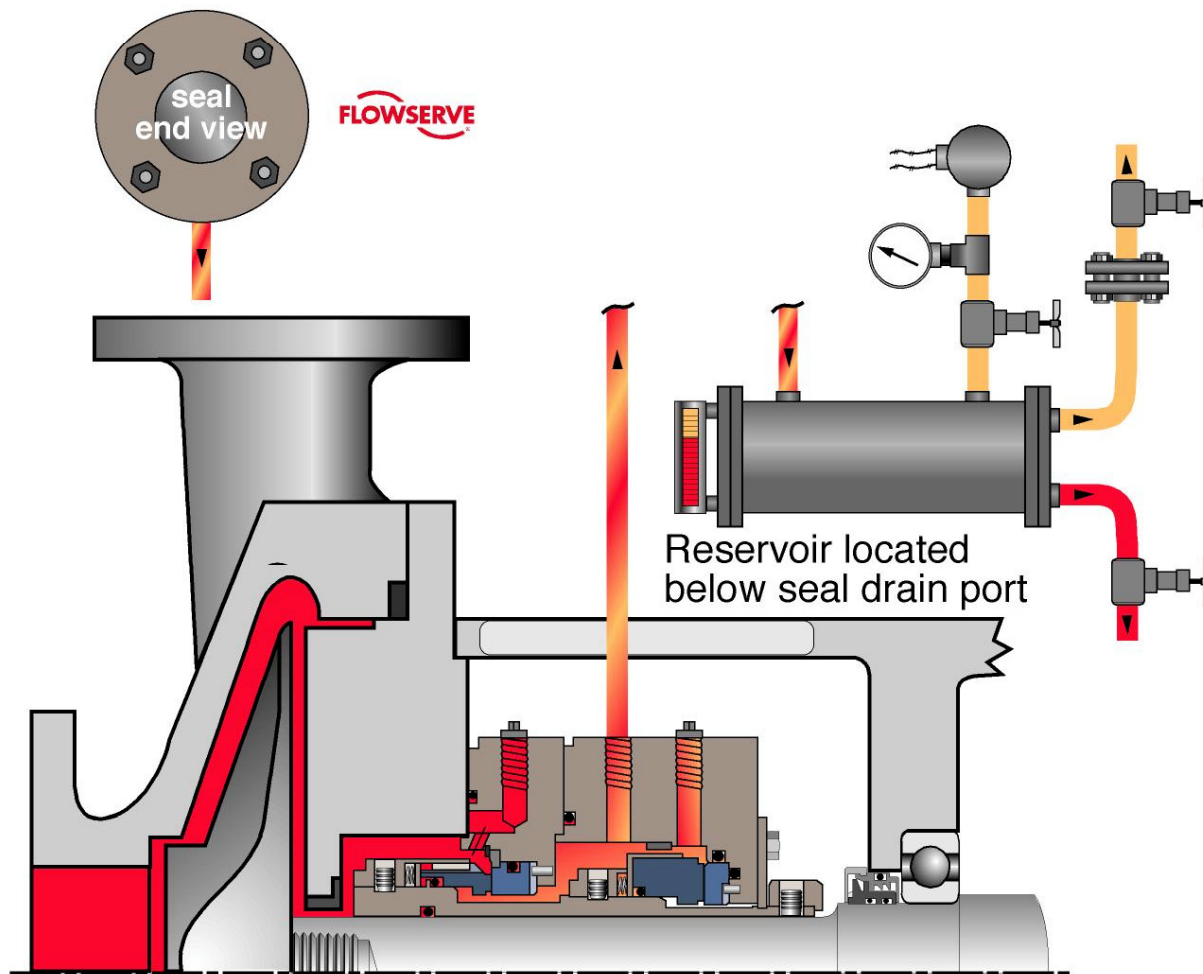




Plan 75

Why

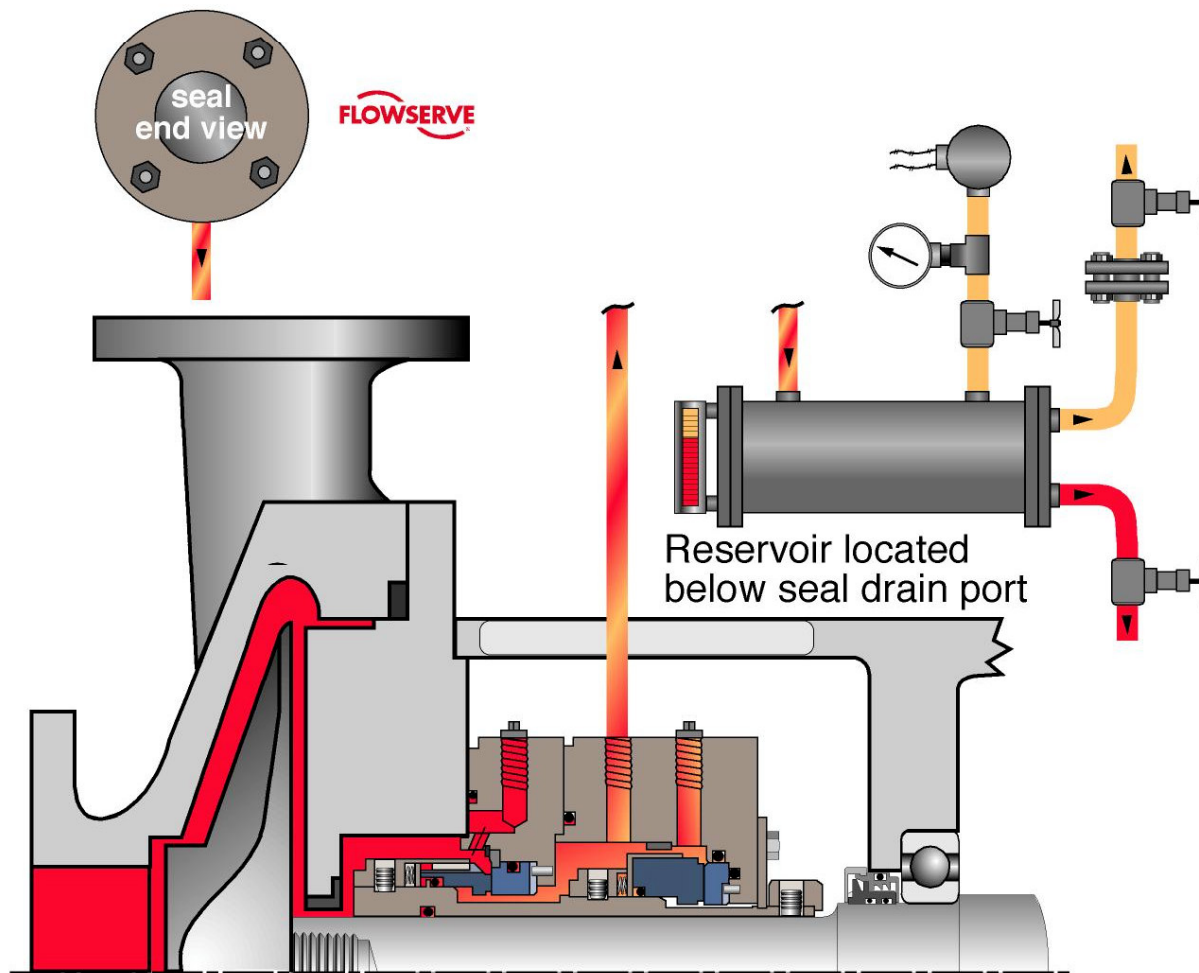
- Leakage collection for zero to very low process emissions.
- Safety indicator for primary seal.



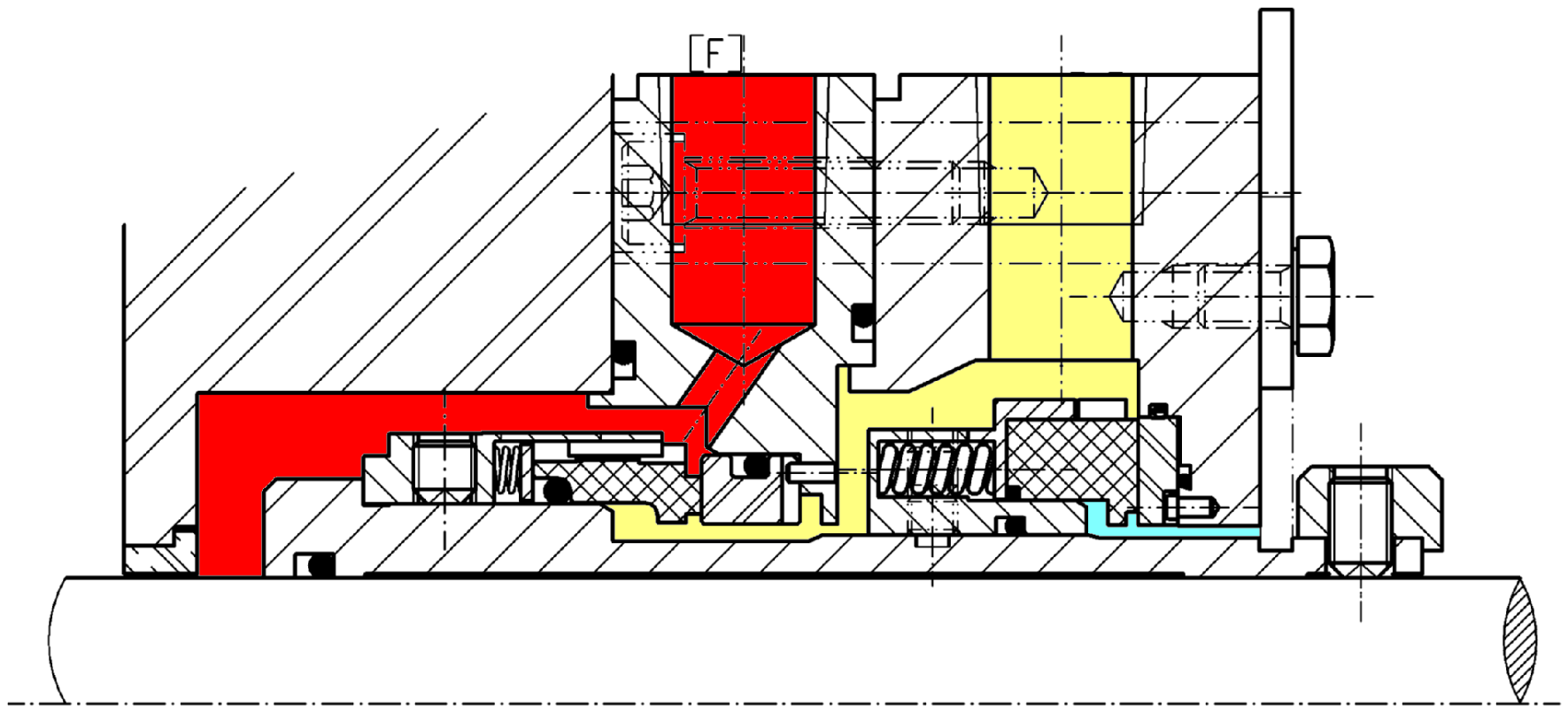
Plan 75

Where

- May be used alone or with Plan 72 on containment seals.
- Fluids that condense at ambient temperature.
- High pressure fluids, light hydrocarbons.
- Hazardous or toxic fluids.
- Clean, non-polymerizing, non-oxidizing fluids.



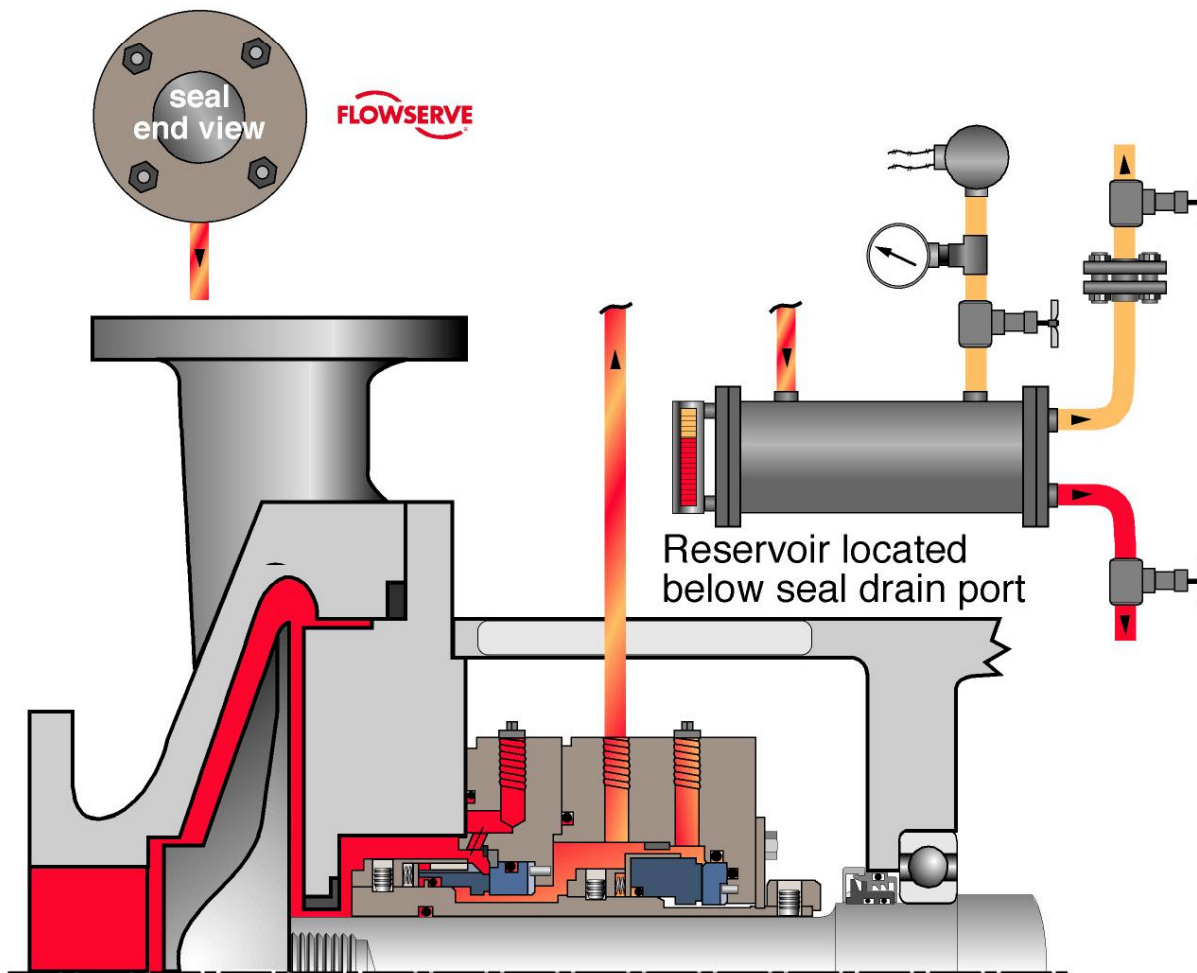
API 682 Type A with Containment 2CW - CS



Plan 75

Preventative Maintenance

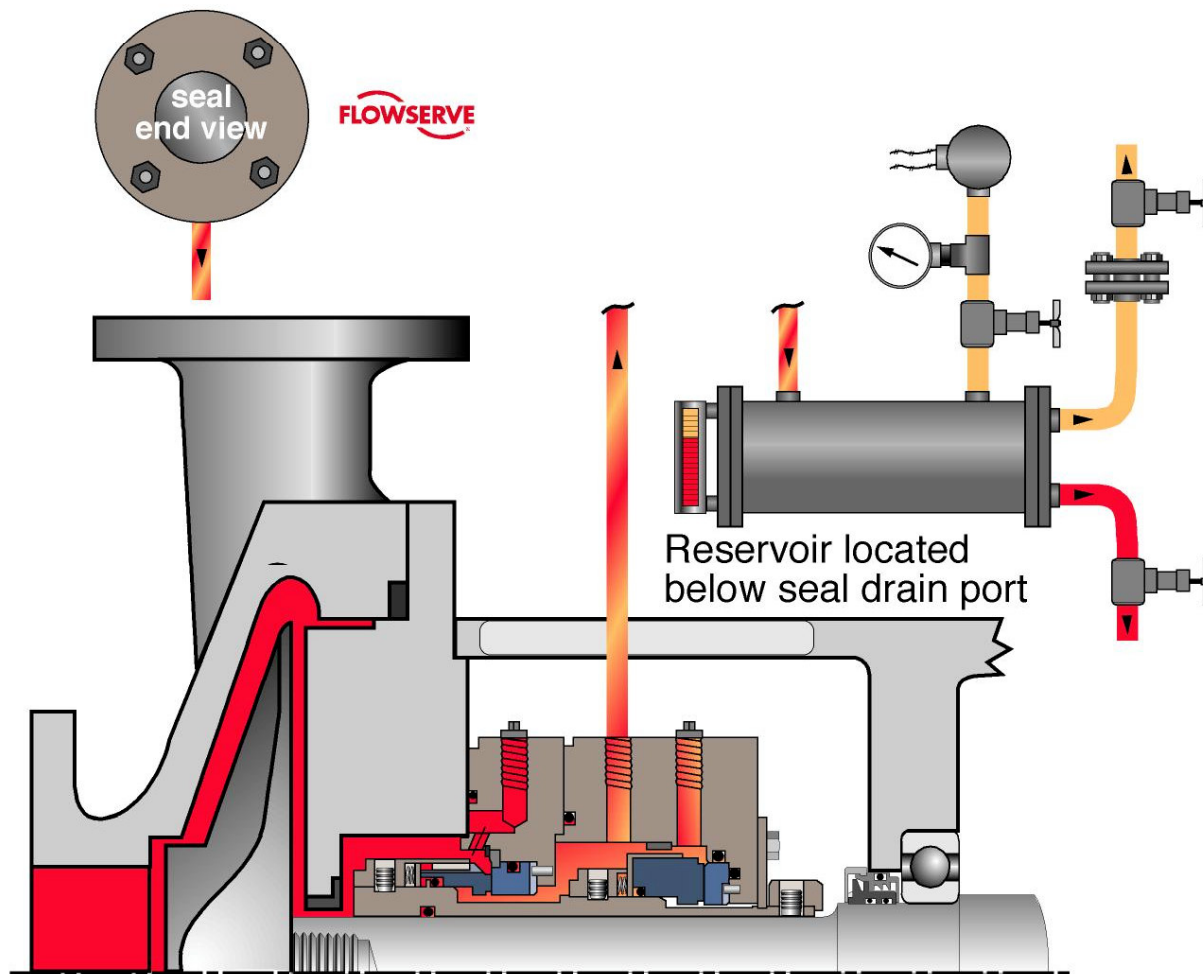
- Collection reservoir must be located below seal drain and downward-sloped piping.
- Continuously vent collection reservoir to low pressure vapor recovery/flare system.
- Drain collection reservoir to liquid recovery system as needed.



Plan 75

Preventative Maintenance (continued)

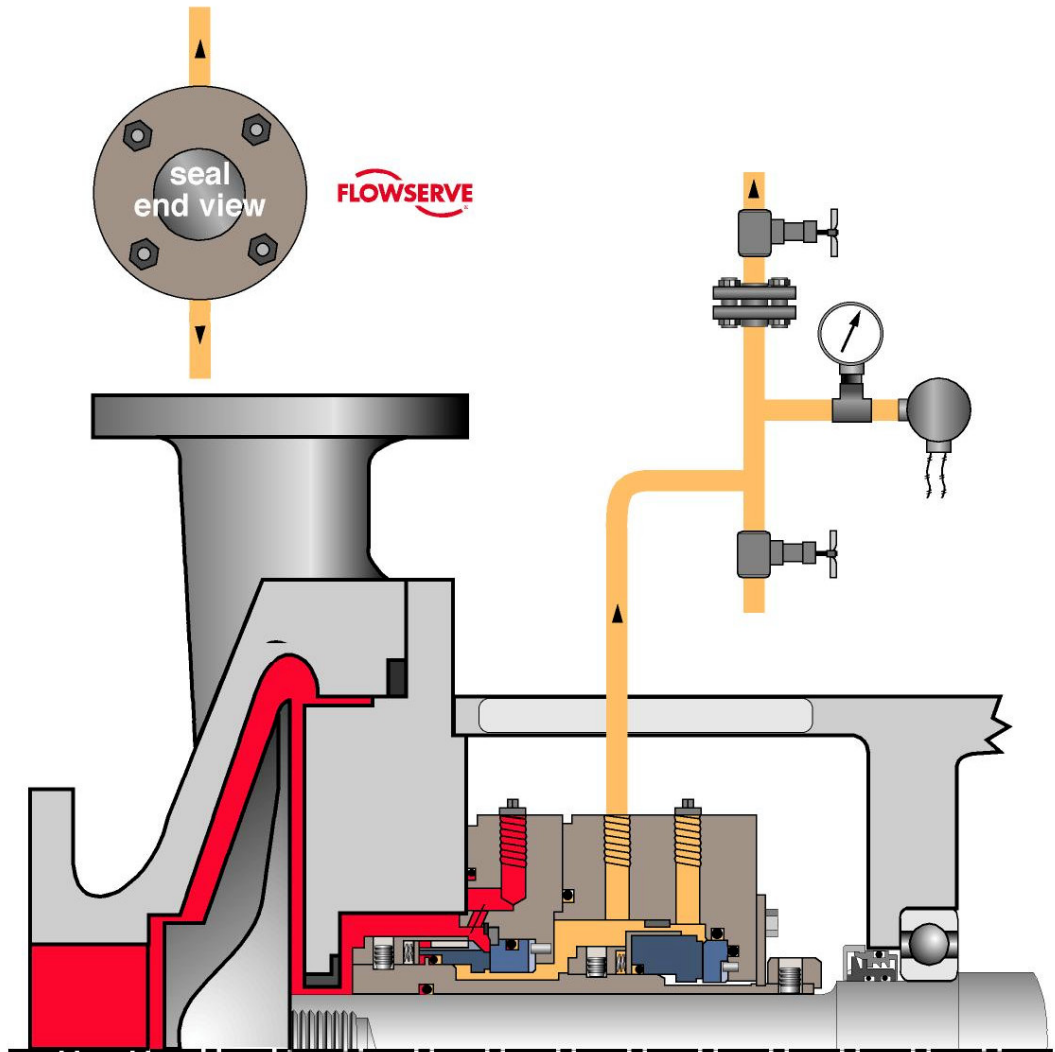
- Primary seal leakage is indicated by increased vent pressure.
- Monitor regularly for liquid level, valve settings, and low vent pressure.

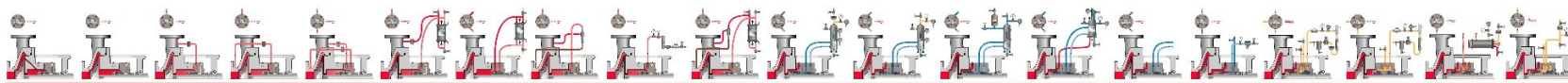
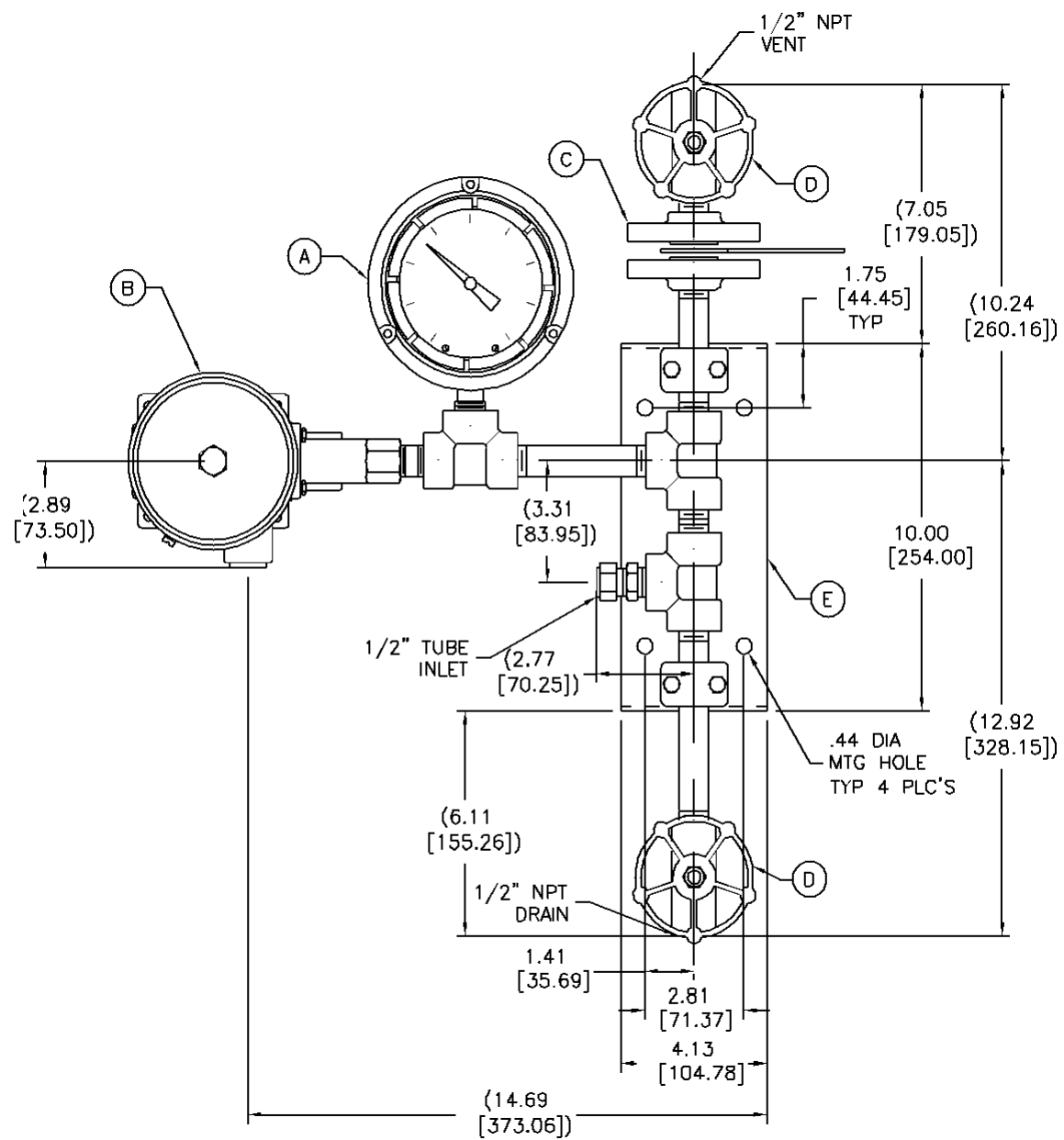


Plan 76

What

- Vent from containment seal cavity to vapor recovery.

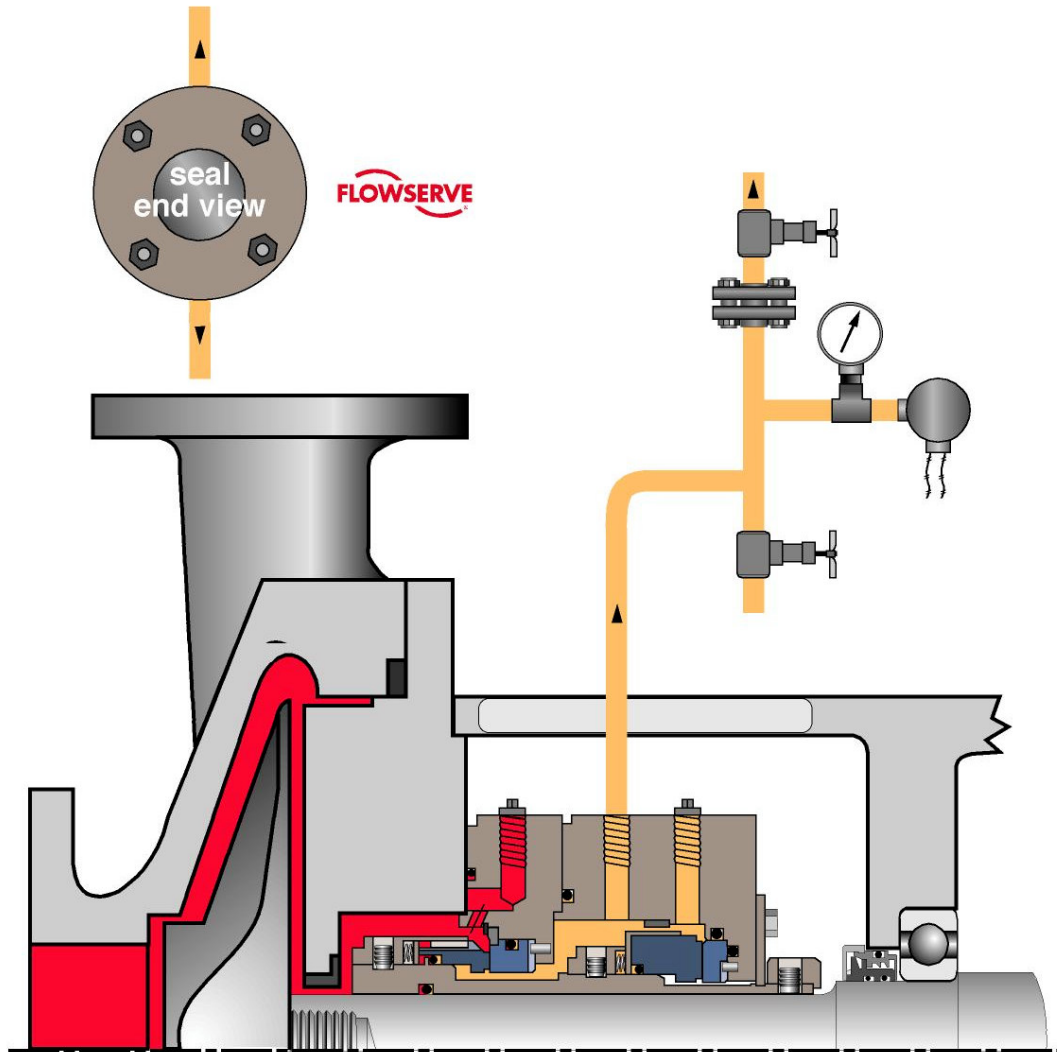




Plan 76

Why

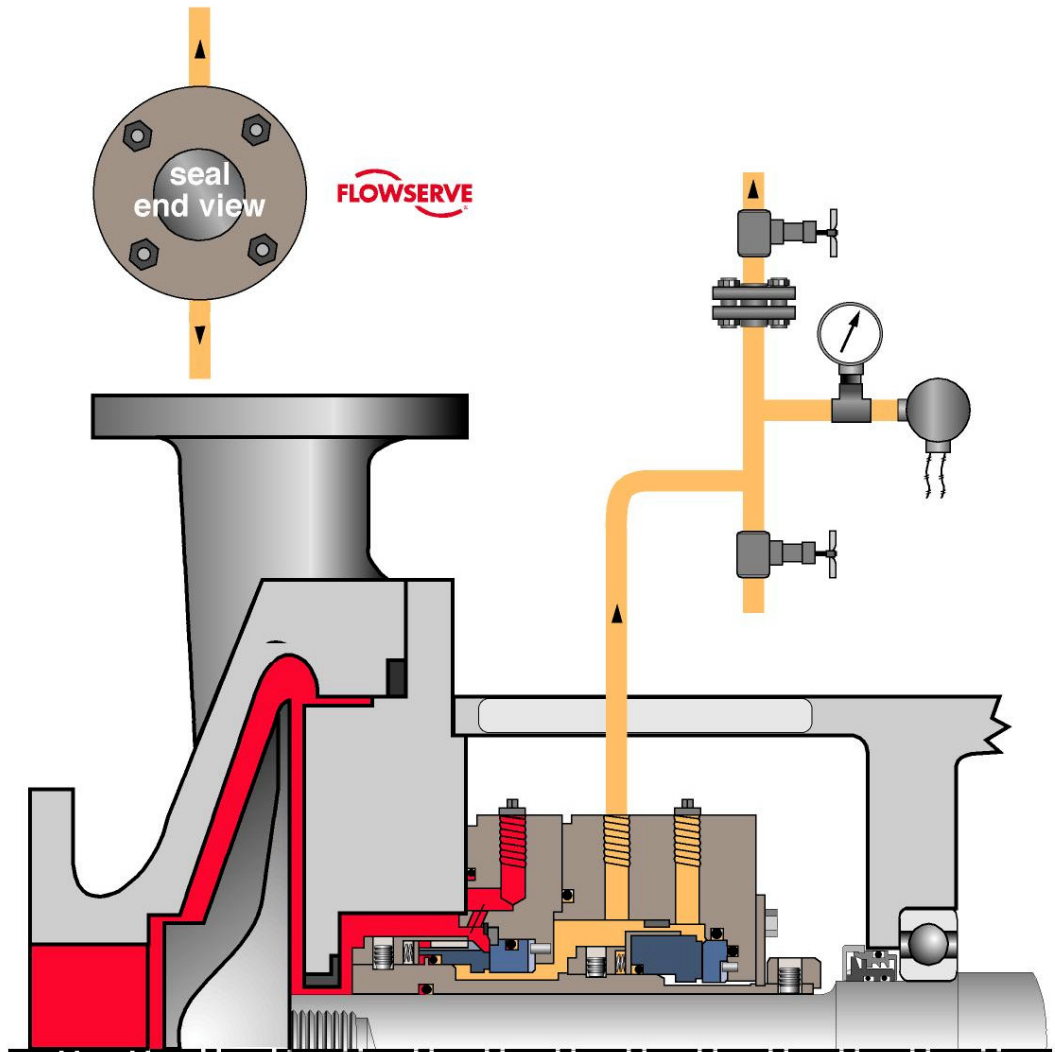
- Leakage collection for zero to very low process emissions.
- Safety indicator for primary seal.



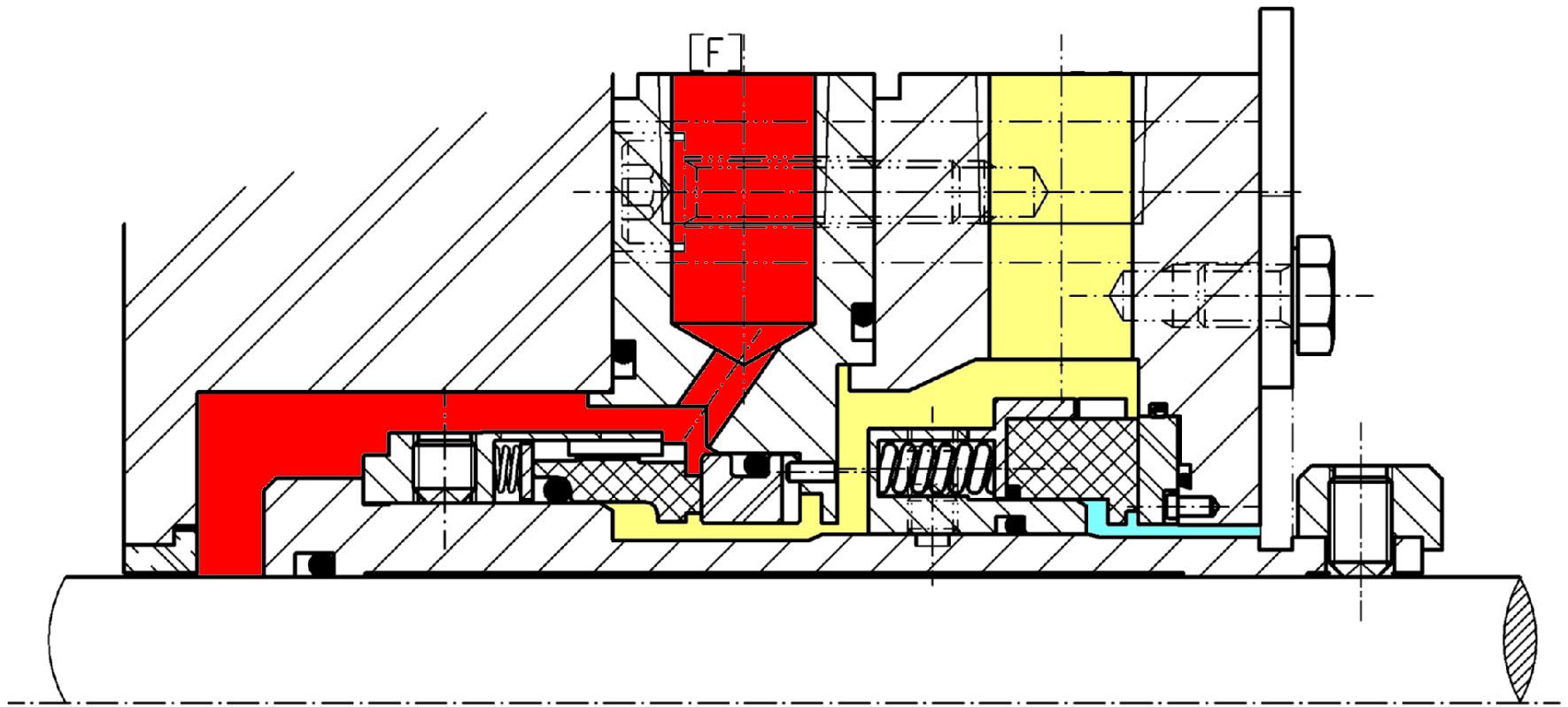
Plan 76

Where

- May be used alone or with Plan 72 on containment seals.
- Fluids that do not condense at ambient temperature.
- High vapor pressure fluids, light hydrocarbons.
- Hazardous or toxic fluids.
- Clean, non-polymerizing, non-oxidizing fluids.



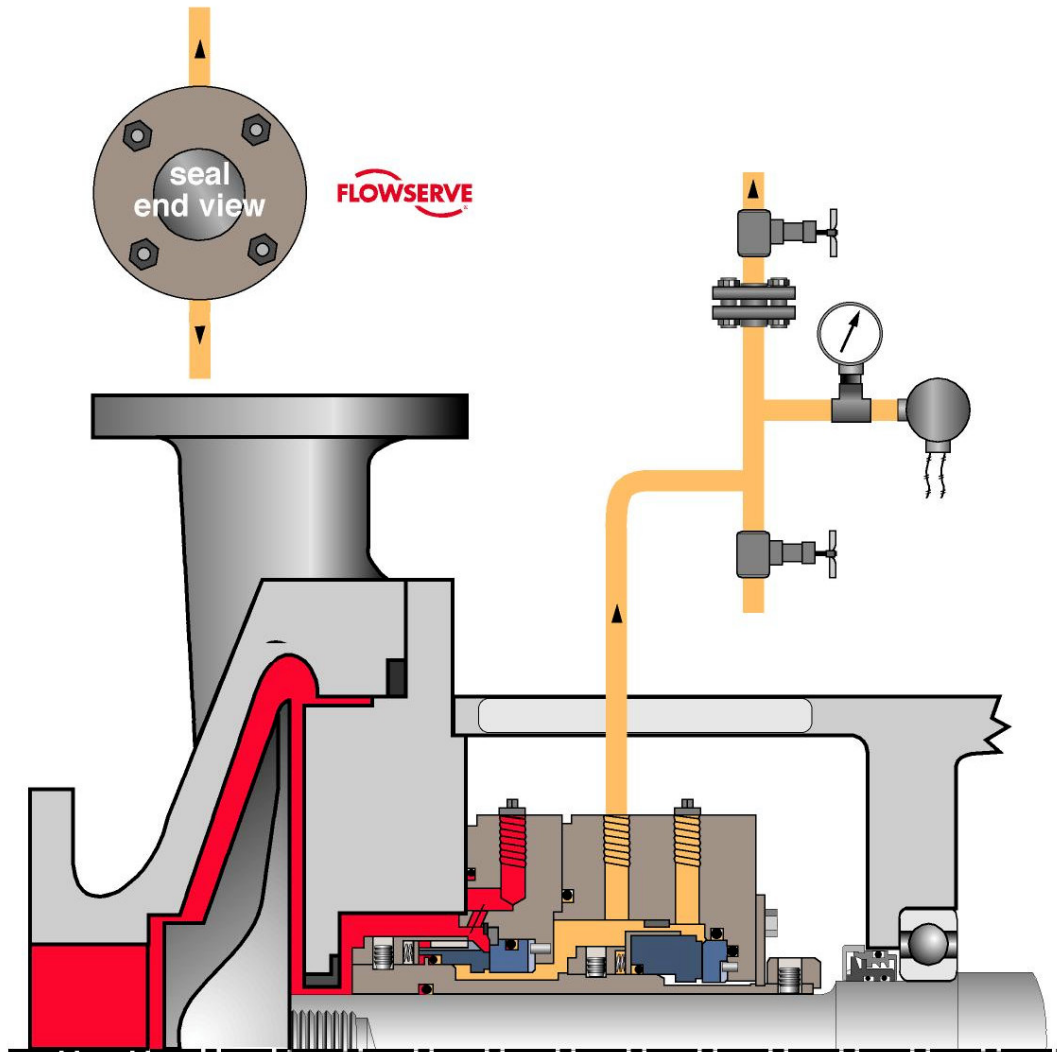
API 682 Type A with Containment 2CW - CS



Plan 76

Preventative Maintenance

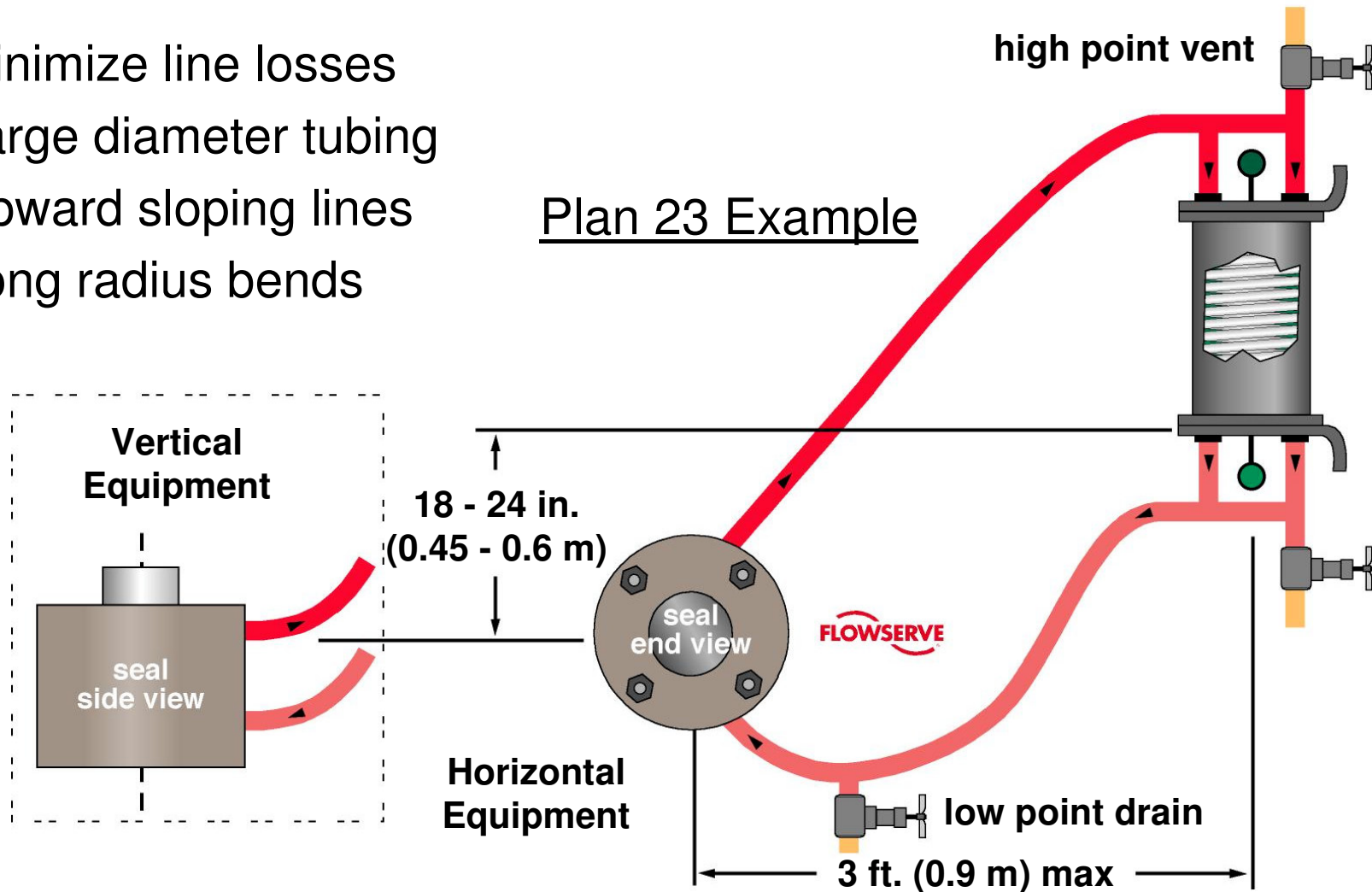
- Continuously vent to low pressure vapor recovery/flare system.
- Vent piping should include a condensate drain.
- Primary seal leakage is detected by increased vent pressure.
- Monitor regularly for valve settings, blocked lines, and low vent pressure.



Good Piping Practices

- ✓ Minimize line losses
- ✓ Large diameter tubing
- ✓ Upward sloping lines
- ✓ Long radius bends

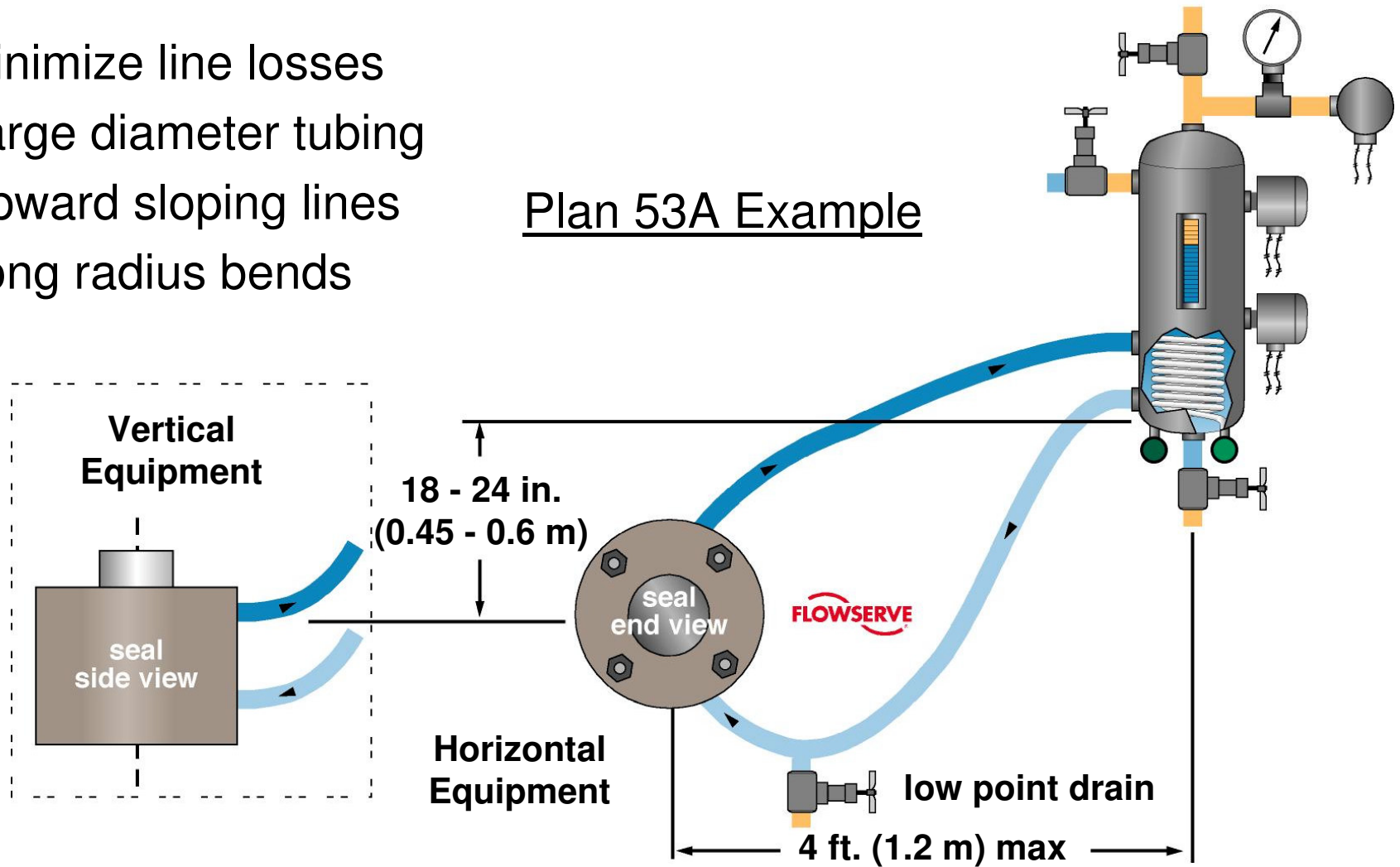
Plan 23 Example



Good Piping Practices

- ✓ Minimize line losses
- ✓ Large diameter tubing
- ✓ Upward sloping lines
- ✓ Long radius bends

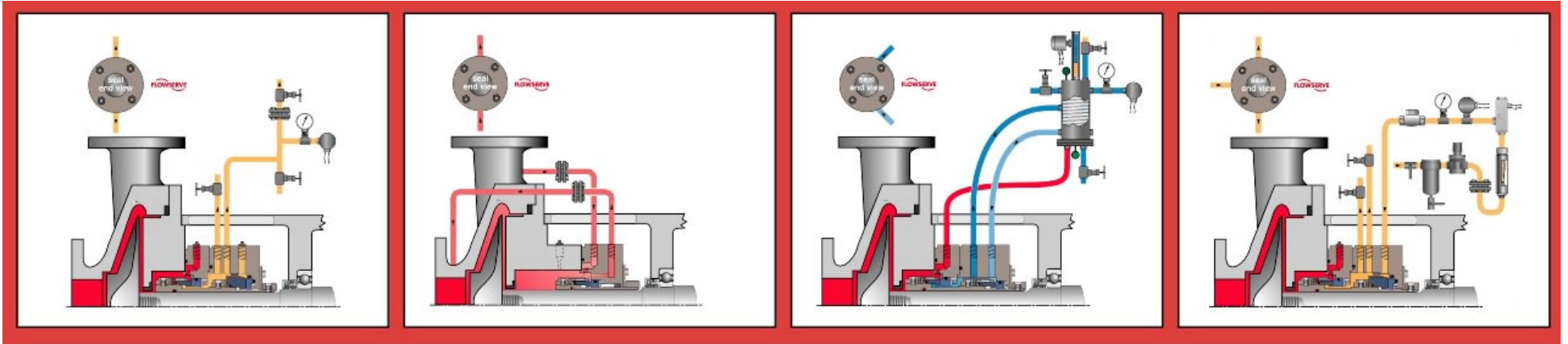
Plan 53A Example



Review

- Intended to create a more favorable environment for the seal
- Collect and detect seal leakage and provide safety backup
- Documented in several API, ASME, and ISO standards
- May require auxiliary equipment or external sources of fluids
- Necessary to improve seal reliability/Safety





Questions?

